1	Stability and catalytic properties of nanostructured carbons in
2	electrochemical environments
3	S. Pérez-Rodríguez ^{a,1} , D. Sebastián ^a , M.J. Lázaro ^{a*} , E. Pastor ^{b*}
4	
5	^a Instituto de Carboquímica (CSIC), Miguel Luesma Castán 4, 50018 Zaragoza, Spain.
6	^b Universidad de La Laguna, Dpto. Química-Física, Avda. Astrofísico Francisco
7	Sánchez s/n, 38071 La Laguna (Tenerife), Spain.
8	
9	
10	¹ Present address: Centre Tecnològic de la Química de Catalunya (CTQC) Marcel·lí
11	Domingo s/n, 43007 Tarragona, Spain.
12	* Corresponding author:
13	M.J. Lázaro: Tel.: +34 976733977; Fax: +34 976733318; E-mail address:
14 15	mlazaro@icb.csic.es E. Pastor: Tel.: +34 92231 8071; Fax: +34 922318002; E-mail address: epastor@ull.es.
16	E. 1 astor. 101. +34 72231 6071, 1 ax. +34 722316002, E-mail address. epastor @ un.es.
17	
18	
19	
20	
21	
22	
23	
24	
25	

26 Abstract

27 This work reports a study of the electrocatalytic properties and stability of 28 nanostructured carbon electrodes by on-line differential electrochemical mass 29 spectrometry (DEMS). A wide electrochemical characterization in 0.1 M NaHCO₃ 30 involving anodic (carbon corrosion and oxygen evolution reaction, OER) and cathodic 31 (CO₂ reduction and hydrogen evolution reaction, HER) key reactions in energy-32 conversion devices was performed. DEMS studies showed that the faradaic current from 33 1.3 to 1.6 V vs. RHE of carbons was only associated to CO₂ formation by corrosion and 34 not to OER, the stability being improved by the graphitic character of carbon. H₂ 35 evolution was also enhanced with graphitic carbon nanofilaments, even though metal 36 traces might positively influence their catalytic activity. By comparison of the faradaic 37 currents and the H₂ formation signals, in the absence and presence of CO₂, a high 38 inhibition of the HER was established for all carbon electrodes due to the species 39 adsorption from CO₂ reduction.

40

41 Keywords: Nanostructured carbons, DEMS, corrosion, O₂ evolution, H₂ evolution, CO₂
42 electroreduction.

44 **1. Introduction**

45 Noble metals or metal oxides supported on carbon materials are conventionally
46 used as catalysts in renewable energy conversion and storage devices, for example in
47 polymer electrolyte membrane (PEM) fuel cells and metal-air batteries [1-7].

48 The commercial carbon black Vulcan XC-72R (supplied by Cabot) is the most 49 commonly used material in the field of electrocatalysis because of their adequate 50 mesoporous distribution and good electrical properties [4, 8]. However, much research 51 effort has been made using advanced nanostructured carbon materials (NCMs) over the 52 last decades, such as graphenes [1], carbon nanotubes (CNTs) [3, 9, 10], carbon 53 nanofibers (CNFs) [3, 11], carbon nanocoils (CNCs) [12, 13], carbon xerogels (CXs) 54 [14, 15], carbon nanocages [5] and ordered mesoporous carbons (OMCs) [2]. These 55 materials offer optimal textural and chemical features which lead to an enhanced 56 performance. For example, OMCs and CXs provide a high surface area and a developed 57 mesoporosity which is essential for achieving a good dispersion of metal nanoparticles 58 and to favour the diffusion of reactants and by-products. Another key specification is 59 the stability of the carbon material since carbon-support corrosion is considered to be 60 one of the main problems facing the performance of fuel cells [16-20]. Also, a high 61 electrical conductivity is required to facilitate electron transfer [3, 4, 14]. In order to solve these issues, more graphitic carbons (e.g., CNTs and CNFs) have been used [3, 9, 62 63 10].

64 Carbon-supported catalysts have been also used in the electrochemical reduction 65 of CO₂ obtaining promising results [21-25]. An enhanced activity was reached on these 66 carbon-based electrocatalysts in comparison to massive metal electrodes, which may be 67 explained by a better distribution of CO₂ on the active surface. However, few efforts 68 have been made involving advanced NCMs [26-28].

69 On the other hand, the use of carbon electrodes for electrochemical energy 70 conversion and storage applications has received special attention during the last years 71 [6, 24, 29-37]. In this context, Zhang and coworkers [6] obtained good electrocatalytic 72 properties for both oxygen reduction and evolution reactions on a N,P-doped 73 mesoporous carbon foam. On the other hand, Wu et al. [36] reported high Faradaic 74 efficiencies (up to 90%) for CO_2 reduction to ethylene and ethanol on nanometre-size 75 N-doped graphene quantum dots. Finally, the hydrogen evolution reaction (HER) has 76 been also recently studied on carbon electrodes obtaining promising results [32, 37].

77 The electrochemical behaviour of carbon materials for energy-conversion 78 applications has been evaluated in detail using conventional electrochemical techniques, 79 as cyclic voltammetry or chronoamperometry [1, 8, 20, 37-42]. However, these 80 measurements do not allow distinguishing between the current signals associated with 81 the production of different species at the electrode surface in the same potential region. 82 For example, oxygen evolution reaction (OER) by water oxidation takes place at 83 potentials above 1.23 V vs. RHE, and consequently, it is accompanied by carbon 84 corrosion. In contrast, the hydrogen formation is a competitive reaction, which occurs 85 during the CO₂ reduction in aqueous electrolytes. This limitation can be resolved by 86 using differential electrochemical mass spectrometry (DEMS), coupling on-line an 87 electrochemical cell to a mass spectrometer. In this way, DEMS allows simultaneously 88 following the electrochemical properties of electrodes and the volatile and gaseous 89 species generated on the electroactive surface, with excellent sensitivity and under 90 potential control. Therefore, DEMS is a powerful in situ tool to investigate the 91 electrochemical behaviour of carbon materials and to elucidate the reaction pathways 92 taking place [16, 17, 21, 43, 44]. But this technique is not commercial and the DEMS 93 configuration has to be adapted for every application.

94 In this work, the electrochemical stability and catalytic behaviour of various 95 nanostructured carbons has been established by DEMS. In particular, OMCs, two types 96 of graphitic carbons, CNFs and CNCs, and the commercial carbon black Vulcan XC-97 72R, have been used. Different cathodic and anodic electrochemical processes have 98 been studied: capacitive properties, tolerance to corrosion and activity toward HER and 99 OER. Furthermore, carbons have been tested in the electrochemical reduction of CO₂. 100 To the best of our knowledge, it is the first work reporting an extensive study of the 101 electrochemical properties and stability of different nanostructured carbons by in-situ 102 electrochemical mass spectrometry.

103

104 **2. Experimental**

105 **2.1 Synthesis of nanostructured carbon materials**

106 OMCs were prepared by the nanocasting technique using a mesoporous silica 107 (SBA-15) as template and a furan resin/acetone as carbon precursor. Finally, OMCs 108 were washed with 1.1 M NaOH in order to remove the silica particles [22, 45].

109 CNFs were synthesized by methane decomposition at 700 °C over a NiCuAl₂O₃ 110 (atomic ratio 78:6:16) catalyst. After CNF synthesis, the metal particles were removed 111 by means of an oxidation treatment with concentrated nitric acid (65 wt%, Panreac) at 112 room temperature for 2 h [11, 22].

113 CNCs were prepared by the catalytic graphitization method using Ni and Co 114 nitrates as graphitization catalysts, a mixture of resorcinol and formaldehyde as the 115 carbon precursor and silica sol to generate mesoporosity. Obtained CNCs were first 116 washed with 1.1 M NaOH (98 wt%, Panreac) solution to remove the silica particles, and 117 subsequently treated with concentrated nitric acid (65 wt%, Panreac) at room 118 temperature for 2 h for eliminating the metal content [22, 46].

In addition to the removal of metal nanoparticles, the treatment with nitric acid led to the creation of a low concentration of oxygen functionalities on CNFs and CNCs, especially carbonyl/quinone groups (see Supporting Information; Tables S1 and S2). The treatment at low temperature was selected to preserve the original structure of nanofibers and nanocoils while removing the non-encapsulated metal [46-48].

124 **2.2 Physicochemical characterization**

Transmission electron microscopy (TEM) micrographs of the NCMs were obtained using a JEOL-2000 FXII microscope equipped with a LaB6 gun at 200 kV and with a spatial resolution of 0.28 nm. To obtain the micrographs, the samples were finely grinded and ultrasonically dispersed in ethanol. A drop of the resultant dispersion was deposited and dried onto a standard copper grid coated with Lacey carbon.

130 X-ray diffraction (XRD) patterns of the materials were recorded using a Bruker 131 AXS D8 Advance diffractometer with a θ - θ configuration and with Cu K α radiation.

