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5       **Functional expression of aryl-alcohol oxidase in**  
6       ***Saccharomyces cerevisiae* and *Pichia pastoris* by**  
7       **directed evolution**

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16   **Running title:** A tandem-yeast expression system for aryl-alcohol oxidase.

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18   *cerevisiae*, *Pichia pastoris*, bioreactor.

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23 **ABSTRACT**

24 Aryl-alcohol oxidase (AAO) plays a fundamental role in the fungal ligninolytic  
25 secretome, acting as a supplier of H<sub>2</sub>O<sub>2</sub>. Despite its highly selective mechanism of action, the  
26 presence of this flavooxidase in different biotechnological settings has hitherto been  
27 hampered by the lack of appropriate heterologous expression systems. We recently described  
28 the functional expression of the AAO from *Pleurotus eryngii* in *Saccharomyces cerevisiae* by  
29 fusing a chimeric signal peptide (pre $\alpha$ proK) and applying structure-guided evolution. Here, we  
30 have obtained an AAO secretion variant that is readily expressed in *S. cerevisiae* and  
31 overproduced in *Pichia pastoris*. First, the functional expression of AAO in *S. cerevisiae* was  
32 enhanced through the in vivo shuffling of a panel of secretion variants, followed by the  
33 focused evolution of the pre $\alpha$ proK peptide. The outcome of this evolutionary campaign -an  
34 expression variant that accumulated 4 mutations in the chimeric signal peptide, plus two  
35 mutations in the mature protein- showed 350-fold improved secretion (4.5 mg/L) and was  
36 stable. This secretion mutant was cloned into *P. pastoris* and fermented in a fed-batch  
37 bioreactor to enhance production to 25 mg/L. While both recombinant AAO from *S. cerevisiae*  
38 and *P. pastoris* were subjected to similar N-terminal processing and had a similar pH activity  
39 profile, they differed in their kinetic parameters and thermostability. The strong glycosylation  
40 observed in the evolved AAO from *S. cerevisiae* underpinned this effect, since when the  
41 mutant was produced in the glycosylation-deficient *S. cerevisiae* strain  $\Delta kre2$ , its kinetic  
42 parameters and thermostability were comparable to its poorly glycosylated *P. pastoris*  
43 recombinant counterpart.

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49 **1. INTRODUCTION**

50 Aryl-alcohol oxidase (AAO, EC.1.1.3.7) is a monomeric extracellular flavoprotein that  
51 oxidizes a wide range of aromatic alcohols to their corresponding carbonyl compounds,  
52 concomitantly releasing H<sub>2</sub>O<sub>2</sub>. As a member of the glucose-methanol-choline (GMC)  
53 oxidoreductase superfamily, this FAD-dependent enzyme is secreted by different  
54 basidiomycetes involved in natural wood decay. The main role of AAO in nature is to supply  
55 ligninolytic peroxidases with H<sub>2</sub>O<sub>2</sub>, as well as to switch on the Fenton reaction in the  
56 combustion of lignin (Ferreira et al., 2005; Hernandez-Ortega et al., 2012a). In terms of  
57 biotechnological settings, AAO could be used in lignocellulose biorefineries to produce 2<sup>nd</sup>  
58 generation biofuels and added-value chemicals (Martinez et al., 2009; Alcalde, 2015).  
59 Moreover, and thanks to a highly enantioselective mechanism, AAO becomes very attractive  
60 for the chiral resolution of secondary alcohols aimed at obtaining valuable building blocks for  
61 pharmaceutical processes (Hernandez-Ortega et al., 2012b). Along these lines, recent findings  
62 highlight the oxidative potential of this enzyme with renewal chemicals, such as furfural  
63 derivatives for the (bio)polymer industry (Carro et al., 2015; Martinez et al., 2017). Despite  
64 these promising features, the lack of suitable heterologous functional expression systems in  
65 which the properties of AAO can be sculptured by directed evolution has precluded the use of  
66 this versatile flavooxidase in different industrial applications. We previously reported the initial  
67 functional expression of AAO from the white-rot fungus *Pleurotus eryngii* in *Saccharomyces*  
68 *cerevisiae* (Viña-Gonzalez et al., 2015). This was achieved by designing a chimeric signal  
69 peptide (pre $\alpha$ proK) that fused the pre- and pro-region of the  $\alpha$ -factor and the K<sub>1</sub> killer toxin  
70 prepro-leaders from *S. cerevisiae*, and subsequently employing directed evolution to restricted  
71 AAO regions. We obtained a panel of AAO secretion variants that was led by the *sac*FX7 mutant,  
72 in which the consensus/ancestral substitution (H91N) was responsible for a ~100-fold  
73 improvement in total activity, as well as enhanced stability in terms of temperature and pH.

