1	One-pot preparation	of iron/alumina	catalyst for th	he efficient grow	th of vertically-
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- 2 aligned carbon nanotube forests
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22	Highlights:
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- One-pot, simple and fully wet method to prepare catalyst layers for the growth of VA-
- 25 CNT arrays.
- Nanotube height, diameter distribution, and crystalline quality comparable to those of
 existing but more costly and less versatile methods.
- The mechanism involves the concomitant formation of an aluminum-based buffer layer
 from aluminum hydroxides, and of catalyst nanoparticles from iron hydroxides at its
 surface.
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- 32

1 Abstract

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The catalytic growth of vertically-aligned carbon nanotubes (VA-CNTs) forest usually requires 3 thin catalyst films deposited by multi-step and costly physical vapor deposition techniques. 4 Here, we demonstrate that an efficient catalyst and its supporting layer for VACNT growth can 5 6 be prepared by using a simple solution of $Fe(NO_3)_3$ and $Al(NO_3)_3$ deposited on silica in a single 7 step. This process being much simpler and cheaper than existing preparation methods, it can easily be transferred to industry for the low-cost, thin and large-area coating of catalyst for VA-8 CNT growth. Our study shows that aluminum hydroxides preferentially react with the SiO₂ 9 surface while iron hydroxides tend to form oxide or hydroxide nanoparticles, thus allowing 10 preparation of an aluminum-based buffer layer with iron-based nanoparticles at its surface. 11 Optimization of the Fe/Al ratio and salt concentrations yielded catalysts with performances 12 similar to standard Fe/Al₂O₃ catalysts prepared by physical vapor deposition. 13

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Graphical Abstract



A simple and inexpensive route of large-scale elaboration of VA-CNTs

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1. Introduction

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During the last 25 years, carbon nanotubes (CNTs) have raised a great interest due to their 3 unique structural and physical properties. Vertically aligned CNTs (VA-CNTs) arrays in 4 particular have shown great potential for many applications such as field emission [1, 2], energy 5 storage [3, 4], gas sensors [5, 6], membranes [7, 8], structural composites [9, 10] or thermal 6 7 interface [11, 12]. Methods to produce tall and high-quality arrays of VA-CNTs are now well established, especially using the water-assisted catalytic chemical vapor deposition (C-CVD) 8 9 process, the so-called "super-growth" [13]. Industrial manufacturing of VA-CNTs is on the rise 10 but their production costs remain high, which strongly hinders the commercialization and wide application of VA-CNT-based materials. 11

12 The growth process of VA-CNTs typically involves a carbon feedstock decomposed at 13 high temperature on metal catalyst nanoparticles supported on an oxide layer, such as SiO₂ [14], MgO [15], or Al₂O₃ [13, 16], which acts as a buffer layer to prevent catalyst ripening and 14 15 diffusion in the bulk of the support (usually a silicon wafer). To date, the best and standard catalyst system for growing dense and tall VA-CNTs is a thin Fe film (0.4-2 nm) supported on 16 17 an Al₂O₃ underlayer (10-100 nm) [17]. Al₂O₃ is particularly efficient as its role is not limited to a simple diffusion barrier but is also believed to reduce hydrocarbon contamination of the 18 surface in the presence of H₂O [18] and to stabilize the oxidation state of iron nanoparticles 19 (Fe²⁺ and Fe³⁺) [19], restricting iron mobility on the surface, and therefore nanoparticle sintering 20 [20]. In most studies to date on VA-CNT growth, the buffer and catalyst layers are typically 21 prepared by physical vapor deposition (PVD) [21]. Although PVD systems are widely used in 22 the semiconductor industry, a less expensive and demanding process of catalyst deposition 23 would be highly beneficial for the large-scale and continuous production of VA-CNT arrays 24 [22]. Our work was therefore motivated by the need for a simpler and cheaper method of 25 26 catalyst preparation for the large-scale industrial production of VA-CNTs. Methods of wet 27 deposition of metal (Fe, Co, Ni,...) have already been reported on alumina or silica have been 28 developed using metal salt solutions or metal colloid suspensions as starting materials. The asmade catalysts showed activities comparable to those of PVD-prepared catalysts [22-26]. Wet-29 30 deposition methods were also developed to prepare the Al₂O₃ underlayer [27-29]. For example, Wang *et al.* developed a fully wet procedure using boehmite nanoplates (γ -AlO(OH)) deposited 31 on a silicon chip, which were converted in a 20-nm thick Al₂O₃ buffer layer by annealing at 32 750 °C in air. After deposition of a colloidal suspension of Fe₃O₄ nanoparticles, they obtained 33 a catalyst yielding millimeter-thick VA-CNT arrays [30]. However, this approach remains 34