 N_2 adsorption-desorption isotherms of the NCMs were measured at -196 °C using a Micromeritics ASAP 2020. The total surface area was calculated from BET (Brunauer, Emmett and Teller) equation and the total pore volume was determined using the single point method at $P/P_0 = 0.99$. V_{meso} and average pore sizes (D_p) were obtained from the analysis of the desorption branch of the N_2 isotherm using the BJH (Barrett, Joyner and Halenda) method.

138 Thermogravimetric analyses (TGA) were carried out on a thermogravimetric 139 SETARAM Setsys Evolution under air atmosphere. The temperature was varied 140 between room temperature and 950 °C with a heating rate of 5 °C min⁻¹.

141 Temperature programmed desorption (TPD) experiments were carried out in an 142 AutoChem II 2920 apparatus to determinate the amount of surface oxygen groups on 143 carbon materials. The profiles of desorbed CO and CO₂ were obtained in a quartz

reactor heated under a constant flow of Ar (50 mLmin⁻¹) at a heating rate of 10 °Cmin⁻¹ 144 145 up to 1000 °C. The amounts of CO and CO₂ desorbed from the carbon samples were 146 analyzed online by mass spectroscopy. The total amount of CO and CO₂ released was calculated by integrating the area under the flow rate versus time curve. Furthermore, 147 148 the ratio CO/CO₂ was obtained as a measure of the surface acidity. The deconvolution 149 of TPD profiles was performed using a multiple Gaussian function and a non-linear 150 least-squared optimization procedure based on the Levenberg-Marquardt algorithm 151 using the software Fytik and assigning as initial estimate distinct desorption 152 temperatures for each group [49, 50]. The CO and CO₂ evolution and the deconvoluted TPD profiles are shown in the Supporting Information (see Figures S1 and S2). 153

154 X-ray photoelectron spectroscopy (XPS) analyses were carried out with an 155 ESCAPlus OMICRON system equipped with a hemispherical electron energy analyser. 156 The spectrometer operated at 150 W (15 mA, 10 kV), using a non-monochromatized MgKa (1253.6 eV) anode and under vacuum ($< 5 \cdot 10^{-9}$) over an area of sample of 157 158 1.75×2.75 mm. A survey scan (1sweep/200 ms dwell) was acquired between 0 and 1100 159 eV, at 0.5 eV step, 0.2 s dwell and 50 eV pass energy. Detailed scans for C 1s and O 1s 160 were obtained at 0.1 eV step, 0.5 s dwell and 20 eV pass energy. For calibration 161 purposes, the C 1s binding energy of the graphitic peak (BE) was referenced at 284.6 162 eV. C and O content was calculated from the corresponding peak areas divided by the 163 appropriate sensitive factors (1.00 for C 1s and 2.85 for O 1s) using the CASAXPS 164 software after Shirley background subtraction. Figure S3 shows the survey XPS spectra 165 and C1s and O1s regions for a selected sample: Vulcan XC-72R.

166 Elemental analysis (EA) of carbon materials were performed in a CHNS-O167 Analyzer Thermo FlashEA 1112.

Inductively coupled plasma atomic emission spectroscopy (ICP-AES) were performed on a Jobin Ybon 2000 spectrometer to determine the silica and metal residues in the carbon matrixes (Table S3).

171

172 **2.3. Electrochemical and spectro-electrochemical characterization**

173 Spectro-electrochemical measurements were carried out at room temperature 174 and atmospheric pressure in a three electrodes electrochemical cell directly attached to a 175 mass spectrometer (Balzers Omnistar quadrupole mass spectrometer), with a Faraday 176 cup detector. The potentiostat-galvanostat was an Autolab PGSTAT302 (Ecochemie). 177 Further details about DEMS set-up can be found elsewhere [51]. A high surface area 178 carbon rod was used as counter electrode, whereas an Ag/AgCl/3M KCl electrode (0.21 179 V vs. normal hydrogen electrode, NHE) placed inside a Luggin capillary was employed as reference. Unless otherwise specified, all potentials in the text are referred to the 180 181 reversible hydrogen electrode (RHE). The working electrode was prepared depositing a 182 thin-layer of the corresponding carbon over a glassy carbon (GC) susbtrate (7.0 mm of 183 diameter, SIGRADUR® G). Carbon suspensions were prepared by mixing 2 mg of the 184 sample, 15 µL of Nafion dispersion (5 wt%, Aldrich) and 500 µL of ultrapure water 185 (Millipore Milli-Q system). The suspension was sonicated for 90 min before deposition. 186 The Nafion content of the carbon thin-film was selected on the basis of previous works 187 for a convenient attachment of NCMs to the electrode surface, but not leading to 188 extensive surface blocking [52]. The capacitance of nanocarbon materials was 189 calculated from the charge in the region 0.3-0.8 V vs. RHE in the base electrolyte by 190 considering the averaged value from positive and negative going scans of cyclic 191 voltammetry performed from -0.1 to 1.6 V vs. RHE.

192 DEMS experiments were carried out in a 0.1 M NaHCO₃ (Merck, p.a.) 193 electrolyte solution deaerated with Ar (pH = 8.4). An aliquot of 10 μ L of the carbon ink 194 was deposited onto the carbon disk and dried to room temperature before every 195 electrochemical characterization, each performed with different potential windows. 196 Freshly prepared working electrodes were used for the capacitance properties and 197 corrosion behaviour on one hand, and the hydrogen evolution and CO₂ reduction on the 198 other hand. For the latter, CO₂ (99.99 %, Air Liquide) was bubbled into the electrolyte 199 for 30 min in order to obtain a CO_2 saturated 0.1 M NaHCO₃ solution (pH = 6.8) and 200 the performance of carbons for CO₂ reduction was established.

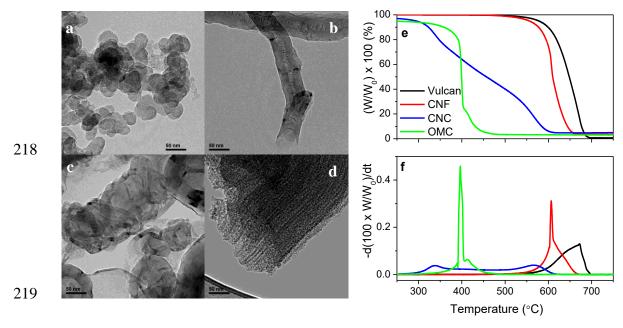
201

202 **3. Results**

203 **3.1** Physicochemical characterization of nanostructured carbon materials

The morphology of NCMs was studied by TEM (see Figure 1a-d). Vulcan is formed by an aggregation of spherical carbon nanoparticles composed of small crystallites. OMCs present an ordered structure, which consists of amorphous carbon nanorods with uniform mesopores. Finally, CNFs and CNCs show well-aligned graphitic layers, forming carbon nanofilaments with "fishbone" morphology or curved ribbons, respectively.

The crystalline structure of carbon materials was analysed by XRD. The diffraction patterns have been previously published and can be consulted elsewhere [22]. All the samples, with the exception of OMCs, showed a peak around $2\theta = 25^{\circ}$, which is associated with the graphite (002) diffraction. The relative intensity of the (002) peak, and hence, the graphitization degree of the carbons, increased in the order: Vulcan < CNCs < CNFs. Finally, OMCs did not show diffraction at $2\theta = 25^{\circ}$ due to the amorphous nature of carbon.



220

Figure 1. TEM images of (a) Vulcan, (b) CNF, (c) CNC and (d) OMC. TG profiles in air of carbon materials in terms of (e) weight percentage and (f) mass variation velocity as a function of the temperature.

224

225 Structural information of NCMs was deduced from TGA in air. Figure 1e shows 226 the TG profiles for all the carbon materials, while Figure 1f displays the rate of mass loss. Different TG profiles were found for the NCMs. OMCs and CNFs presented a 227 228 pronounced mass loss around 400 and 600°C, respectively, which is associated with 229 carbon combustion. OMCs displayed less oxidation tolerance due to their amorphous 230 character, while graphitic CNFs showed an improved condition toward combustion. In 231 contrast, two broad oxidation peaks centred at 338 and 567 °C were obtained in the 232 derivative curve vs. temperature (Figure 1f) for CNCs, indicating the presence of two 233 kinds of carbon phases with different nature: the first peak can be ascribed to the 234 oxidation of the amorphous phase, while the second one can be attributed to the 235 graphitic fraction. Finally, Vulcan presented the highest oxidation resistance with a 236 gasification temperature at 672 °C. Other authors have obtained similar results [53-56]. 237 As general trend, the oxidation temperature is higher as the carbon crystallinity 238 increases. Indeed, the synthetic materials follow this sequence. However, a lower 239 thermal stability would be expected for Vulcan. This behaviour could be explained by 240 the presence of sulphur groups (0.62 wt% from EA) which can increase the oxidation 241 resistance [57, 58]. Additionally, despite the low residual metal content of CNCs and 242 CNFs (below 1 wt% according to the results obtained by ICP (Table S3), it may act as 243 an oxidation catalyst, decreasing the onset temperature for the burn-off of these carbons 244 [47].

