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Optimization and characterization of CLEAs of the very thermostable dimeric peroxidase from *Roystonea regia*[†]

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This paper describes the optimization of the immobilization of the peroxidase from *Roystonea regia* (RPTP) using the technique of the crosslinking enzyme aggregates. The immobilization was optimized using response surface methodology and after evaluating three different precipitants, ethanol was finally selected. Three variables were analyzed, glutaraldehyde concentration, precipitant concentration and time before collecting the RPTP-CLEAs. The immobilization yield was around 75%. The activity of the RPTP-CLEA was very high, this was even more patent at pH 3, where the free RPTP was fully inactive and the RPTP-CLEA maintained 40% of the maximum activity. In stress inactivations, the RPTP-CLEA maintained the very high thermostability that presented the free enzyme at 90 °C and pH 7 (half-live of 50 min). At pH 3, the free enzyme suffered subunit dissociation as a first step of the inactivation, this is not possible using RPTP-CLEAs and provided a very high thermostabilization (that depends on the enzyme concentration). The stability of the enzyme in the presence of hydrogen peroxide is good at low concentrations of this reagent (e.g., 10 mM), but if the concentration is higher (e.g., 300 mM), the enzyme stability drops. The immobilization provides an improved stability in the presence of this oxidant, but the values reached may not be high enough for some applications. The RPTP-CLEAs may be used for the decoloration of methyl orange solutions using 5 mM of hydrogen peroxide for 4 cycles (4 h each cycle) without apparent decrease in activity (but only degrading around 50% of the substrate). Using 225 mM of this oxidative reagent, the activity slowly decreased after each cycle (but enabling the full destruction of the colorant). This immobilized enzyme may be used even at pH 3 and 225 mM hydrogen peroxide, conditions where the free enzyme is completely inactive.

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1. Introduction

Peroxidases are ubiquitous oxidoreductases that use hydrogen peroxide or alkyl peroxides as oxidants. They may have different

uses as industrial biocatalysts.¹ They may effectively catalyze selective oxidations of electron-rich substrates, which include the hydroxylation of arenes, the oxyfunctionalizations of phenols and aromatic amines, the epoxidation and halogenation of olefins, the oxygenation of heteroatoms and the enantioselective reduction of racemic hydroperoxides.^{2,3} They can also catalyze the oxidative polymerization of different compounds (e.g., phenols and aromatic amines).⁴ Peroxidase may be also of interest in contamination control, e.g., soil detoxification, or remediation of wastewater industrial dyes.⁵ Peroxidases have also found use in analytical systems in biosensors, as the determination of the hydrogen peroxide concentration linked to different oxidases.⁴

Hydrogen peroxide is a substrate of these enzymes, and this makes that the enzyme needs to be in contact with it, with the likely problems that this can generate in terms of enzyme stability.⁶ In many instances, the enzyme has been coupled to an oxidase to generate, *in situ* and in a continuous way, low amounts of this compound that could have a lower effect on enzyme stability.^{7–9}

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The peroxidase from royal palm (*Roystonea regia*) (RPTP) has special interest due to its reported extreme thermostability and resistance to acid conditions. It was first described in pure form in 2001, as an enzyme having a molecular weight of 51 kDa and an isoelectric point of 3.5.¹⁰ It is a dimeric enzyme very highly glycosylated (nine *N*-glycosylation sites) whose structure has been recently resolved.^{11,12} RPTP belongs to the family of class III secretory plant peroxidases and it contains one heme group and two calcium-binding sites in similar locations.