complex and requires several steps: i) preparation and purification of the boehmite solution, ii)
deposition of the particles, iii) annealing to form an Al₂O₃ layer, iv) preparation and deposition
of the Fe₂O₃ colloidal suspension. Our goal was therefore to build on the versatility of wet
methods while developing a simpler and cheaper process than those previously reported.

Here, we report a simple and fully wet approach to prepare catalysts able to grow dense and tall 5 6 VA-CNT arrays on oxidized silicon wafers. The main novelty is that the aluminum-based buffer 7 layer and the catalyst nanoparticles at its surface are formed together in a single step. This method is based on the dip-coating of a single solution of a mixture of $Fe(NO_3)_3$, $Al(NO_3)_3$ and 8 NH₄OH which are widely available and low-cost precursors. Although similar approaches were 9 already tested in previous works, they did not yield tall VA-CNT arrays (< 50 µm) [31-33]. We 10 show here that a careful optimization of the concentrations of the different species in the 11 12 solution leads to a growth activity and a VA-CNT quality comparable to those obtained with typical PVD-made catalysts in the same growth conditions. 13

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2. Experimental

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17 2.1. Materials

Fe(NO₃)₃.9H₂O (ACS Reagent, >98%), Al(NO₃)₃.9H₂O (ACS Reagent, >98%), NH₄OH (5 M) 18 were purchased from Sigma-Aldrich and used without further purification. He (99.995%), H₂ 19 20 (99.9995%) and C₂H₄ (99.95%) were purchased from Linde Gas. Gas flow were controlled using Brooks GF80 mass flow controllers. Silicon wafers were thermally oxidized on both sides 21 22 to reach a layer of 600 nm of SiO₂. For reference, PVD Al₂O₃ sublayers were prepared by depositing 20 nm of Al₂O₃ by radio-frequency non-reactive sputtering. For control experiments 23 24 with PVD Fe, 1 nm of Fe was further evaporated on top of the Al₂O₃ layer. Just prior to dipcoating, thermally oxidized Si substrates (ca. 15x50 mm²) were washed by immersion into an 25 active NH₄OH (5 M) / H₂O₂ (5 M) / H₂O mixture for 15 min and then thoroughly washed with 26 H_2O . Substrates coated with Al_2O_3 were thoroughly washed with acetone, isopropanol and H_2O . 27 28

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2.2. Solution and catalyst preparation

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0.50 g of Fe(NO₃)₃.9H₂O was added to a 100 mL solution of 0.025 M NH₄OH to yield a clear
brown solution (Fe solution, Figure 1). Then, 0.46 g Al(NO₃)₃.9H₂O was added to yield a
transparent brown and acidic solution (pH ~ 4) hereafter called FeAl[X] solution with X being

the Fe/Al molar ratio in the solution. These solutions were then dip-coated at 20 mm.min⁻¹ in a
humidity- and temperature-controlled chamber (RH ≈ 50% at 27 °C) on freshly cleaned
thermally oxidized silicon wafers. The samples were dried at room temperature for 1-24 h
before CVD experiments.

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2.3. VA-CNT growth

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VA-CNT growth was performed using a standard water-assisted protocol [13]. Briefly, the 8 9 samples were placed on top of a silicon sample holder (40x50 mm²) in a 2-inches tubular furnace and heated in a He/H₂ mixture (600/400 sccm) during 15 min from room temperature 10 to 750 °C. At 750 °C, 200 ppm of H₂O were added using a small flow of He in a water bubbler 11 which was maintained at low temperature (typically 5 °C) and the samples were kept at 750 °C 12 13 in this atmosphere for 5 min. Humidity was controlled using an hygrometer (MIS Probe 2, General Electrics) prior to each experiment. Then, the samples were exposed for 10 min to a 14 15 He/C₂H₄ mixture (810/190 sccm) with 200 ppm H₂O to grow VA-CNTs. The furnace was then cooled under He at a temperature below 100 °C before opening and withdrawal of the samples 16 17 to prevent VACNT oxidation.