Textural properties of the NCMs were studied by N₂-physisorption and the results are summarized in Table 1. OMCs present the highest adsorption capacity whereas CNFs display the lowest surface area although with a significant mesoporosity (98% in terms of pore volume). On the other hand, the commercial carbon and CNCs show similar surface areas and mesopore contribution. Regarding the average pore size, Vulcan and CNFs exhibit larger pores (10-11 nm) than OMCs and CNCs (4 nm).

251

Table 1. Textural parameters of carbon materials: total BET surface area (S_{BET}), total pore volume (V_T), mesopore volume (V_{meso}), mesopore fraction (in terms of pore volume) and average pore diameter (D_p).

Sample	S _{BET} (m ² g ⁻¹)	V _T (cm ³ g ⁻¹)	V _{meso} (cm ³ g ⁻¹)	Mesopore fraction (%)	D _p (nm)
Vulcan	238	0.38	0.31	83	10.4
CNF	76	0.24	0.24	98	11.5
CNC	234	0.17	0.13	78	4.1
ОМС	812	0.55	0.31	57	3.8

256 TPD experiments provided a good insight on surface oxygen group distribution 257 of the NCMs. Table 2 shows the amounts of CO and CO₂ released, obtained by the 258 integration of the areas under the TPD peaks versus time, together with the oxygen 259 content (O_{TPD}, wt%). The number of oxygen atoms per surface area is also presented, 260 considering the S_{BET} obtained on the N_2 physisorption experiments (Table 1). Interestingly, CNCs and CNFs present high oxygen contents per surface area (11.0 and 261 262 3.7 atoms nm⁻², respectively) due to the creation of functional groups during the metal 263 removing treatment with nitric acid (see Supporting Information, Tables S1 and S2). 264 Although CNFs and CNCs were subjected to the same purification treatment, the 265 oxygen content for the former material was much lower (\sim 3 times in terms of O atoms 266 nm⁻²). In this context, CNFs present a low amount of defects due to their highly 267 graphitic character, leading to a low reactivity for the creation of oxygenated species.

268 The oxygen content was also determined by means of elemental analysis (EA) (Table 2, O_{EA}). This technique provides an oxygen content closer to the amount in the 269 270 samples considered as a bulk material. Results correlated quite well with the TPD 271 measurements, showing that the volatile matter of these samples corresponds with the 272 amounts of CO and CO₂ desorbed. However, an O_{TPD} amount of 4.8 wt% was obtained 273 on OMCs, while around 2 times more (8.4 wt%) was measured from EA. This 274 behaviour may be explained by surface groups in interior sites which are not desorbed at 275 1000 °C due to diffusion restrictions caused by the low pore size (4 nm) and the high surface area (812 m²g⁻¹) of this material. TPD allows determining only oxygen groups 276 277 that are desorbed during temperature variation, *i.e.* available for desorption [59], while 278 EA considers the whole sample. This means that almost half of oxygen groups present 279 in OMC are occluded in small or even blind/closed pores and did not desorb at 280 temperatures below 1000°C.

281 Finally, XPS was also used as a complementary method to obtain the surface 282 oxygen content (Table 2, O_{XPS}). Higher oxygen contents were determined by XPS for 283 all the materials in comparison to those obtained by TPD or EA. XPS is a surface 284 sensitive technique which accounts only for the elements a few nanometers close to the 285 analysis surface. In our case, carbon atoms in the bulk do not contribute to the XPS 286 signal. Thus, the general trend concerning higher O_{XPS} values compared to O_{TPD} and/or 287 O_{EA} indicates that oxygen functional groups are mainly present on the surface of 288 carbons and not in the carbon matrix, as expected.

The nature and the amount of surface oxygen functional groups were estimated from deconvolution of TPD profiles. Acidic groups (carboxylic and lactones) are decomposed into CO_2 at lower temperatures, whereas basic and neutral groups (phenols, quinones and carbonyls) are desorbed as CO at higher temperatures. Anhydrides originate both CO_2 and CO [49]. Table 3 summarizes the estimated distribution of oxygen functional groups obtained from the deconvolution of CO and CO_2 evolutions.

295

Table 2. Surface chemistry measured by TPD (total amount of CO and CO₂ released, CO/CO₂ ratio and total oxygen content), XPS (surface oxygen content) and EA (total oxygen content) of carbon materials. The number of oxygen atoms per surface area was obtained considering the total O_{TPD} and the S_{BET} from N₂ physisorption isotherms.

Sample	CO (µmol g ⁻¹)	CO2 (µmol g ⁻¹)	CO/CO ₂	Otpd (wt%)	O (atoms nm ⁻²)	OEA (wt%)	Oxps (wt%)
Vulcan	174	106	1.7	0.6	1.0	0.4	2.3
CNF	320	71	4.5	0.7	3.7	1.2	4.7
CNC	2602	832	3.1	6.8	11.0	6.8	9.3
OMC	1475	770	1.9	4.8	2.2	8.4	11.1

Sample	Carboxylic acid	Anhydride	Lactone	CO desorption	Phenol	Carbonyl/ Quinone
Vulcan	37	6	19	11	5	24
CNF	10	11	9	15	13	43
CNC	18	10	1	12	24	36
ОМС	27	15	4	11	21	23

303 peaks 1 and 2 of the CO_2 profiles.

304

305 A different oxygen functional group distribution was found for the NCMs. 306 Phenol and carbonyl/quinone groups were predominant for the materials subjected to 307 the purification treatment with nitric acid. These groups are generated during the 308 oxidation treatment with nitric acid, as it is shown in Supporting Information (Tables S1 309 and S2). In contrast, a large contribution of acid groups (carboxylic acids and lactones) 310 was developed for Vulcan and OMCs. In agreement with these results, a lower value of 311 the ratio CO/CO_2 (see Table 2) was obtained for the last materials (around 2). In 312 contrast, CNFs and CNCs presented high ratios (4.5 and 3.1, respectively), indicating an 313 enhanced surface basicity as a result of the purification treatment with HNO₃ [60].

314

315 **3.2** Electrochemical and spectro-electrochemical characterization

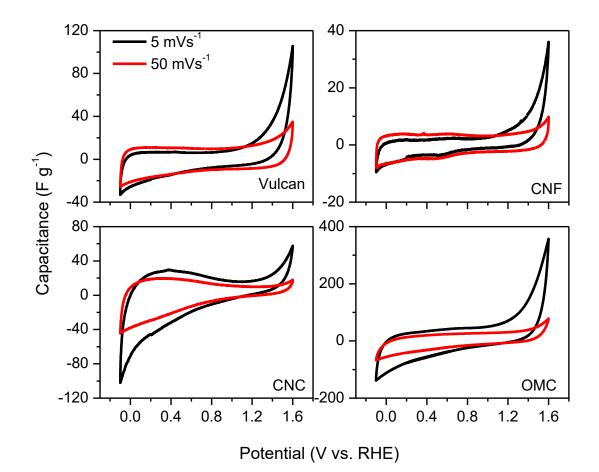
316 *3.2.1 Capacitance properties*

317 Cyclic voltammograms (CVs) were recorded at 5 and 50 mV s⁻¹ in 0.1 M 318 NaHCO₃ cycling the potential between -0.1 and 1.6 V vs. RHE. The specific 319 capacitance, *C*, was calculated from the correlation between current density, *i*, and the 320 variation of potential, E, with time, t, by using the Equation 1:

321 $i [A g^{-1}] = C [F g^{-1}] \cdot dE(V)/dt(s)$

(1)

322 where dE/dt is the scan rate, being constant in our experiments. The curves of specific 323 capacitance versus potential are given in Figure 2.



324

Fig. 2. CVs of carbon materials in 0.1 M NaHCO₃.