The structural stability of RPTP has been described to be pH-dependent.¹³ At pH 3, where ion pairs have disappeared due to protonation, the thermally induced denaturation of RPTP is irreversible and strongly dependent upon the scan rate, suggesting that this process is under kinetic control. Moreover, thermally induced transitions at this pH value are dependent on the protein concentration, allowing it to be concluded that in solution RPTP behaves as a dimer, which undergoes thermal denaturation coupled with dissociation.¹³ The authors proposed the dimeric nature of the enzyme as one of the main factors responsible for the unusually high stability of RPTP. However, this dimeric nature may become a problem when the enzyme is used as a biocatalyst; as enzyme dissociation of an immobilized enzyme may lead to their operational inactivation (*via* washing of the released subunits).¹⁴

The enzyme has been used in diverse reactions, such as oxidation of luminol,¹⁵ a conducting complex of polyaniline and poly(2-acrylamido-2-methyl-1-propanesulfonic acid).¹⁶

In this paper, we have intended the immobilization of this highly stable enzyme for the first time in the literature. Due to their glycosylated (that may make complex an intense interaction with the surface of a support) and multimeric nature, we have decided to try the potential of the chemical crosslinking enzyme aggregates (CLEAs) proposed by Prof. Sheldon.^{17–20} This method has the advantage of not requiring the use of a support, being quite simple and having been described to be a good method to prevent dissociation of multimeric enzymes.²¹ The disadvantages are mainly related to diffusional problems (all the solid of the biocatalysts may be enzyme).²² Due to the complexity of the many variables that can have a relevant role in the final performance of the CLEA,²³ we decided to use the strategy of experimental design following a response surface methodology, to detect any kind of likely covariance that could exist, using as main parameter the optimization the CLEA activity.²⁴ This strategy has already shown the advantages in the design of CLEAs from other enzymes.²⁵ The final features of the optimized CLEA will be analyzed in terms of stability/activity at different pH values, effect of enzyme concentration on stability, stability on the presence of hydrogen peroxide, finally the reuse of the CLEA in the decolourization of methyl orange will be presented.

2. Materials and methods

2.1. Materials

Leaves of royal palm tree (*Roystonea regia*) were harvested in the territory of the state of Santander, Colombia. Only green leaves were used. Hydrogen peroxide (30 wt% in H₂O), poly(ethylene

glycol) (PEG) (MW 10 000) and ethanol were purchased from Merck. Guaiacol was from J. T. Baker. Glutaraldehyde and methyl orange were from Sigma-Aldrich. All reagents and solvents were of analytical grade.

2.2. Extraction of peroxidase from royal palm (RPTP) leaves

Peroxidase from royal palm leaves was extracted and partially purified as described by Sakharov *et al.*¹⁰ (see Table 1-S and Fig. 1-S†). The leaves of palm tree were washed with distilled water and milled. The samples obtained were divided in two equal portions. The first part was homogenized in 10 mM buffer phosphate at pH 6.0 (4 mL g^{−1}) and submitted to gentle stirring for 12 hours. The homogenate was filtered and used as extraction solution for the second portion, stirred for 12 hours, filtered and stored at 4 °C. The pellet was discarded. To remove pigments, PEG and (NH₄)₂SO₄ were added to a concentration of 14% and 10% (% w/v), respectively, to the solution obtained. The solution was stirred until homogenization and held at 25 °C until the formation of two phases. The dark phase was separated and discarded. The eluted containing active peroxidase was concentrated using Amicons ultra centrifugal filters with low-binding Ultracel membranes of 30 000 NMWL and centrifugation (5000×g; 15 min; 4 °C). The fraction containing peroxidase activity was collected and stored at 4 °C.

2.3. Standard determination of enzyme activity

This assay was performed by measuring the increase in absorbance at 470 nm produced by the release of tetraguaiacol in the oxidation of 18.2 mM guaiacol in 10 mM sodium phosphate at pH 6 and 25 °C (ϵ under these conditions is 5200 M^{−1} cm^{−1}) containing 2 mM of hydrogen peroxide. To start the reaction, a volume of 20–100 μ L of peroxidase solution or suspension was added to 2.5 mL of substrate solution. One international unit of activity (U) was defined as the amount of enzyme that oxidases 1 μ mol of guaiacol per minute under the conditions previously described. Protein concentration was determined using Bradford's method²⁶ and bovine serum albumin was used as the reference.