The samples presented in this study were prepared in four different runs. During each run, a reference catalyst prepared by PVD with 1 nm of Fe on 20 nm of Al₂O₃ (**PVD: Fe@Al₂O₃**) was added in the furnace and the thickness of VACNT grown on it was controlled by an optical camera to confirm the reproducibility of the growth conditions independently of the environmental conditions.

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24 2.4. Characterization

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Scanning electron micrographs were obtained using a Hitachi S4800 operating at 10 kV. 26 27 Raman characterization of the VA-CNTs was performed at a laser wavelength of 532 nm using 28 a Horiba Jobin-Yvon T64000 spectrometer equipped with a silicon camera cooled with liquid nitrogen and a microscope. The focused laser spot on the sample was typically 1 µm. Atomic 29 30 force micrographs were obtained using a Brucker AFM D3100 in tapping mode using a NCH point probe with a tip radius of 5 nm at F = 242.9 kHz, Q = 460 and k = 18 N.m⁻¹. X-Ray 31 Photoelectron spectroscopy (XPS) measurements were performed on Mepitel®. The excitation 32 source produced a monochromatic Al Ka line (1486.6 eV) and worked at 100 W of power. The 33 34 analyzed surface had a 400-um diameter. All XPS components were assigned from the analysis

of the values reported for reference compounds and referenced in the NIST database [34]. X-1 Ray diffraction (XRD) patterns were obtained using a PAN analytical X'Pert Pro MPD 2 diffractometer at Cu K α irradiation ($\lambda = 1.5418$ Å) with a step size of 0.033° (2 θ scale) in the 3 12° - 80° interval. Note that in the case of powders submitted to a reducing treatment for 4 subsequent XRD characterization, the samples were stored under inert gas just after the 5 reducing treatment to prevent oxidation in air. For other samples, they were normally exposed 6 7 to air as during the elaboration process before XRD and oxidation in air was taken into account for the XRD interpretation. Transmission Electron Microscopy (TEM) was first performed on 8 9 a JEOL 1200 EX II operated at 100 kV. High-Resolution TEM (HRTEM) micrographs were obtained with a FEI Titan Cs image aberration-corrected microscope working at 80 kV. In the 10 latter case, the observations were performed at low temperature (approx. 77 K) to avoid electron 11 irradiation damage of the nanotubes and possible contamination of the samples. Micrographs 12 13 were subsequently analyzed using the Gatan Digital Micrograph software taking intensity profiles through each tube to measure their diameter distribution. 14

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16 **3. Results**

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We first studied the influence of the catalyst preparation parameters on the features of the grown 18 CNTs. Figure 1 shows the typical procedure for the experiments conducted throughout this 19 study. First, we investigated the activity of a solution of Fe(NO₃)₃ in dilute NH₄OH (Fe 20 solution). The role of NH₄OH is to allow the formation of metal hydroxides able to condense 21 into nanoparticles. This solution was dip-coated on a thermally oxidized Si wafer (Fe@SiO₂) 22 and on a silicon wafer coated with an extra layer of 20 nm of Al₂O₃ deposited by PVD 23 (Fe@Al₂O₃). The activity of these catalysts was compared to that of a reference catalyst 24 prepared by PVD with 1 nm of Fe on 20 nm of Al₂O₃ (PVD: Fe@Al₂O₃). In each run, the 25 26 thickness of the VA-CNTs grown on the reference PVD catalyst was measured to be 660 µm 27 +/- 10 %, thus confirming the good reproducibility of the growth conditions. We observed that 28 thick VA-CNT arrays were grown on both PVD:Fe@Al2O3 and Fe@Al2O3, with thickness of, respectively, 650 µm and 590 µm (Table 1, entries 1 and 2). At the opposite, a thin layer of 29 entangled CNTs was grown with Fe@SiO2, in good agreement with previous studies performed 30 in the absence of an alumina under-layer [35, 36]. Second, we studied the influence of a PVD 31 Al₂O₃ under-layer on the activity of the FeAl[X] catalysts. As shown in table 1 (entry 3), a 32 FeAl[1] solution dip-coated on PVD Al₂O₃ (FeAl[1]@Al₂O₃) yielded a VA-CNT array with a 33 34 thickness of 690 μ m, while a slightly thinner array (550 μ m) was obtained with the same solution deposited on Si/SiO₂ (FeAl[1]@SiO₂, entry 7). Together, these results confirm the
 well-documented effect that an Al₂O₃ under-layer strongly promotes VA-CNT growth from Fe
 catalyst nanoparticles.