326

327 All carbon materials displayed a double-layer capacitive behaviour [61] together with anodic current rapidly increasing with high positive potential starting at about 1 V 328 329 vs. RHE. The latter is associated to irreversible reaction (carbon oxidation as will be 330 discussed in following sections) as indicated by differences between the two scan rates reported (5 and 50 mV s⁻¹). However, different profiles are evident from comparison of 331 332 the double layer currents and the behaviour at potentials approaching 0 V vs. RHE. 333 Capacitance values are summarized in Table 4, calculated from the averaged value in 334 the interval 0.3-0.8 V vs. RHE, where no carbon oxidation occurs. OMCs showed the

highest capacitance owing to their large specific surface area (812 m² g⁻¹), while CNFs 335 336 presented the lowest value in correlation with the low BET surface area of this carbon $(76 \text{ m}^2 \text{ g}^{-1})$. Indeed, the capacitance (Table 4, F g⁻¹) approximately follows the trend of 337 BET surface area (Table 1, m² g⁻¹). Furthermore, the graphitic character of CNFs 338 339 influences also the values of capacitance as charges are preferably accumulated on the 340 defects [61, 62]. In addition, a small pseudocapacitance contribution was observed on 341 CNCs and CNFs (0.4-0.7 V vs. RHE) associated with the reversible oxidation/reduction 342 of quinone groups generated during the oxidation treatment of the samples with nitric 343 acid [63], as was determined by TPD. This contribution was lower for CNFs due to the 344 smaller amount of oxygen per surface area. Interestingly, CNCs exhibited a dramatic 345 decrease of capacitance from about 0.5 V to 1.4 V vs. RHE, which may be related to the 346 porosity saturation as pointed out by Mysyk et al. [64]. They reported a decrease of the 347 double-layer current as a consequence of a porous volume not sufficiently developed, as 348 correlated to nitrogen physisorption ex-situ measurements.

In contrast, Vulcan and OMCs did not present pseudocapacitance as a higher contribution of acid groups (e.g. carboxylic acids and lactones), which are electrochemically inactive in the double layer region [65], was obtained for these materials (Table 3). OMCs showed higher ohmic resistance than the other NCMs, as envisaged from the positive slope of capacitance vs. potential, due to its amorphous character, leading to a low electrical conductivity.

- 355
- 356
- 357
- 358

Table 4. Electrochemical features of nanocarbon materials. Normalized ionic currents are referred to the m/z = 44, ascribed to CO₂ evolution.

Sample	Capacitance (F g ⁻¹)	Faradaic current at 1.5 V vs. RHE (A g ⁻¹)	Ionic current (m/z = 44) at 1.5 V vs. RHE (mA bar ⁻¹)	Normalized ionic current at 1.5 V vs. RHE (mA bar ⁻¹ F ⁻¹)	Normalized ionic current at 1.5 V vs. RHE (mA bar ⁻¹ O.wt% ⁻¹)
Vulcan	15	0.36	22.2	36.8	9.7
CNF	4	0.09	2.4	15.5	0.5
CNC	16	0.17	5.0	7.6	0.5
ОМС	24	0.38	32.4	34.0	2.9

361

362 Interestingly, redox couples associated with the formation/reduction of metal 363 surface oxides (which appear in this potential window as shown in [66]) were not 364 observed on CNFs and CNCs, confirming that the purification treatment with HNO3 365 was effective for removing metal impurities from the surface. In fact, the total metal 366 content obtained from ICP was below 1 wt% (see Table S3). In addition, Ni, Cu or Co impurities were not detected by XPS confirming that the surface amount was negligible. 367 368 Therefore, the residual metal load seems to be encapsulated in the carbon matrixes and 369 it is not accessible for the electrochemical reactions.

370

371 3.2.2 Carbon electrooxidation: CO₂ evolution

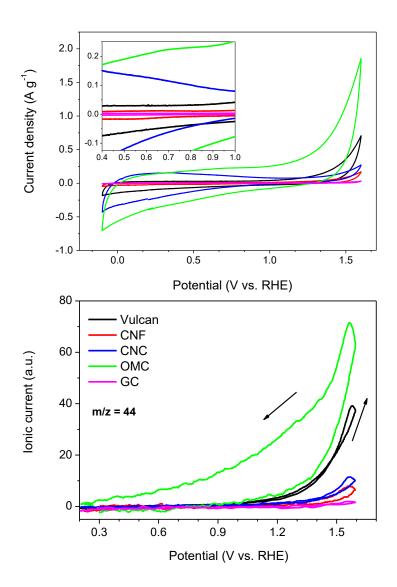
The anodic faradaic currents observed in the voltammograms of the NCMs (Figure 2, in the potential region from 1.3 to 1.6 V) could be associated with the oxygen evolution reaction (EOR) by water oxidation and/or the CO_2 evolution by carbon corrosion. OER is a key reaction in the air electrode of some batteries and electrolyzers, while carbon corrosion is considered to be one of the main problems facing the performance of fuel cells. Although the electrochemical oxidation of carbon-based electrodes has been widely studied [7, 29, 67], few works have used 379 spectroelectrochemical techniques [16, 18, 19, 68], which could provide a robust
380 strategy to design effective/stable catalysts.

In this work the performance of nanostructured carbon catalysts in the base electrolyte from -0.1 to 1.6 V was monitored by on line mass spectrometry following the mass signals associated to the formation of O_2 (m/z = 32) and CO_2 (m/z = 44) evolution reactions. The mass signal m/z = 32 did not present changes during the anodic scan showing that oxygen evolution does not take place on carbons at these potentials, and hence, the anodic faradaic currents (from 1.3 to 1.6 V) are only due to carbon oxidation.

388 Figure 3 shows a comparison of the CVs (upper panel) and the corresponding 389 mass spectrometric cyclic voltammograms (MSCVs) for CO_2 evolution (m/z = 44) of 390 the samples at 5 mV s⁻¹ in 0.1 M NaHCO₃. First of all, it has to be noted that the GC 391 used as substrate does not contribute significantly to the total faradaic and ionic (m/z =392 44) currents of the NCMs. As was expected, a decrease in the graphitic character of the 393 materials led to an increase of the CO₂ formation by corrosion following the sequence: 394 CNFs < CNCs < Vulcan < OMCs. This behavior is explained by differences in the 395 surface heterogeneity of the samples, and consequently, in the amount of surface 396 defects, as well as the surface area. On one hand, it is well known that the higher the 397 surface area the larger the amount of available labile carbon surface sites for carbon 398 oxidation. On the other hand, normalizing the ionic current (m/z = 44) by the 399 capacitance gives an indication of the carbon oxidation rate per unit of 400 electrochemically accessible surface area (Table 4), following the order CNCs < CNFs 401 < OMCs < Vulcan. Surface defects exhibit a higher activity for the adsorption of 402 oxygenated species, which may act as corrosion intermediates [68, 69]. Graphitic 403 materials (CNCs, CNFs) present reduced surface heterogeneity and low density of

404 surface defects, while non crystalline carbons (Vulcan, OMCs) develop a higher density 405 of active sites [68, 69]. Therefore, derived from a large surface area and a surface more 406 prone to oxidation due to its amorphous character, OMCs displayed the greatest 407 oxidation rate (A g^{-1}). In fact, this material presents the onset potential for CO₂ 408 evolution at 1.0 V vs RHE and the intensity of the mass signal m/z = 44 is several times 409 higher in comparison to those obtained on graphitic carbons (CNCs and CNFs). A 410 significant difference was also found in terms of oxygen speciation and CO₂ evolution 411 rate. Upon normalization of the ionic current (m/z = 44) per surface oxygen content 412 obtained by XPS (Table 4, O_{XPS}) the samples characterized by a high graphitization 413 degree show the lowest normalized ionic current, whereas OMCs and Vulcan, with 414 more labile oxygen groups like carboxylic acids or lactones (Table 3) exhibit larger 415 normalized ionic currents. This corroborates that the presence of more stable oxygen 416 groups, together with low surface area (e.g. CNFs), prevent carbon from 417 electrochemical oxidation.

418

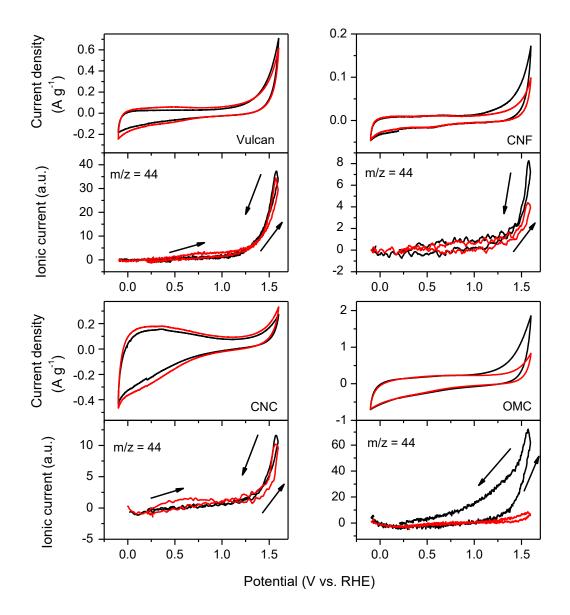


420

421 Fig. 3. CVs (upper panel) and MSCVs for CO₂, m/z = 44, (bottom panel) of carbon 422 materials in 0.1 M NaHCO₃ (v = 5 mV s⁻¹).