2.4. Cross linked enzyme aggregates (CLEAs) preparation

CLEAs were prepared according to Schoevaart *et al.*¹⁹ using ethanol, acetone or PEG for protein precipitation and glutaraldehyde as crosslinking agent.²⁷ A volume of 3 mL of protein precipitant at different concentrations (50, 70 or 90% v/v) was added to 0.3 mL of peroxidase solution (RPTP, 0.5 mg mL^{−1}) at 4 °C and constant stirring (magnetic stirring at 300 rpm). After 1 hour, glutaraldehyde was added to the desired concentration (0.5, 1.25 or 2% (w/v)) and the reaction mixture was incubated for 6, 12 or 18 h. CLEAs were centrifuged and recovered by centrifugation, washed with 25 mM phosphate buffer, and finally stored at 4 °C.

2.5. CLEAs preparation experimental design

A full factorial design (3³) with three variables varying at three levels was carried out in order to obtain the optimal conditions for

CLEAs preparation. Precipitant concentration (50–70% v/v), glutaraldehyde concentration (0.5–2.0% w/v) and reaction time (6–12 h) were evaluated. One experimental design was performed for each precipitant: ethanol, acetone and PEG. Table 1 shows the 27 experiments of each design. The runs were performed in a random order, but are presented in standard order in the tables.

2.6. RPTP thermal inactivation experiments

Solutions containing different concentrations of enzyme preparations were suspended in 10 mM of sodium citrate at pH 3 or sodium phosphate at pH 7 at different temperatures. Periodically, samples were withdrawn and the activity was measured using guaiacol as indicated above. Half-lives were calculated from the observed inactivation courses.

2.7. RPTP inactivation in the presence of hydrogen peroxide

Enzyme preparations were suspended in 10 mM of sodium citrate at pH 3 or sodium phosphate at pH 6 at different hydrogen peroxide concentrations (10 mM–1.2 M) at 25 °C. Periodically, samples were withdrawn and the activity was measured using guaiacol. Half-lives were calculated from the observed inactivation courses.

2.8. Operational stability

Methyl orange was prepared in 50 mM of sodium citrate at pH 3 or sodium phosphate at pH 6 to a final concentration of 45 μ M, containing hydrogen peroxide at different concentrations (5 or 225 mM). 4.6 U of CLEAs were suspended on dye solution and gently stirred for 4 hours at 25 °C. Spectrophotometrically dye degradation was scanned over a wavelength range of 250–650 nm. Standard calibration curve was prepared at maximum wavelength and used for the estimation of dye concentration in aqueous phase. Once the reaction was completed, the CLEAs were recovered from the reaction suspension mixture, washed with distilled water and used again in a fresh methyl orange solution.

3. Results

3.1. Optimization of the protocol of preparation of the peroxidase CLEAs

Initially, for the preparation of peroxidase CLEAs, three precipitant agents were evaluated: ethanol, acetone and PEG (MW 10 000). Precipitant concentration, glutaraldehyde concentration and reaction time were tested, for each one of these precipitant agents, by an experimental design. The matrix of these experiments and the results for each precipitant agent is presented in Table 1. In general, preparations using ethanol