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Third, we studied the influence of the Fe/Al ratio (X=[Fe]/[Al]) on the activity of the 7 FeAl[X]@Al₂O₃ catalysts. The maximum VA-CNT thickness (660 µm) was obtained with a 8 Fe/Al ratio of 0.6 (FeAl[0.6]@SiO₂, Table 1, entry 5). Importantly, this thickness is comparable 9 to the one obtained with the reference PVD catalyst thus demonstrating that catalysts prepared 10 by a simple dip-coating step can yield VA-CNT forests with heights similar to PVD-made 11 catalysts. Higher and lower Fe/Al ratio yielded thinner VA-CNT layers (Table 1, entries 4-9). 12 Fourth, the effect of increasing the total concentration of Fe and Al salts was investigated. By 13 14 doubling the total concentration in Fe and Al salts, significantly taller VA-CNTs were obtained:

 $640 \,\mu\text{m}$ for **2xFeAl[1]@SiO**₂ (entry 12) by comparison to 550 μm for **FeAl[1]@SiO**₂ (entry 7).

640 μm for 2xFeAl[1]@SiO₂ (entry 12) by comparison to 550 μm for FeAl[1]@SiO₂ (entry 7).
Note that for Fe solution deposited on PVD Al₂O₃, doubling the Fe concentration has little

effect: 620 μ m for **2xFe@Al₂O₃** (entry 10) to be compared to 590 μ m for **Fe@Al₂O₃** (entry 2).

All together, these results highlight the high potential of this fully-wet single-step approach
 since a simple coating by Fe and Al salt solutions directly on Si/SiO₂ shows performances
 comparable to those of PVD catalysts.

The morphologies of the VA-CNT arrays were then analyzed by scanning electron microscopy 4 5 (SEM) as shown in Figure 2. SEM pictures showed well aligned CNTs on all the samples grown 6 on Al₂O₃ (Fig. 2a-c) while less aligned and curly CNTs were observed for the samples grown 7 from FeAI[X]@SiO₂ (Fig. 2d-h) with X between 0.2 and 1.5. Since alignment is essentially caused by steric interactions between CNTs, this supports that FeAl[X]@SiO2 catalysts yield 8 a lower CNT density of the VACNT forests than PVD catalysts. In general, a lower 9 homogeneity in CNT height was observed in VA-CNTs grown from FeAl[X]@SiO2 catalysts 10 when compared to PVD catalysts, which also points toward a less homogeneous and less dense 11 12 distribution of active catalyst particles.

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14 Table 1. VA-CNT height, Raman G-band positions and G/D ratio ($\lambda = 532$ nm) of the

	Catalyst	[Fe] (mol.L ⁻¹)	[Fe]/[Al]	VA-CNT	G	CD
Entry				height	band	G/D
				(µm)	(cm ⁻¹)	ratio
1	PVD: Fe@Al ₂ O ₃	N/A	N/A	660 +/- 10%	1584	3.2
2	Fe@Al ₂ O ₃	0.0125	N/A	590	1583	2.2
3	FeAl[1]@Al2O3	0.0125	1	690	1581	3.7
4	FeAl[0.2]@SiO2	0.0125	0.2	420	1576	1.1
5	FeAl[0.6]@SiO2	0.0125	0.6	660	1576	1.2
6	FeAl[0.8]@SiO2	0.0125	0.8	550	1578	2.8
7	FeAl[1]@SiO2	0.0125	1	550	1579	1.5
8	FeAl[1.5]@SiO2	0.0125	1.5	450	1584	1.5
9	FeAl[2]@SiO2	0.0125	2	250	1577	1.2
10	2xFe@Al ₂ O ₃	0.25	N/A	620	1575	4.8
11	2xFeAl[0.8]@SiO ₂	0.25	0.8	n.d.	1580	2.5
12	2xFeAl[1]@SiO2	0.25	1	640	1580	3.1

15 samples grown from the different catalysts.