423

Subsequently, corrosion tests were carried out cycling 200 times the potential from 0.9 to 1.6 V at 50 mV s⁻¹. CVs were recorded between -0.1 and 1.6 V at 5 mV s⁻¹, before and after these experiments to evaluate the influence of surface oxidation on the electrochemical behaviour of NCMs. Simultaneously to the electrochemical analysis, DEMS measurements were performed following the formation of CO_2 (m/z = 44). CVs (upper panel) and MSCVs for m/z = 44 (bottom panel) can be observed in Figure 4,



431

432 **Fig. 4.** CVs (upper panels) and MSCVs for CO₂, m/z = 44, (bottom panels) of carbon 433 materials in 0.1 M NaHCO₃ (v = 5 mV s⁻¹). Black curves: prior to corrosion tests. Red 434 curves: after 200 cycles at 50 mV s⁻¹ between 0.9 and 1.6 V vs. RHE.

435

436 Results depend on the nature of the carbon material: CNCs and Vulcan 437 preserved the anodic current and the CO_2 formation at high potentials (1.3-1.6 V), 438 whereas a decrease of both faradaic and ionic (m/z = 44) currents was observed for 439 OMCs and CNFs. Although the origin of this different behaviour is not completely clear, it can be related to differences in the amount of oxygenated species of the NCMs
(Table 2) or in the textural properties (Table 1). According to bibliography [17, 70], a
high concentration of adsorbed species on the carbon surface facilitates the gasification
of carbon to CO₂ following the Equation 2:

444
$$C + H_2 O \rightarrow CO_2 + 2H^+ + 4e^-$$
 (E⁰ = 0.207 V vs. RHE) (2)

445 On the other hand, textural properties play also an important role. A high surface 446 area increases the probability of corrosion. Furthermore, a developed mesoporosity 447 favours the water interaction needed for the formation of oxygenated species, while 448 small pore sizes hinder H₂O diffusion to the active sites. In this context, Vulcan 449 presented a low amount of functional groups and a moderate surface area, and 450 consequently, similar corrosion currents (both faradaic and a CO₂ ionic current) for the first and the 200th cycle were recorded (Figure 4, upper left panel). In contrast, a high 451 content of O atoms nm⁻² was obtained on CNFs due to the treatment with nitric acid, 452 453 which may be responsible of the high anodic current related to CO₂ production obtained 454 in the first CV (Figure 4, black curve in upper right panel). In addition, although CNFs 455 exhibited the lowest surface area, they present a significant mesoporosity, which may 456 promote carbon corrosion.

In the case of OMCs, the noticeable current at potentials above 1.3 V in Figure 4
(black curve in bottom right panel) may be attributed to the high surface area of this
material and its amorphous character, which enhances carbon corrosion.

Finally, CNCs presented the highest oxygen content but similar corrosion currents during anodic cycling (similar CO₂ production after and before long-term corrosion test) (Figure 4, bottom left panel), which may be explained by their textural features. In fact, CNCs presented similar surface area and mesopore contribution than Vulcan and the same behaviour was obtained for both materials.

Future works will be designed using the identical location transmission electron microscopy with carbon based electrodes to get insights on morphology changes of NCMs upon potential cycling and carbon oxidation.

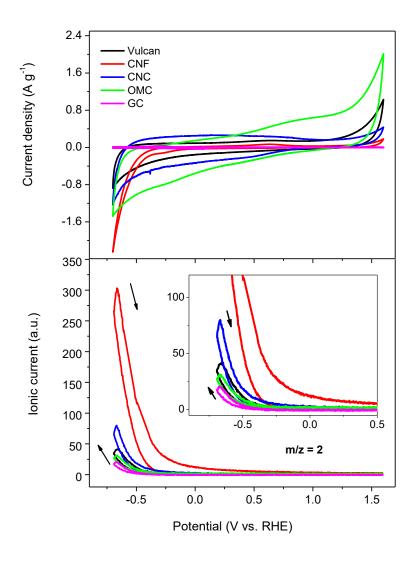
- 468
- 469

3.2.3 Catalytic activity towards the HER

470 At potentials below 0.0 V vs. RHE, the hydrogen evolution reaction (HER) takes 471 place by water reduction in aqueous electrolytes. H₂ evolution is a key reaction in 472 electrochemical energy conversion devices and a lot of works have studied the activity 473 of carbon-supported electrodes [71, 72]. However, the performance of carbon electrodes 474 has not been widely evaluated [32, 37]. In this work, the activity of carbon catalyst 475 based electrodes toward the hydrogen evolution was also evaluated by DEMS. CVs were recorded in the potential range from -0.7 to 1.6 V at 5 mV s⁻¹ in the base 476 477 electrolyte. Simultaneously, the mass signal associated with molecular hydrogen (m/z =478 2) was recorded (Figure 5).

479 It is observed that the HER was favoured in the following order OMC < Vulcan 480 < CNC << CNF. Indeed, a high faradaic current and a large H₂ production (about 15) 481 fold times more than the GC used as substrate) was obtained for CNFs with an onset 482 potential at -0.3 V. Conversely, Vulcan and OMCs presented low H₂ formation (more 483 similar to the GC substrate) in the selected potential range. This improved condition for 484 HER on CNFs and CNCs may be ascribed to their highly graphitic character and/or the 485 presence of metal impurities. It has been reported that delocalized π -electrons of 486 graphene layers act as Lewis bases adsorbing protons from solution and thus aiding the 487 evolution of hydrogen at lower overpotentials [73]. The influence of residual metal 488 impurities, even if below 1wt% according to results from ICP, cannot be discarded even 489 if metal appears encapsulated in the carbonaceous matrixes. Nevertheless, metal traces

490 were not detected by XPS analyses and the redox couples associated with the 491 formation/reduction of metal oxides were not detected in the CVs for CNFs and CNCs, 492 so the contribution of metal traces to the total current for application in high hydrogen 493 evolution devices (water electrolyzers) is expected to be low even if the turnover 494 frequency is much higher on metals, since the density of metal active sites is much 495 lower than the ones coming from graphene layers in these materials.



496

497 **Fig. 5**. CVs (upper panel) and MSCVs for H_2 , m/z = 2, (bottom panel) of carbon 498 materials in 0.1 M NaHCO₃ (v = 5 mV s⁻¹).

499

500 It is remarkable that, in the positive-going potential scan, a significant anodic

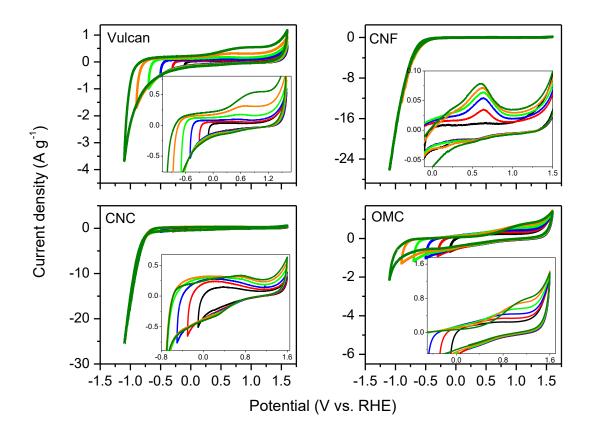
501 peak appears in the region from -0.2 to 1.2 V (Figure 5) for all NCMs, which is related 502 to hydrogen oxidation. It can be better observed by comparison of the voltammograms 503 in the potential region from -0.7 to 1.6 V and the blanks (see Figure S4). The high 504 overvoltage required for hydrogen oxidation suggests that hydrogen formed during the 505 cathodic excursion may penetrate inside the porous structure of the carbon bulk and be 506 retained (absorbed hydrogen) or be adsorbed. Then, during the anodic scan, this 507 hydrogen will be oxidized to protons. Several authors have obtained similar results [39, 508 74-76].

509 In order to study in detail the hydrogen absorption/adsorption capacity of the NCMs, several CVs were recorded at 5 mV s⁻¹ in the base electrolyte, with a stepwise (-510 511 0.2 V) shift of cut-off potential to more negative values down to -1.1 V. The obtained 512 curves are given in Figure 6. During the first cycling with the cut-off potential at -0.1 V, 513 only a typical charging of the double layer takes place for all the carbons. At potentials 514 below -0.5 V, the hydrogen absorption/adsorption and its posterior oxidation start to be 515 evident for all the samples. All the NCMs displayed higher currents for hydrogen 516 oxidation while shifting the cut-off potential to more negative values (see graphic insets 517 in Figure 6). However, differences in the potential location of the hydrogen oxidation 518 region were obtained.

519 Vulcan and OMCs showed a more and more pronounced hump shift toward the 520 positive direction by cycling to more negative potentials. These results prove that 521 hydrogen adsorbs at these catalysts and this adsorption is stronger (at more energetic 522 sites) as the potential is shifted negatively. Consequently, the hydrogen oxidation 523 gradually requires a higher polarization [39, 74-76].