Table 1 Experimental design for CLEA preparation

Run	Precipitant concentration (%)	Glutaraldehyde concentration (%)	Reaction time (h)	Specific activity (U mg ⁻¹)		
				Ethanol	Acetone	PEG
1	–1 (50) ^a	–1 (0.5)	–1 (6)	34	1	488
2	–1 (50)	–1 (0.5)	0 (12)	61	36	512
3	–1 (50)	–1 (0.5)	1 (18)	83	58	522
4	–1 (50)	0 (1.25)	–1 (6)	61	61	568
5	–1 (50)	0 (1.25)	0 (12)	244	178	592
6	–1 (50)	0 (1.25)	1 (18)	288	85	595
7	–1 (50)	1 (2.0)	–1 (6)	81	165	6
8	–1 (50)	1 (2.0)	0 (12)	295	669	183
9	–1 (50)	1 (2.0)	1 (18)	295	162	178
10	0 (70)	–1 (0.5)	–1 (6)	1700	229	301
11	0 (70)	–1 (0.5)	0 (12)	913	500	391
12	0 (70)	–1 (0.5)	1 (18)	904	124	426
13	0 (70)	0 (1.25)	–1 (6)	966	424	669
14	0 (70)	0 (1.25)	0 (12)	2000	318	1038
15	0 (70)	0 (1.25)	1 (18)	1927	282	1041
16	0 (70)	1 (2.0)	–1 (6)	1079	0	124
17	0 (70)	1 (2.0)	0 (12)	600	59	90
18	0 (70)	1 (2.0)	1 (18)	780	20	61
19	1 (90)	–1 (0.5)	–1 (6)	1018	4	1301
20	1 (90)	–1 (0.5)	0 (12)	1476	75	1355
21	1 (90)	–1 (0.5)	1 (18)	502	40	1459
22	1 (90)	0 (1.25)	–1 (6)	1948	91	1724
23	1 (90)	0 (1.25)	0 (12)	1888	46	1997
24	1 (90)	0 (1.25)	1 (18)	478	7	1863
25	1 (90)	1 (2.0)	–1 (6)	459	117	11
26	1 (90)	1 (2.0)	0 (12)	323	51	5
27	1 (90)	1 (2.0)	1 (18)	449	19	8

^a Numbers in parenthesis are the real values for each variable.

Fig. 1 Effect of pH on the guaiacol activity of different peroxidase preparations. Activity was determined as described in Section 2. 100% relative activity was the maximum activity for each preparation. Circles: CLEAs, squares: soluble RPTP.

and PEG presented good activity. The soluble enzyme, after extraction, has 910 U mg^{-1} ; the highest CLEAs activity was found using high concentrations of precipitant agent (70 or 90%), where it was possible to obtain a specific activity two-times higher than the soluble enzyme (runs 22 and 23). However, the immobilization yield (comparing initial enzyme units and final immobilized units) was around 75% using ethanol. There are some likely explanations for this discrepancy. First, the yield may be not 100% just because some enzyme molecules may be not precipitated (we have detected around 7% of the RPTP activity in the supernatant) or because no all CLEAs were recovered (e.g., very small particles may be lost during elimination of the supernatants after centrifugation). Second, the specific activity using the free enzyme is based in an indirect determination of enzyme concentration, and that may give no a no-real protein concentration value, while CLEA is actually weighted. Moreover, even if the enzyme accounts for more than 50% of the total protein in the crude (see Fig. 1-S[†]), the enzyme may be partially purified during the

immobilization if certain selectivity in the target protein precipitation is achieved. In any case, even although the comparison with the free enzyme may be unreliable, the comparison between CLEAs activities should be a real one. And a recovered activity of 75% considering the high diffusion problems of this kind of immobilization protocol may be considered very successful.

Using acetone, a color change was observed in the reaction medium, probably due to the formation of the Schiff's base, the reaction product between the ϵ -amino groups of Lys residues and the reactive groups of glutaraldehyde.²⁸ The CLEAs prepared using acetone presented lower activity than the soluble enzyme. Thus, acetone was discarded as precipitant agent for preparation of peroxidase CLEAs.

The statistical analysis for the preparations using ethanol and PEG can be observed in the Pareto charts, at a significant level of 0.1, presented in Fig. 2-S and 3-S,[†] respectively. Using ethanol as precipitant agent, among the main effects (linear effects) only the precipitant concentration was statistically significant, with a positive effect, which means that the higher the concentration, the higher the activity, as mentioned before. Using PEG, precipitant concentration and glutaraldehyde concentration were statistically significant, but with opposite effects. While precipitant concentration was positive, glutaraldehyde concentration was negative, *i.e.* increasing its concentration the CLEA activity decreased. The relationship between the variables is presented in the response surface plots in the Fig. 4-S and 5-S,[†] for ethanol and PEG, respectively. Observing the contour plots for ethanol as precipitant agent, it can be seen that the optimal conditions to prepare peroxidase CLEAs is ethanol concentration of 80%, glutaraldehyde concentration of 1% and a reaction time of 12 h. Whereas using PEG as precipitant agent, the optimal conditions were PEG concentration of 90%, glutaraldehyde concentration of 0.9% and reaction time of 15 h. In both cases, it was possible to obtain very high specific activities, higher than the soluble enzyme.²⁹ However, due to the lower cost of ethanol and the slightly higher activity obtained using this precipitant agent (2011 U mg^{-1} versus 1912 U mg^{-1} – predicted by the models), ethanol was chosen as precipitant agent for peroxidase CLEAs preparation. Optimal conditions using ethanol enabled a recovered activity of 77%.