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Figure 2. SEM pictures of the VA-CNTs grown from: a. PVD: Fe@Al<sub>2</sub>O<sub>3</sub>, b. Fe@Al<sub>2</sub>O<sub>3</sub>,
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     c. FeAl[1]@Al2O3, d. FeAl[1]@SiO2, e. FeAl[0.2]@SiO2, f. FeAl[0.6]@SiO2, g.
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     FeAl[0.8]@SiO<sub>2</sub>, h. FeAl[1.5]@SiO<sub>2</sub>, i. 2xFe@ Al<sub>2</sub>O<sub>3</sub>, j. 2xFeAl[1]@SiO<sub>2</sub>.
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Figure 3. a,b) Representative HRTEM pictures of CNTs and catalyst crystalline nanoparticles (highlighted by a red contour) after growth using the FeAl[1]@SiO₂ catalyst. In b), a Fast Fourier Transform (FFT) has been applied to the TEM image and the crystalline spots corresponding to the catalyst NPs have been selected to apply an inverse FFT for building the insert image at the top left. c,d) Outer tubes diameter distribution diagram of FeAl[1]@SiO₂ (c) and Fe@Al₂O₃ (d), respectively.

The diameter distribution of the CNTs grown from **PVD:** Fe@Al₂O₃, Fe@Al₂O₃, and **FeAl[1]@SiO**₂ were evaluated by TEM and found to be comparable for the three samples with most tubes having diameters of 5 +/- 1 nm. The structure of the CNTs grown from **FeAl[1]@SiO**₂ was further analyzed by high-resolution TEM showing that mainly double- and triple-wall CNTs were obtained (Figure 3, mean size 5.6 +/- 1.6 nm with a ratio of 2.4 DWCNTs for 1 TWCNT). By comparison, VA-CNTs grown from Fe@Al₂O₃ showed slightly thinner nanotubes with a higher proportion of DWCNTs (5.2 +/- 0.8 nm with 3.3 DWCNTs for 1

- 1 TWCNT, Figure 3). The crystalline quality of all CNTs was found relatively good and
- 2 comparable to that reported in the literature for VA-CNTs grown from PVD-made catalysts.



Figure 4. Raman spectra of VA-CNT arrays grown from the different catalysts.

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The samples were then analyzed by micro-Raman spectroscopy (Figure 4). All the VA-CNTs
samples showed a G band at around 1580 cm⁻¹ (see Table 1) as expected from a sample

dominated by multi-walled CNTs (MWCNTs) with diameters in the range of 3-7 nm as 1 measured by HRTEM (Figure 3). All samples also displayed D and 2D (G') bands at positions 2 in the range of 1327-1338 cm⁻¹ and 2642-2670 cm⁻¹, respectively. This is also in good 3 agreement with the positions expected for MWCNTs at 532 nm of laser excitation. Many 4 samples showed additional signals at low frequencies (less than 280 cm⁻¹) associated with the 5 radial breathing modes (RBMs) of small diameter CNTs (d = 1-3 nm). The occurrence of RBMs 6 7 is systematically associated with higher intensities of the G and 2D bands and to downshifted D and 2D bands as also expected when moving toward such smaller-diameter CNTs. Since 8 9 CNTs of 1-3 nm were not observed during our HRTEM observations but display an intrinsically higher Raman cross section due to the resonance effect, the results agree with samples mainly 10 composed of double/triple-wall CNTs with 3-7 nm diameter with traces of CNTs with 1-3 nm 11 12 diameter. The proportion of small-diameter CNTs was generally found higher for the catalysts deposited on PVD alumina. Note that having a mixture of large-diameter CNTs (weakly 13 resonant and with low G/D ratio) and small-diameter CNT (highly resonant and with high G/D 14 15 ratio) hinders the use of the G/D ratio (Table 1) to evaluate the overall crystalline purity of the sample. Instead, for the samples studied here, a higher G/D ratio essentially denotes a higher 16 17 proportion of small-diameter CNTs in agreement with the other Raman features (more intense 18 RBMs, downshifted D and 2D bands). By comparing the Raman spectra at different positions, one may roughly estimate that large- and small-diameter CNTs display a G/D ratio in the range 19 of 1-2 and 2-6, respectively and quite independently of the catalyst. Of course, this value is 20 expected to strongly vary with the growth conditions (temperature, precursor pressure) used 21 [37]. Overall, the TEM and Raman results shows that our wet-based catalyst preparation 22 method allows the preparation of VA-CNT arrays with similar morphology and structural 23 quality than standard PVD catalyst, yet with the use of simpler protocol and laboratory 24 equipment. 25