74           The current work describes a tandem-yeast expression system for AAO that links the  
75   directed evolution for secretion in *S. cerevisiae* to its over-production in *Pichia pastoris* on a  
76   bench-bioreactor scale. Harnessing the high frequency of homologous DNA recombination of  
77   *S. cerevisiae*, mutant libraries were constructed by shuffling *Sac*FX7 with an ensemble of AAO  
78   secretion variants, while the chimeric peptide was further subjected to independent  
79   mutational loading. The resulting evolved AAO was transferred to *P. pastoris* for  
80   overproduction in a fed-batch bioreactor and characterized biochemically. To shed light on the  
81   effects exerted by hyperglycosylation in *S. cerevisiae*, the recombinant variant expressed in *P.*  
82   *pastoris* was further benchmarked with its counterpart secreted by a glycosylation-deficient *S.*  
83   *cerevisiae* strain.

## 84   **2. MATERIAL AND METHODS**

### 85   **2.1 Strains and chemicals**

86           All chemical were reagent-grade purity. Basal salts, PTM1 salts, *p*-methoxybenzyl  
87   alcohol, ABTS (2,2'-azino-bis(3-ethylbenzothiazoline-6-sulphonic acid)), horseradish peroxidase  
88   (HRP), Taq polymerase and the Yeast Transformation Kit were purchased from Sigma-Aldrich  
89   (SaintLouis, MO, USA). Zymoprep Yeast Plasmid Miniprep, Yeast Plasmid Miniprep Kit I and  
90   Zymoclean Gel DNA Recovery Kit were from Zymo Research (Orange, CA, USA). The *P. pastoris*  
91   expression vector (pPICZ B), the *P. pastoris* strain X-33 and zeocin were purchased from  
92   Invitrogen (Carlsbad, CA, USA). The protease deficient *S. cerevisiae* strain BJ5465 ( $\alpha$  *ura3-52*  
93   *trp1 leu2 $\Delta$ 1 his3 $\Delta$ 200 pep4::HIS3 prb1 $\Delta$ 1.6R can1 GAL*) was from LGC Promochem (Barcelona,  
94   Spain) whereas the glycosylation deficient *S. cerevisiae* strain YDR483W BY4742 (MATA $\alpha$   
95   *his3 $\Delta$ 1 leu2 $\Delta$ 0 lys2 $\Delta$ 0 *ura3 $\Delta$ 0  $\Delta$ KRE2*) was from ATCC (Manassas, VA, USA).  
96   The *Escherichia coli* strain XL2-Blue competent cells and Phusion DNA Polymerase were  
97   obtained from Agilent Technologies (Santa Clara, CA, USA). Restriction endonucleases Bsal,  
98   XhoI, XbaI, KpnI, PmeI, the DNA Ligation Kit, the Antarctic phosphatase, EndoH and T4 DNA*

99 Ligase were purchased from New England Biolabs (Ipswich, MA, USA). Oligonucleotide primers  
100 were acquired from Isogen Life Science (Barcelona, Spain).

## 101 **2.2 Culture media**

### 102 **2.2.1 Culture media for *Saccharomyces cerevisiae***

103 Minimal medium contained 0.67% (w:v) yeast nitrogen base, 1.92 g/L yeast synthetic  
104 drop-out medium supplement without uracil, 2% (w:v) raffinose and 25 µg/mL  
105 chloramphenicol. SC drop-out plates contained 0.67% (w:v) yeast nitrogen base, 1.92 g/L yeast  
106 synthetic drop-out medium supplement without uracil, 2% (w:v) bacto agar, 2% (w:v) D-  
107 glucose and 25 µg/mL chloramphenicol. YP medium contained 10 g yeast extract, 20 g peptone  
108 and double-distilled H<sub>2</sub>O (ddH<sub>2</sub>O) to 650 mL. Expression medium contained 144 mL YP 1.55x,  
109 13.4 mL 1M KH<sub>2</sub>PO<sub>4</sub> pH 6.0 buffer, 22.2 mL 20% galactose (w:v), 0.222 mL 25 µg/mL  
110 chloramphenicol and ddH<sub>2</sub>O to 200 mL.