Fig. 2 Thermal stability of the different peroxidase preparations under different conditions. Other specifications are described in Section 2. Panel A: thermal inactivation at 65°C and pH 3. Panel B: thermal inactivation at 90°C and pH 7. Full circles: 1.2 U of CLEAs, empty circles: 0.6 U of CLEAs, full squares: 1.2 U of RPTP, empty squares: 0.6 U of RPTP.

Fig. 3 Hydrogen peroxide stability of the different peroxidase preparations under different conditions. Other specifications are described in Section 2. Panel A: inactivation at pH 3. Panel B: inactivation at pH 7. Circles: CLEAs, squares: RPTP.

3.2. Characterization of the peroxidase CLEAs compared to the free enzyme

3.2.1. Activity/pH profile of the free and peroxidase CLEAs.

Fig. 1 shows the activity/pH profile of both samples of peroxidase. The free enzyme has a clear maximum activity at pH 7, with a rapid activity drop at basic or acidic pH values. The CLEA has maximum activity at pH 6, and the activity drop at alkaline pH values is similar to that experimented by the free enzyme, however at acidic pH value the enzyme retained much higher activity. At pH 3, the immobilized peroxidase exhibited around 40% of the maximum activity, while the free enzyme is almost fully inactive. This way, the range of likely pH values to use this enzyme is greatly increased after immobilization.

3.2.2. Stability at different pH values. This enzyme has been reported to be very thermostable.¹⁰ It has been proposed that its very high thermostability may be related to the dimeric nature of the enzyme.^{11,12} On the other hand, it has been reported that in certain cases, the inactivation of multimeric enzymes starts *via* subunit dissociation¹⁴ and this may be a problem for the industrial use of diluted samples of this kind of enzymes. Fig. 2a shows the inactivation course of free enzyme and CLEA at two different concentrations, at pH 7 and 90 °C.

The figure confirms the very high stability of the enzyme (that remained fully active after 3 h at 70 °C, results not shown). The half-lives of both CLEA and free enzyme (50 min) are very similar and did not significantly depend on the concentration of the enzyme, suggesting that under these conditions the enzyme is not dissociated before becoming inactivated. However, at pH 3 and 65 °C the situation is fairly different (Fig. 2b). First, CLEA preparation is much more stable than the free enzyme. Second, the free enzyme is less stable if the concentration decreased. This suggested that at pH 3, the first step of the inactivation of the free enzyme is the enzyme subunit dissociation, and the CLEA immobilization is able to fully prevent this dissociation because it involves all enzyme subunits.²¹

3.2.3. Stability in the presence of hydrogen peroxide. Hydrogen peroxide is a reagent that may rapidly inactivate enzymes by chemical modification of different groups, but in this case it is also a substrate of the enzyme.⁶ Therefore, the enzyme needs to be resistant to this reagent to be used at industrial level, or may be used in more sophisticated reactor configurations or generating the hydrogen peroxide *in situ* (e.g., using an oxidase).⁷ Fig. 3 shows that the free peroxidase is very unstable at 300 mM hydrogen peroxide and 25 °C at both pH 7 and 3 (half-lives of 130 minutes at pH 7 and 20 minutes at pH 3), the immobilization using CLEA technology allows to greatly improve enzyme stability (half-lives of 1060 and 450 minutes at pH 7 and 3, respectively). The stabilization is higher at pH 3 (perhaps by preventing the dissociation of the enzyme subunits,

Fig. 4 Effect of hydrogen peroxide concentration on the half live of the immobilized enzyme. Other specifications are described in Section 2. Circles: pH 3, rhombus: pH 6.