524 In contrast, the oxidation hump was set at a constant value for CNFs and CNCs, 525 although it is not as evident for the last material due to its wide and not defined

526 hydrogen oxidation region. Considering the CVs in Figure 6, very high currents for 527 HER were found on these carbons at potentials below -0.7 V, showing that the main 528 contribution is hydrogen formation. As a consequence, it is concluded that hydrogen is 529 retained in these samples but the adsorption of hydrogen on high energy places does not 530 proceed. Therefore, the oxidation of absorbed hydrogen is observed but no shift to more 531 positive potentials is recorded. Other authors have obtained a low hydrogen-adsorption 532 capacity on oxidized samples [74, 77].



533

Fig. 6. Dependence of the voltammetry properties of carbon materials in 0.1 M NaHCO₃ with the value of negative potential cut-off ($v = 5 \text{ mV s}^{-1}$, stepwise = 200 mV).

537

538 It is important to note that the oxidation of hydrogen (hump observed at 0.65 for 539 CNFs and 0.74 V for CNCs during the anodic scan) overlaps with the current attributed to the quinone/hydroquinone groups (created during the metal remove treatments with
nitric acid) [76]. Similarly, these carbons displayed a reduction peak during the cathodic
scans, at 0.5 V and 0.3 V, respectively.

543

544 3.2.4 HER in the presence of CO₂ in the solution: evidences for CO₂ electroreduction

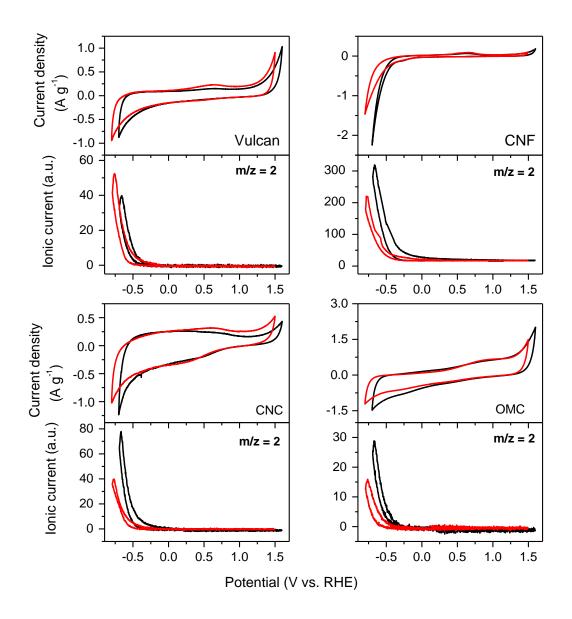
545 During CO_2 conversion in aqueous electrolytes, the HER occurs as a competitive 546 reaction by the water reduction. However, the presence of adsorbed hydrogen onto the 547 catalyst surface is a requirement for CO₂ activation. Thus, an effective electrode for 548 CO₂ reduction must suppress the HER so that all the adsorbed hydrogen will be 549 consumed only by CO₂ hydrogenation. Recently, high electrocatalytic activities to 550 hydrocarbons and oxygenates have been reported on carbon electrodes [33-36]. 551 However, to the best of our knowledge, this is the first work reporting the electrochemical activity for CO2 reduction of nanostructured carbons by on-line 552 553 electrochemical mass spectrometry.

In this work, DEMS experiments were recorded from -1.4 to 0.9 V vs. Ag/AgCl, with the purpose of studying the electrochemical behavior of the nanostructured carbons toward the CO_2 reduction in parallel to the HER. In order to consider the differences of pH between the electrolytes (8.4 in the electrolyte saturated with N₂ and 6.8 after CO_2 saturation), voltammograms were represented versus the RHE using the Equation 3:

559 $E_{RHE} = E_{Ag/AgCl} + 0.21 + 0.059 \text{ pH}$

(3)

Figure 7 shows the CVs (upper panel) and the corresponding MSCVs for hydrogen evolution (bottom panel) registered at 5 mV s⁻¹ in the base electrolyte, in absence (black curves) or in presence (red curves) of dissolved CO₂.



563

Fig. 7. CVs (upper panels) and MSCVs for H_2 , m/z = 2, (bottom panels) of carbon materials in 0.1 M NaHCO₃ (v = 5 mV s⁻¹). Black curves: Ar saturated solution. Red curves: CO₂ saturated solution.

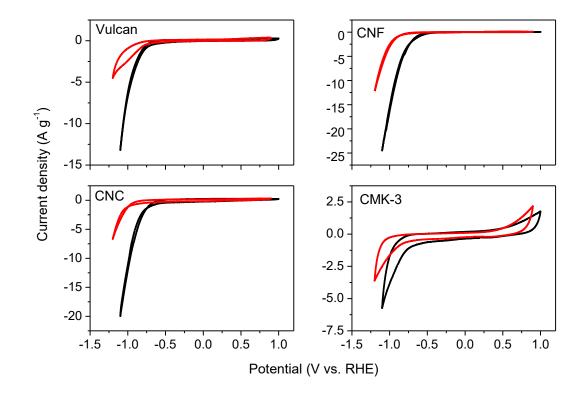
567

In the presence of CO₂, there is a clear shift of the potential for hydrogen evolution towards more negative values (between 90 and 150 mV negative shift) for all the nanocarbon catalysts. The evidences are clear in terms of both faradaic and ionic $(m/z = 2, H_2)$ currents. This shift might be ascribed to the adsorption of reduced CO₂related species (CO_{2,red}) on the surface of carbon catalysts hindering the adsorption of 573 hydrogen to the catalytic active sites, and therefore, leading to lower hydrogen evolution 574 rates. Among them, the largest decrease of hydrogen evolution rate was observed for the 575 CNF catalyst, with about 50 % lower faradaic and ionic current density. The extent of 576 diminution in HER rate in the presence of CO_2 can be related to the favorable 577 adsorption of ($CO_{2,red}$) species on the surface of catalytic active sites. This can be 578 interpreted as CNF presenting the highest density of ($CO_{2,red}$) adsorption sites among all 579 the NCMs herein investigated.

580 According to the bibliography [24, 78, 79], these adsorbates may be mainly 581 CO_{ad,} although the formation of other adsorbed species (such as formates) cannot be 582 discarded. To better identify the possible formation of CO₂ reduction intermediates, 583 current transients stepping the potential from 0.2 to -0.7 V vs. RHE were performed in 584 the CO₂ saturated electrolyte monitoring the mass signals m/z = 15 (CH₃⁺: methane), 30 585 (CH₃CH₃⁺ or H₂CO⁺: ethane or formaldehyde), 29 (CH₃CH₂⁺ or CHO⁺: ethane/ethanol 586 or an aldehyde), and 45 (HCHOO⁺ or CH₃CHOH⁺: formic acid or ethanol). The 587 formation of electrolysis products was not detected by DEMS indicating that volatile 588 species were not formed at these potentials. As a consequence, the decrease of HER rate 589 might be ascribed to the reversible adsorption of (CO_{2,red}) species on the surface of 590 carbon but not following the formation of volatile short-chain organic molecules in this 591 potential window.

592 CVs at more negative potentials were carried out for the NCMs from -1.8 V to 593 0.3 V vs. Ag/AgCl (from -1.1 V to 1 V vs. RHE in the case of the electrolyte saturated 594 with Ar and from -1.2 V to 0.9 V vs. RHE in the presence of CO₂) to further research 595 the activity of carbons for CO₂ reduction. The curves in the presence (red curves) and in 596 the absence of dissolved CO₂ (black curves) for each sample are shown in Figure 8. 597 After saturation with CO₂, lower hydrogen evolution cathodic currents were developed

for all carbon materials at -1.1 V vs. RHE that those obtained in the CO₂-free solution
corroborating the adsorption of species derived from CO₂ reduction.



600

601 **Fig. 8.** CVs of carbon materials in 0.1 M NaHCO₃ ($v = 5 \text{ mV s}^{-1}$) in presence and 602 absence of CO₂. Black curves: Ar saturated solution (from -1.1 V to 1 V vs. RHE). Red 603 curves: CO₂ saturated solution (from -1.2 V to 0.9 V vs. RHE).

604

605 Comparing the faradaic current at -1.1 V in the presence and in the absence of 606 CO₂ (black and red curves in Figure 8), a strong inhibition of the current was obtained 607 on the carbon black Vulcan (76%), CNFs (70%) and CNCs (83%), while a lower value 608 was obtained on OMCs (56%), which could be associated to a lower adsorption of 609 (CO_{2,red}) intermediates on the last carbon surface. In this context, OMCs exhibited a low 610 cathodic current in absence of CO_2 (see Figure 8, black curve) and consequently, a low 611 hydrogen coverage, resulting in a poor affinity for the adsorption of (CO₂)_{red} species. 612 Moreover, it is well established that the depletion of hydrogen ions in the near surface

613 of the electrode/electrolyte influences the catalytic behavior [80-82], which effect on the 614 hydrogen evolution is thus more evident for CNF and CNC. These samples are 615 characterized by the highest values of HER rate both in the base and the CO_2 -saturated 616 electrolyte.

