

Real Time Optimization of the Sterilization Process in a Canning Industry

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C. Vilas*, A.A. Alonso

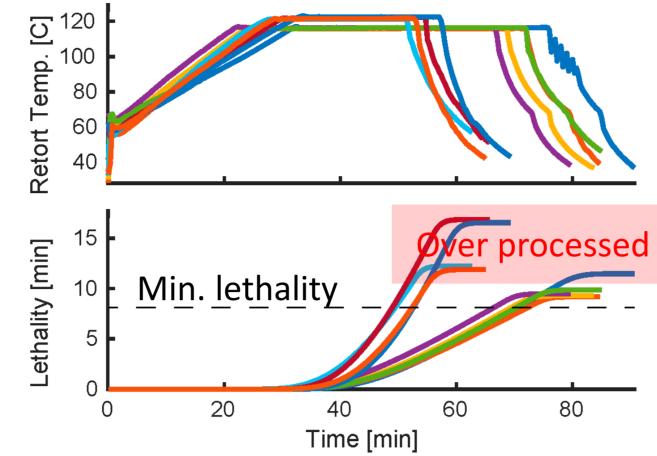
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(Bio)Process Engineering Group, Marine Research Institute, IIM-CSIC, Vigo (Spain) E-mail: carlosvf@iim.csic.es

MOTIVATION AND OBJECTIVE

Sterilization process is aimed to inactivate harmful microorganisms present in food. Drawbacks:

- It is a demanding operation in terms of energy and time consumption.
- It adversely affects food quality [1].
- Plant perturbations may lead to food safety/quality problems [2].

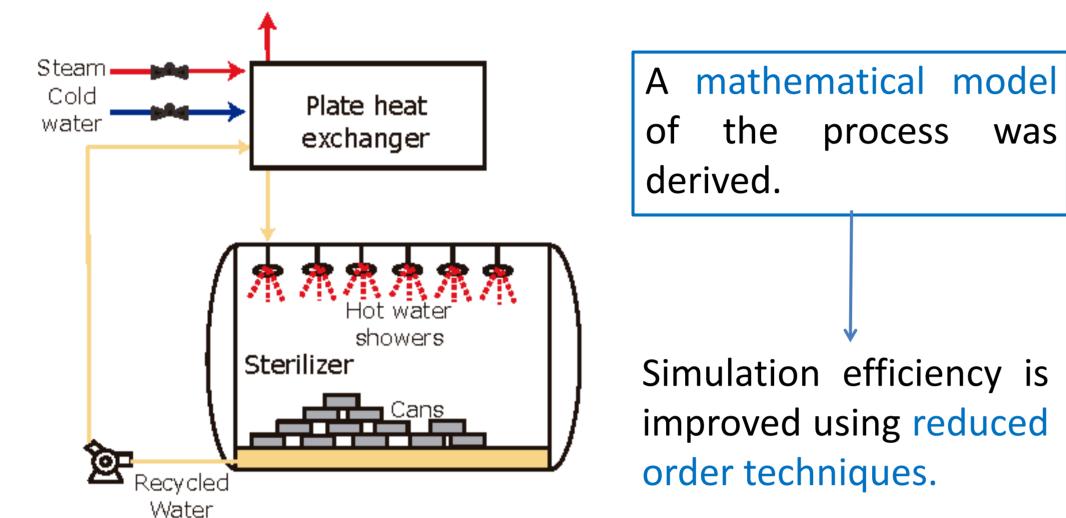


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Objective: To design a model-based RTO strategy able to correct the influence of unexpected perturbations.

- Food safety/quality, process time and energy consumption are taken into account.
- Food quality refers to surface color.
- Food safety refers to microbial lethality (F0).

PROCESS AND RTO SCHEME



The RTO Scheme

- Temp. set point and process time are fixed at the beginning.
- The mathematical model combined with on-line plant measurements is used to assess final product safety.
- If the model predicts safety problems a new Temperature set point is computed through optimization.

Simulation efficiency is improved using reduced

The sterilization process

- Cold water is heated with steam using a plate heat exchanger (PHE). •
- Hot water from PHE is introduced in the sterilizer. \bullet
- Food cans are heated at a given T during an amount of time. ullet
- Cold water is introduced at the end to cool down the food cans.