Fig. 5 Effect of H₂O₂ concentration on methyl orange destruction with the immobilized enzyme at pH 6. Other specifications are described in Section 2. Circles: 225 mM, rhombus: 5 mM.

Fig. 6 Reusability of CLEAs on methyl orange destruction. Other specifications are described in Section 2. Circles: 225 mM at pH 6, rhombus: 5 mM at pH 6, triangles: 225 mM at pH 3.

that may expose more enzyme surface to the deleterious action of the H_2O_2 , but the CLEA is still more stable at pH 7 than at pH 3. Fig. 4 shows the effect of H_2O_2 concentration on the half live of the immobilized enzyme. While at concentrations under 10 mM H_2O_2 the enzyme remained fully active after 10 h, at 300 mM the half-live is only 7.5 h and using 1.2 M is just over 4 h.

3.3. Operational stability

Fig. 5 shows the peroxidase-CLEA catalyzed destruction of 45 μM methyl orange using 5 or 225 mM hydrogen peroxide at pH 6. Using 225 mM hydrogen peroxide, the conversion is near 100% after 4 h. Using 5 mM hydrogen peroxide, conversion is around 50% after 1 h, and hardly increased if the time is prolonged to 4 h. To measure the operation stability under both conditions, we decided to use as 100% the decoloration values obtained at 3 h (225 mM H_2O_2) or 1 h (5 mM H_2O_2), but using cycles of 4 h (that is, after 4 h the enzyme was recovered and reused) in both cases to have comparable reaction cycle-time (Fig. 6). While using 225 mM H_2O_2 at pH 6 the conversion at 3 h were reduced from 85% to 60% in 4 cycles, using 5 mM H_2O_2 the enzyme remained fully active after the 4 cycles (Fig. 6). At pH 3 and using 225 mM H_2O_2 , conditions where the free enzyme was fully inactive (Fig. 1) and with low stability (Fig. 2), the immobilized enzyme suffered a progressive decrease in enzyme activity after each cycle, going from a elimination of 55% in the first cycle (significantly lower than at pH 6, according to the lower activity at this pH value), to only a 10% in the fourth cycle. However, it is remarkable that we have been able to prepare a biocatalyst that may be used several cycles under conditions where the free enzyme is fully inactive.

4. Conclusions

This paper details the optimization of the preparation of CLEAs of the dimeric peroxidase from *Roystonea regia*. The final recovered activity was 77% of the initial one, a very high value considering the diffusion problem of these preparations and the difficulty in fully recovering all the solid. These CLEAs have permitted to fully prevent the enzyme dissociation that occurred at pH 3 and high temperature. Thus, while at pH 7 the RPTP stability observed after the CLEA preparation is only marginally higher than that of the free enzyme, at pH 3 the

stabilization achieved is quite significant and depended on the concentration of the free enzyme (because this decreases when the enzyme concentration does). Nevertheless, the stability of the peroxidase-CLEAs remains much higher at pH 7 than at pH 3.

The free RPTP stability in the presence of low concentrations of hydrogen peroxide is very good, but if we used moderate hydrogen peroxide concentrations, the stability is not so good. The immobilization *via* the optimized CLEA protocol provide a significant stabilization in the presence of this reagent, but still the half live is relatively low for industrial purposes.

Thus, the RPTP-CLEA could be reused for 4 cycles without any loss of activity at pH 6 and using 5 mM of hydrogen peroxide, but removing only 50% of the color generated by 45 μM of methyl orange. Use of higher concentrations of hydrogen peroxide permitted a full color removal, but the enzyme decreased the activity in a significant way each reaction cycle. Thus, further efforts to have more stable RPTP biocatalysts seem convenient to increase its prospects as industrial biocatalyst.

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