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27 **4. Discussion**

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To understand the effect of the addition of the Al salt, the catalyst formation mechanism was
investigated using Atomic Force Microscopy (AFM), X-ray Diffraction (XRD) and X-ray
Photoelectron Spectroscopy (XPS).



Figure 5. AFM images of a. FeAl[1]@SiO₂ before annealing, b. FeAl[1]@SiO₂ after
annealing at 750 °C under H₂ and c. PVD: Fe@Al₂O₃ after annealing at 750 °C under H₂.

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5 AFM observations of the samples after deposition of solution FeAl[1] on Si/SiO₂ and drying 6 were first performed. As shown in Figure 5a, large nanoparticle aggregates of 10-50 nm were observed on the surface. Since the diameter of a MWCNT is strongly related to the size of its 7 8 catalyst particle [36, 38], these particles are not likely to be directly responsible for the observed catalytic activity since the CNT diameter distribution was determined to be 5.6 +/- 1.6 nm 9 10 (Figure 3c). Interestingly, after annealing at 750°C under a He/H₂ mixture with 200 ppm H₂O and rapid cooling to RT under a He/H2 flow, well-defined and smaller nanoparticles were 11 12 observed (height around 5 nm) on the surface (Figure 5b). When compared to the PVD catalyst (Figure 5c) whose surface is very homogeneous after reduction, FeAl[1]@SiO₂ surface shows 13 the presence of some larger nanoparticles (around 10 nm in height). This is in good agreement 14 with our SEM observations of less dense and curvy VA-CNTs [39] obtained with the catalysts 15 prepared by dip-coating. From AFM measurements, it is clear that a severe surface 16 reconstruction occurs during the H₂ treatment. 17



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Figure 6. a. XRD of the dry residue of Fe(NO₃)₃ aqueous solution with 1 equivalent of 2 NH4OH before reduction showing mainly the presence of NH4NO3 [40] (ICSD collection 3 4 code 002772). b. XRD of the dry residue of a Al(NO₃)₃ aqueous solution with 1 equivalent of NH4OH before reduction showing mainly the presence of NH4NO3 [40] c. XRD of a dry 5 6 residue of a FeAl[1] solution showing mainly the presence of Wuestite (Iron Oxide Fe0.902O) [41] (ICSD collection code 040089) and NH4NO3 [40]. d. XRD of FeAl[1] 7 8 impregnated on high surface area silica solution after reduction under H₂ at 750°C 9 showing only the typical large shoulder of amorphous silica.

To further investigate the composition of the thin catalyst film before CVD experiments, XRD 10 measurements of the solid residue obtained after evaporation of the different solutions were 11 performed. Before reduction, the solid residue of a $Fe(NO_3)_3$ aqueous solution with 1 equivalent 12 of NH₄OH (Fe solution) showed the presence of crystalline NH₄NO₃ (Figure 6a) with average 13 crystal sizes larger than 100 nm. The same result was obtained for the solid residue of a 14 Al(NO₃)₃ aqueous solution with 1 equivalent of NH₄OH (Figure 6b). The residue of **FeAl[1**] 15 16 also showed the presence of crystalline NH₄NO₃ nanoparticles, along with crystalline FeO nanoparticles (Figure 6c). However, there was no signature of crystalline Al-based compounds. 17

Interestingly, when solution FeAl[1] was coated on high surface-area silica and reduced under H₂, no diffraction peaks were observed, which indicates that large metallic Fe nanoparticles were not formed in agreement with AFM observations (Figure 6d). The disappearance of the large NH₄NO₃ crystal nanoparticles previously observed provides an explanation for the evolution of surface roughness observed by AFM before and after H₂ reduction as further supported by the decomposition temperature of NH₄NO₃ (210°C).