617 Finally, significant differences were observed in the HER currents depending on 618 the positive potential limit. On one hand, in the case of the amorphous NCMs (OMCs, Vulcan), when they are cycled up to 1.6 V vs. RHE (Figure 6) the hydrogen evolution 619 620 current is noticeably lower than when the upper potential is 1.0 V vs. RHE (Figure 8, 621 black curves). More specifically, the current density at -1.1 V vs. RHE decreases from 13.3 A g^{-1} to 3.7 A g^{-1} for Vulcan (72%) and from 5.8 A g^{-1} to 2.1 A g^{-1} for OMCs 622 (64%) when cycling up to 1.6 V vs. RHE. The amorphous nature of carbon together 623 624 with the narrower porosity of these NCMs lead to the accumulation of oxygenated 625 species during the electrochemical oxidation at highly positive potentials, which results 626 in a decrease of the number of available active sites for HER. Whereas, in the case of 627 CNFs and CNCs there is a slight increase of current (~10%) when cycling up to 1.6 V 628 vs. RHE. Being less prone to corrosion, the catalytically active sites for HER in 629 graphitic carbons are not affected negatively upon applying highly positive potentials 630 but appear to be slightly more active or new active sites are created. Insights on this 631 phenomena will be studied by investigated the morphology of carbon materials by 632 identical location TEM analyses in the future.

633

634 **4. Conclusions**

In this work, the electrochemical and electrocatalytical performances of
nanostructured carbon electrodes (CNFs, CNCs, OMCs, Vulcan XC-72R) has been
studied by on-line differential electrochemical mass spectrometry (DEMS) in moderate

alkaline media (0.1 M NaHCO₃). The capacitance of the different materials is directly related to their surface area and hydrophilicity, as derived from the chemical characterization. DEMS results showed that the faradaic current in the base electrolyte from 1.3 to 1.6 V vs. RHE were associated only with the CO₂ formation (m/z = 44) by carbon corrosion and not with oxygen evolution (m/z = 32). Additionally, it was found that an increase of the graphitic character of the carbons resulted in a decrease of CO₂ generation due to the lower amount of surface defects in graphitic carbons.

645 On the other hand, spectro-electrochemical measurements showed a different 646 activity toward the H₂ evolution reaction (m/z =2), being the reaction favored on the 647 most graphitic carbon (CNFs) with an ionic current for m/z =2 signal 15 fold times 648 higher than the GC used as substrate.

Finally, H_2 evolution reaction was studied in the presence of CO_2 for evaluation of the materials in the electrochemical reduction of CO_2 . A significant decrease in the cathodic current developed in the H_2 evolution region (from -0.5 to -1.1 V vs. RHE) was obtained in a CO_2 -saturated 0.1 M NaHCO₃ solution for all carbon materials, which demonstrates the adsorption of species derived from CO_2 reduction at all carbon surfaces. However, volatile organic products were not detected by DEMS.

655

656 Acknowledgments

The authors gratefully acknowledge financial support given by Spanish MINECO (*CTQ2011-28913-C02-01 and 02*). S. Pérez-Rodríguez acknowledges Gobierno de Aragón for the DGA grant. Furthermore, the authors wish to thank Dra. Ana Beatriz García (INCAR-CSIC) for the TPD measurements.

661

662 **References**

- 663 [1] E. Antolini, Appl. Cat. B, 123–124 (2012) 52-68.
- 664 [2] A. Walcarius, Chem. Soc. Rev., 42 (2013) 4098-4140.
- 665 [3] S. Sharma, B.G. Pollet, J. Power Sources, 208 (2012) 96-119.
- 666 [4] C.W.B. Bezerra, L. Zhang, H. Liu, K. Lee, A.L.B. Marques, E.P. Marques, H. 667 Wang, J. Zhang, J. Power Sources, 173 (2007) 891-908.
- 007 wang, J. Zhang, J. 10wer Sources, 175(2007) 891-908.
- 668 [5] J. Qiao, Y. Liu, F. Hong, J. Zhang, Chem. Soc. Rev., 43 (2014) 631-675.
- 669 [6] J. Zhang, Z. Zhao, Z. Xia, L. Dai, Nat. Nano., 10 (2015) 444-452.
- 670 [7] Y. Cheng, S.P. Jiang, Prog. Nat. Sci.: Mater. Int., 25 (2015) 545-553.
- [8] S. Tang, G. Sun, J. Qi, S. Sun, J. Guo, Q. Xin, G.M. Haarberg, Chin. J. Catal., 31(2010) 12-17.
- 673 [9] P. Serp, M. Corrias, P. Kalck, Appl. Catal., A, 253 (2003) 337-358.
- [10] X. Guo, Y. Zhang, C. Deng, X. Li, Y. Xue, Y.-M. Yan, K. Sun, Chem. Commun.,
 51 (2015) 1345-1348.
- 676 [11] D. Sebastián, I. Suelves, R. Moliner, M.J. Lázaro, A. Stassi, V. Baglio, A.S. Aricò,
 677 Appl. Cat. B, 132-133 (2013) 22-27.
- 678 [12] T. Hyeon, S. Han, Y.-E. Sung, K.-W. Park, Y.-W. Kim, Angew. Chem. Int. Edi.,
 679 42 (2003) 4352-4356.
- [13] M.J. Lázaro, V. Celorrio, L. Calvillo, E. Pastor, R. Moliner, J. Power Sources, 196
 (2011) 4236-4241.
- 682 [14] B. Liu, S. Creager, J. Power Sources, 195 (2010) 1812-1820.
- [15] C. Alegre, L. Calvillo, R. Moliner, J.A. González-Expósito, O. Guillén-Villafuerte,
 M.V.M. Huerta, E. Pastor, M.J. Lázaro, J. Power Sources, 196 (2011) 4226-4235.
- 685 [16] S.J. Ashton, M. Arenz, J. Power Sources, 217 (2012) 392-399.
- [17] L.C. Colmenares, A. Wurth, Z. Jusys, R.J. Behm, J. Power Sources, 190 (2009) 1424.
- [18] C.-C. Hung, P.-Y. Lim, J.-R. Chen, H.C. Shih, J. Power Sources, 196 (2011) 140146.
- 690 [19] W. Li, A.M. Lane, Electrochem. Commun., 11 (2009) 1187-1190.
- [20] Y. Shao, J. Wang, R. Kou, M. Engelhard, J. Liu, Y. Wang, Y. Lin, Electrochim.
 Acta, 54 (2009) 3109-3114.

- 693 [21] S. Pérez-Rodríguez, G. García, L. Calvillo, V. Celorrio, E. Pastor, M.J. Lázaro, Int.
 694 J. Electrochem., 2011 (2011).
- 695 [22] S. Pérez-Rodríguez, N. Rillo, M.J. Lázaro, E. Pastor, Appl. Cat. B, 163 (2015) 83696 95.
- 697 [23] G. Centi, S. Perathoner, G. Winè, M. Gangeri, Green Chem., 9 (2007) 671-678.
- 698 [24] N. Yang, S.R. Waldvogel, X. Jiang, ACS Appl. Mater. Interfaces, 8 (2016) 28357-699 28371.
- 700 [25] S. Pérez-Rodríguez, E. Pastor, M.J. Lázaro, J. CO₂ Util., 18 (2017) 41-52.
- [26] C. Genovese, C. Ampelli, S. Perathoner, G. Centi, J. Energy Chem., 22 (2013) 202213.
- [27] M. Gangeri, S. Perathoner, S. Caudo, G. Centi, J. Amadou, D. Bégin, C. PhamHuu, M.J. Ledoux, J.P. Tessonnier, D.S. Su, R. Schlögl, Catal. Today, 143 (2009) 5763.
- [28] O.A. Baturina, Q. Lu, M.A. Padilla, L. Xin, W. Li, A. Serov, K. Artyushkova, P.
 Atanassov, F. Xu, A. Epshteyn, T. Brintlinger, M. Schuette, G.E. Collins, ACS Catal., 4
 (2014) 3682-3695.
- 709 [29] J. Zhang, Z. Xia, L. Dai, Sci. Adv., 1 (2015).
- [30] N. Cheng, Q. Liu, J. Tian, Y. Xue, A.M. Asiri, H. Jiang, Y. He, X. Sun, Chem.
 Commun., 51 (2015) 1616-1619.
- [31] H.B. Yang, J. Miao, S.-F. Hung, J. Chen, H.B. Tao, X. Wang, L. Zhang, R. Chen,
 J. Gao, H.M. Chen, L. Dai, B. Liu, Sci. Adv., 2 (2016).
- [32] G. Gao, Y. Jiao, F. Ma, Y. Jiao, E. Waclawik, A. Du, J. Catal., 332 (2015) 149155.
- 716 [33] X. Mao, T.A. Hatton, Ind. Eng. Chem. Res., 54 (2015) 4033-4042.
- 717 [34] W. Li, M. Seredych, E. Rodríguez-Castellón, T.J. Bandosz, ChemSusChem, 9718 (2016) 606-616.
- [35] X. Sun, X. Kang, Q. Zhu, J. Ma, G. Yang, Z. Liu, B. Han, Chem. Sci., 7 (2016)
 2883-2887.
- [36] J. Wu, S. Ma, J. Sun, J.I. Gold, C. Tiwary, B. Kim, L. Zhu, N. Chopra, I.N. Odeh,
 R. Vajtai, A.Z. Yu, R. Luo, J. Lou, G. Ding, P.J.A. Kenis, P.M. Ajayan, Nat. Commun.,
- 723 7 (2016) 13869.
- [37] G.-f. Long, K. Wan, M.-y. Liu, Z.-x. Liang, J.-h. Piao, P. Tsiakaras, J. Catal., 348
 (2017) 151-159.
- 726 [38] Y. Shao, G. Yin, J. Zhang, Y. Gao, Electrochim. Acta, 51 (2006) 5853-5857.