RESULTS AND DISCUSSION

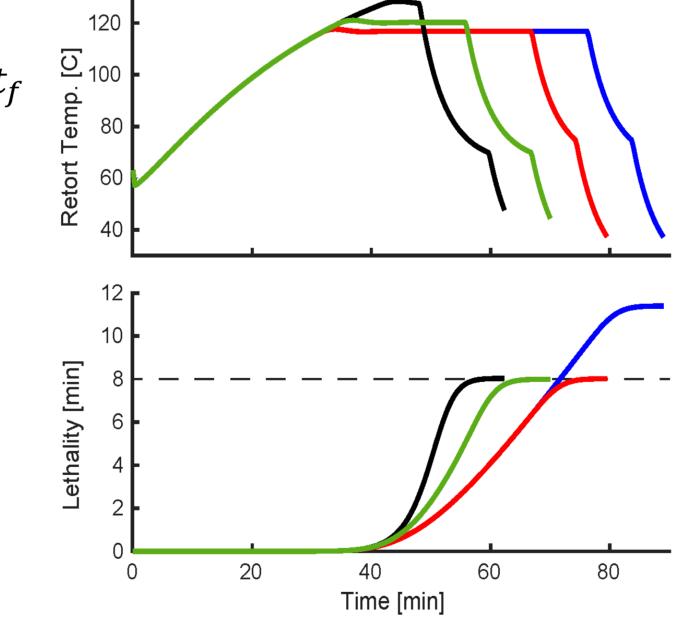
Optimization problem:

$$\min(J) = w_1 E + w_2 \left(100 - C(t_f) \right) + w_3 t_f$$

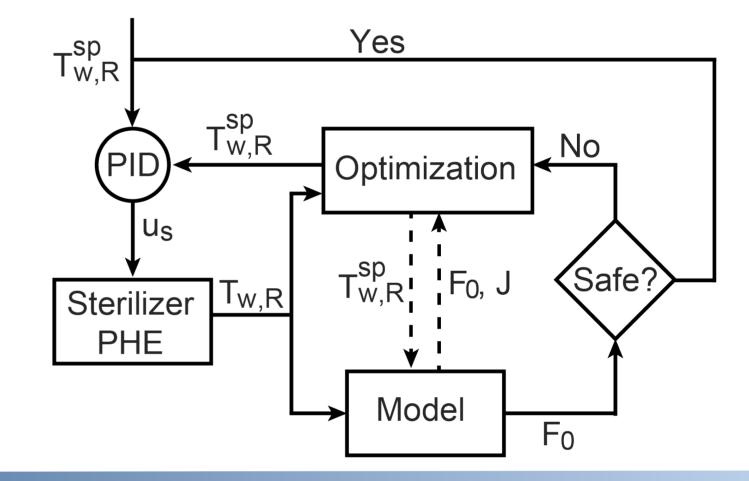
Subject to:

- Model equations
- 110 °C $\leq T_{w,R} \geq 130$ °C
- $F_0(t_f) \ge 8 \min$

Improvement (in %) of the RTO profiles with respect a real implemented profile (blue line)



- The optimal profile is implemented in the plant.
- Constant profiles were considered (legislation issues).



Three profiles were obtained:

- In RTO1 (red line), only process time was ● allowed to change. It improves the original profile in all senses (time, energy and color).
- In RTO2 (black line) temperature was also allowed to change. It is the most aggressive and the shortest one. It provides the best color and the largest energy consumption.

| | Energy | Color | Time |
|------|--------|-------|------|
| RTO1 | 2,7 | 2,8 | 10,7 |
| RTO2 | -5,7 | 8,0 | 30,0 |
| RTO3 | 1,3 | 5,7 | 21,1 |

Blue line: Batch implemented in a real canning plant (over processed)

In RTO3 profile (green line) weights in J ulletchanged. It improves the process in all senses allowing to reduce cycle time.

CONCLUSIONS

- Typical sterilization cycles in the canning industry are conservative and lead to food overprocessing (particularly in the event of unknown perturbations).
- The RTO approach allows: \bullet
 - o designing cycles that ensure food safety while optimizing food quality and process costs.
 - taking into account unexpected process disturbances to minimize their effects.
- Larger improvements are expected using variable retort temperature (VRT) profiles instead of constant ones.

REFERENCES

[1] A. A. Teixeira, G. S. Tucker (1997). On-line retort control in thermal sterilization of canned foods. Food Control, 8:13-20.

[2] A. A. Alonso, et al (2013). Real time optimization for quality control of batch thermal sterilization of prepackaged foods. Food Control, 32(2):392–403, 2013.

ACKNOWLEDGEMENTS

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