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8 XPS analysis were then performed. Surface analysis of sample FeAl[1]@SiO₂ after drying, but
9 before reduction under H₂, showed a very large contribution of the SiO₂ substrate with 25.5%
10 of Si, and only 5.0% of Al and 5.0% of Fe (Table 2).

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Sample Name	Treatment	Si (2p)	O (1s)	Fe (2p)	Al (2p)
FeAl[1]@SiO2	after deposition	25.7	64.2	5.1	5.1
FeAI[1]@SiO2	after H ₂ reduction	36.7	58.3	1.2	3.7
Fe@SiO2	after H ₂ reduction	41.1	58.4	0.5	0,0
Fe@Al ₂ O ₃	after H ₂ reduction	0,0	55.8	1.0	43.1

12 Table 2. Surface composition of the catalyst: elemental composition from XPS.

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Since XPS is only sensitive to the top 10 nm of the surface, this indicates that the deposited 14 15 layer is very thin (less than 10 nm) and/or not continuous. The Fe 2p_{3/2} profile is made of two contributions: an Fe(II) contribution at 709.8 eV and an Fe(III) contribution at 711.1 eV with a 16 17 Fe(II)/Fe(III) ratio of 1.65, plus two satellite peaks at higher energy (Figure 7a). This excludes the presence of metallic iron (expected at ~707 eV), of iron silicide (Fe₃Si expected at 707.5 18 eV) and of iron silicate (Fe₂SiO₄ expected at 708.9-709.0 eV). It also excludes the possibility 19 20 of a single Fe(II) or Fe(III) compound, or of Fe₃O₄ only (which has an Fe(II)/Fe(III) ratio of 21 0.5). For the Fe(III) peak at 711.1 eV, the most likely assignment is FeO(OH) (expected at 711.0-711.8 eV) or alternatively Fe₂O₃ (which is expected at 710.7-711.4 eV). For the Fe(II) 22 peak at 709.8 eV, the most likely assignment is FeO which is expected at 709.6-710.3 eV. The 23 Al 2p peak is found at 74.8 eV (Figure 7c) which would nicely agree with an aluminosilicate 24 such as Al₂OSiO₄ (expected at 74.5-74.9 eV) or an aluminum silicate hydroxide such as 25 Al₂Si₄O₁₀(OH)₂ (expected at ~74.7 eV), which in both cases would support a strong anchoring 26 of aluminum with the SiO₂ substrate. 27

After H₂ annealing, an even larger atomic contribution of Si (36.6 %) was observed, with 3.7% 1 of Al and 1.2% of Fe remaining on the surface (Table 2), showing significant Fe diffusion in 2 the SiO₂ matrix at high temperature (750°C). The Fe $2p_{3/2}$ profile displayed little change with 3 still two contributions: an Fe(II) contribution at 710.1 eV and an Fe(III) contribution at 711.4 4 5 eV with about the same Fe(II)/Fe(III) ratio as before reduction (Figure 7b). At the opposite, the Al 2p peak was strongly downshifted to 74.0 eV (Figure 7c), which could be assigned to 6 7 Al(OH)₃ (expected at 73.9-74.4 eV) or alternatively to FeAl₂O₄ (expected at ~74.3 eV). The latter one should give rise to an Fe 2p_{3/2} contribution at ~710.0 eV which is in good agreement 8 with the Fe(II) peak observed at 710.1 eV. We performed the same H₂ treatment and XPS 9 analysis on the same solution without $Al(NO_4)_3$ (*i.e.* Fe@SiO₂) and found that the amount of 10 Fe remaining at the surface was about three times less (Table 2). This provides an additional 11 support for the formation of an iron aluminate such as FeAl₂O₄ which would stabilize Fe at the 12 13 surface of SiO₂. The remaining Fe(III) peak is assigned to Fe₂O₃ and/or FeO(OH) formed from reduced iron when exposed to air (Figure 7d). 14