- [39] C. Vix-Guterl, E. Frackowiak, K. Jurewicz, M. Friebe, J. Parmentier, F. Béguin,
 Carbon, 43 (2005) 1293-1302.
- [40] K. Jurewicz, C. Vix-Guterl, E. Frackowiak, S. Saadallah, M. Reda, J. Parmentier, J.
 Patarin, F. Béguin, J. Phys. Chem. Solids, 65 (2004) 287-293.
- 731 [41] E. Antolini, Appl. Cat. B, 88 (2009) 1-24.
- [42] M. Carmo, V.A. Paganin, J.M. Rosolen, E.R. Gonzalez, J. Power Sources, 142
 (2005) 169-176.
- [43] S. Pérez-Rodríguez, M. Corengia, G. García, C.F. Zinola, M.J. Lázaro, E. Pastor,
 Int. J. Hydrogen Energy, 37 (2012) 7141-7151.
- 736 [44] S.J. Ashton, M. Arenz, Electrochem. Commun., 13 (2011) 1473-1475.
- [45] M.J. Lázaro, L. Calvillo, E.G. Bordejé, R. Moliner, R. Juan, C.R. Ruiz,
 Microporous Mesoporous Mater., 103 (2007) 158-165.
- 739 [46] V. Celorrio, L. Calvillo, S. Pérez-Rodríguez, M.J. Lázaro, R. Moliner,
 740 Microporous Mesoporous Mater., 142 (2011) 55-61.
- 741 [47] D. Sebastián, I. Suelves, R. Moliner, M.J. Lázaro, Carbon, 48 (2010) 4421-4431.
- [48] L. Calvillo, M.J. Lázaro, I. Suelves, Y. Echegoyen, E. García-Bordejé, R. Moliner,
 J. Nanosci. Nanotechnol., 9 (2009) 4164-4169.
- [49] J.L. Figueiredo, M.F.R. Pereira, M.M.A. Freitas, J.J.M. Órfão, Carbon, 37 (1999)
 1379-1389.
- [50] J.L. Figueiredo, M.F.R. Pereira, M.M.A. Freitas, J.J.M. Órfão, Ind. Eng. Chem.
 Res., 46 (2007) 4110-4115.
- 748 [51] O. Guillén-Villafuerte, G. García, M.C. Arévalo, J.L. Rodríguez, E. Pastor,
 749 Electrochem. Commun., 63 (2016) 48-51.
- [52] D. Sebastián, A.G. Ruíz, I. Suelves, R. Moliner, M.J. Lázaro, V. Baglio, A. Stassi,
 A.S. Aricò, Appl. Cat. B, 115 (2012) 269-275.
- 752 [53] A. Grondein, D. Bélanger, Carbon, 50 (2012) 4335-4342.
- 753 [54] A. Grondein, D. Bélanger, Fuel, 90 (2011) 2684-2693.
- 754 [55] H. Chhina, S. Campbell, O. Kesler, J. Power Sources, 179 (2008) 50-59.
- [56] D. Banham, F. Feng, T. Fürstenhaupt, K. Pei, S. Ye, V. Birss, J. Power Sources,
 196 (2011) 5438-5445.
- 757 [57] S. Xiao, S. Liu, J. Zhang, Y. Wang, J. Power Sources, 293 (2015) 119-126.
- 758 [58] D. Shao, D. Tang, J. Yang, Y. Li, L. Zhang, J. Power Sources, 297 (2015) 344-350.
- 759 [59] H.P. Boehm, Carbon, 40 (2002) 145-149.

- [60] A.E. Aksoylu, M. Madalena, A. Freitas, M.F.R. Pereira, J.L. Figueiredo, Carbon,39 (2001) 175-185.
- 762 [61] E. Frackowiak, F. Béguin, Carbon, 40 (2002) 1775-1787.
- [62] E. Frackowiak, K. Jurewicz, K. Szostak, S. Delpeux, F. Béguin, Fuel Process.
 Technol., 77–78 (2002) 213-219.
- 765 [63] E. Frackowiak, F. Béguin, Carbon, 39 (2001) 937-950.
- [64] R. Mysyk, E. Raymundo-Piñero, F. Béguin, Electrochem. Commun., 11 (2009)
 554-556.
- 768 [65] L. Wei, G. Yushin, Nano Energy, 1 (2012) 552-565.
- 769 [66] S. Gao, X. Jiao, Z. Sun, W. Zhang, Y. Sun, C. Wang, Q. Hu, X. Zu, F. Yang, S.
- 770 Yang, L. Liang, J. Wu, Y. Xie, Angew. Chem. Int. Ed., 55 (2016) 698-702.
- [67] N.-T. Suen, S.-F. Hung, Q. Quan, N. Zhang, Y.-J. Xu, H.M. Chen, Chem. Soc.
 Rev., 46 (2017) 337-365.
- [68] S. Maass, F. Finsterwalder, G. Frank, R. Hartmann, C. Merten, J. Power Sources,
 176 (2008) 444-451.
- 775 [69] B. Avasarala, R. Moore, P. Haldar, Electrochim. Acta, 55 (2010) 4765-4771.
- 776 [70] H.-S. Oh, K. Kim, Y.-J. Ko, H. Kim, Int. J. Hydrogen Energy, 35 (2010) 701-708.
- [71] F. Safizadeh, E. Ghali, G. Houlachi, Int. J. Hydrogen Energy, 40 (2015) 256-274.
- 778 [72] P.C.K. Vesborg, B. Seger, I. Chorkendorff, J. Phys. Chem. Lett., 6 (2015) 951-957.
- [73] M.S. Shafeeyan, W.M.A.W. Daud, A. Houshmand, A. Shamiri, J. Anal. Appl.Pyrolysis, 89 (2010) 143-151.
- 781 [74] K. Fic, E. Frackowiak, F. Beguin, J. Mater. Chem., 22 (2012) 24213-24223.
- [75] F. Béguin, K. Kierzek, M. Friebe, A. Jankowska, J. Machnikowski, K. Jurewicz, E.
 Frackowiak, Electrochim. Acta, 51 (2006) 2161-2167.
- 784 [76] K. Jurewicz, E. Frackowiak, F. Béguin, Appl. Phys. A, 78 (2004) 981-987.
- [77] M.J. Bleda-Martínez, J.M. Pérez, A. Linares-Solano, E. Morallón, D. Cazorla Amorós, Carbon, 46 (2008) 1053-1059.
- [78] P.A. Christensen, A. Hamnett, A.V.G. Muir, N.A. Freeman, J. Electroanal. Chem.,
 288 (1990) 197-215.
- 789 [79] K. Hara, A. Kudo, T. Sakata, J. Electroanal. Chem., 421 (1997) 1-4.
- 790 [80] M. Auinger, I. Katsounaros, J.C. Meier, S.O. Klemm, P.U. Biedermann, A.A.
- 791 Topalov, M. Rohwerder, K.J.J. Mayrhofer, Phys. Chem. Chem. Phys., 13 (2011) 16384792 16394.

- [81] I. Katsounaros, J.C. Meier, S.O. Klemm, A.A. Topalov, P.U. Biedermann, M.
 Auinger, K.J.J. Mayrhofer, Electrochem. Commun., 13 (2011) 634-637.
- 795 [82] D. Strmcnik, M. Uchimura, C. Wang, R. Subbaraman, N. Danilovic, V. van der,
- A.P. Paulikas, V.R. Stamenkovic, N.M. Markovic, Nat Chem, 5 (2013) 300-306.
- 797 798