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Figure 7. Fe 2p XPS spectra of a) FeAl[1]@SiO₂ before H₂ reduction, and b) after H₂
reduction; c) Al 2p XPS spectra of FeAl[1]@SiO₂ before H₂ reduction (blue), and after H₂
reduction (black) compared to Fe@Al₂O₃ after H₂ reduction (red); Fe 2p XPS spectra of
d) Fe@SiO₂ after H₂ reduction and e) Fe@Al₂O₃ after H₂ reduction.

9 Taken together, these results support the following picture (Figure 8). During air drying, Al(OH)₃ tends to react with the SiO₂ surface (*e.g.* with hydroxyl groups) to form a surface layer 10 11 of aluminosilicate or aluminum silicate hydroxide compounds, while Fe(OH)₃ tends to form 12 FeO or FeO(OH) nanoparticles. During H₂ annealing, particles of Fe oxides and hydroxides can 13 either get reduced to metallic iron which then tends to diffuse into the SiO₂ substrate. Alternatively, in the presence of surface aluminum oxides or hydroxides, they can form surface 14 15 layers of iron aluminates which are less reducible and act as a buffer layer which stabilizes small iron nanoparticles at their surface. So, beside its standard role of diffusion barrier, SiO₂ 16

plays another role in our process, by allowing the formation of a mixed Al-Si oxidized layer 1 which will anchor and stabilize catalyst nanoparticles. If exposed to a carbon source during 2 CVD, these stabilized iron particles will allow the growth of long CNTs. Instead, if exposed to 3 air, these iron nanoparticles will quickly become oxidized into Fe(III) compounds such as Fe₂O₃ 4 5 or FeO(OH). This mechanism supports that increasing the concentration of Al in the solution at constant ratio with Fe should increase the surface coverage with aluminum compounds and 6 7 therefore a higher density of stabilized iron particles and so a higher yield of long and defective nanotubes: this is in perfect line with our previous observation that doubling the proportion of 8 9 Fe and Al promotes both a taller VACNT forest and a lower defect density (see entry 12 of 10 table 1).





13 Figure 8. Proposed mechanism for catalyst formation and evolution.

14

12

15 **5.** Conclusion

16

In this study, a fully wet process was developed to prepare, in a single deposition step, a catalyst 17 to grow VA-CNT arrays on standard SiO₂/Si wafers. This is important from a materials 18 engineering point of view because the process is much simpler and cheaper than existing 19 20 preparation methods. We therefore expect it to be easily transferred to industry for low-cost and 21 large-area coating of catalyst for VA-CNT growth. This catalyst, prepared from a mixture of Fe(NO₃)₃ and an Al(NO₃)₃, yields VACNT height comparable to those of Fe/Al₂O₃ catalysts 22 prepared by PVD which is standardly used for VA-CNT growth. Our study showed that, when 23 mixed together, aluminum hydroxides preferentially react with the SiO₂ surface while iron 24

hydroxides tend to react together to form oxide or hydroxide nanoparticles: this explains why 1 a single solution step can be used to prepare both an aluminum-based buffer layer and catalyst 2 nanoparticles at its surface. This is important from a materials science point of view because it 3 shows that chemical affinities between reactants can be played with to elaborate the catalyst 4 nanoparticles and their supporting layer together in a single step. Following this initial 5 demonstration, the approach may be further optimized and generalized to other catalysts to 6 7 increase the homogeneity and density of the CNT forest and obtain a better control of the CNT diameter and crystalline quality. This simple and versatile approach appears as a strong 8 9 alternative to PVD to easily prepare VA-CNT forests on various substrates, such as curved, porous or conducting substrates. Importantly for applications in electronics and 10 electrochemistry requiring to electrically contact VA-CNT arrays, this process requires only a 11 very thin layer of insulating oxide material, therefore allowing a more intimate contact between 12 13 CNTs and their substrate.

14

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26

27 Data availability

28 No raw/processed data are required to reproduce these findings.

29

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