### 111 **2.2.2 Culture media for *Pichia pastoris***

112 YPD medium contained 10 g/L yeast extract, 20 g/L peptone, 4 g/L D-glucose and 25  
113 µg/mL zeocin whereas YPD plates also contained 2% (w:v) bacto agar. BMD1 medium  
114 contained 100 mM potassium phosphate buffer pH 6.0, 3.5 g/L yeast nitrogen base without  
115 amino acids, 400 µg/L biotin and 10 g/L D-glucose. BMM2 medium contained 100 mM  
116 potassium phosphate buffer pH 6.0, 3.5 g/L yeast nitrogen base without amino acids, 400 µg/L  
117 biotin and 2% methanol (v:v). BMM10 medium contained 100 mM potassium phosphate  
118 buffer pH 6.0, 3.5 g/L yeast nitrogen base without amino acids, 400 µg/L biotin and 10%  
119 methanol (v:v). BMMY medium contained 100 mM potassium phosphate buffer pH 6.0, 3.5 g/L  
120 yeast nitrogen base without amino acids, 400 µg/L biotin and 0.5% methanol (v:v). Basal salts  
121 medium contained 26.7 mL/L 85% phosphoric acid, 0.93 g/L CaSO<sub>4</sub>·2H<sub>2</sub>O, 14.9 g/L  
122 MgSO<sub>4</sub>·7H<sub>2</sub>O, 18.2 g/L K<sub>2</sub>SO<sub>4</sub>, 4.13 g/L KOH and 40 g/L glycerol.

### 123 **2.2.3 Culture media for *Escherichia coli***

124 Luria-Bertani (LB) medium contained 10 g NaCl, 5 g yeast extract, 10 g peptone, 1 mL  
125 100 mg/mL ampicillin and ddH<sub>2</sub>O to 1 L whereas LB agar plates also contained 2% (w:v) bacto  
126 agar.

## 127 **2.3. Laboratory evolution**

### 128 **2.3.1 In vivo shuffling**

129 PCR reactions were performed separately with mutants *sac*FX7, *sac*13H2, *sac*10G5,  
130 *sac*7A11, *sac*4C7 and *sac*12G12. Reaction mixtures were prepared in a final volume of 50  $\mu$ L  
131 containing DNA template (0.92 ng/ $\mu$ L), 90 nM oligo sense RMLN (5'-  
132 CCTCTATACTTTAACGTCAAGG-3'), 90 nM Reverse primer RMLC (5'-  
133 GGGAGGGCGTGAATGTAAGC-3'), 0.3 mM dNTPs (0.075 mM each), 3% (v:v) dimethylsulfoxide  
134 (DMSO), 1.5 mM MgCl<sub>2</sub>, increasing concentrations of MnCl<sub>2</sub> (0.025, 0.05, 0.1 mM) and 0.05  
135 U/ $\mu$ L Taq DNA polymerase. PCRs were performed in a thermocycler (Mycycler, Bio-  
136 Rad, Hercules, CA, USA) and parameters were: 95°C for 2 min (1 cycle); 95°C for 45 s, 50°C for  
137 45 s, 74°C for 45 s (28 cycles); and 74°C for 10 min (1 cycle). The PCR products were mixed with  
138 the linearized episomal shuttle vector pJRoc30 (at a PCR product/linearized plasmid ratio of  
139 6:1) and transformed into competent *S. cerevisiae* cells to promote in vivo DNA shuffling. The  
140 whole gene was reassembled in vivo by transformation into *S. cerevisiae*, a process facilitated  
141 by the design of ~50-bp overhangs flanking each recombination area. Transformed cells were  
142 plated on SC drop-out plates and incubated for 3 days at 30°C. Colonies containing the whole  
143 autonomously replicating vector were picked and subjected to high-throughput screening.

### 144 **2.3.2 MORPHING library at the pre $\alpha$ proK**

145 The pre $\alpha$ proK signal peptide of *sac*FX8 variant (261 bp) was used as DNA template for  
146 focused random mutagenesis technique MORPHING (Mutagenic Organized Recombination  
147 Process by Homologous IN vivo Grouping) (Gonzalez-Perez et al., 2014). Mutagenic PCR was  
148 prepared in a final volume of 50  $\mu$ L containing: 90 nM RMLN, 90 nM C-ter prokiller (5'-

149 ACGCTTGCCACTGCTGGAAT-3'), 0.3 mM dNTPs (0.075 mM each), 3% DMSO, 0.1 mM MnCl<sub>2</sub>,  
150 1.5 mM MgCl<sub>2</sub>, 0.05 U/μL I Taq polymerase DNA, and 0.92 ng/μL template. The amplification  
151 parameters were 95°C for 2 min (1 cycle); 94°C for 45 s, 50°C for 45 s, and 74°C for 30 s (28  
152 cycles); and 74°C for 10 min (1 cycle). The whole AAO gene (1701 bp) was amplified by high-  
153 fidelity PCR in a final volume of 50 μL containing: 250 nM oligo sense N-ter AAO (5'-  
154 GCCGATTTTGACTACGTTGTCGTCG-3'), 250 nM oligo antisense RMLC, 1 mM dNTPs (0.25 mM  
155 each), 3% DMSO, 0.05 U/μL Phusion DNA polymerase, and 2 ng/μL template. High-fidelity PCR  
156 was performed using the following parameters: 95°C for 2 min (1 cycle); 94°C for 30 s, 50°C for  
157 30 s, 74°C for 2 min (30 cycles); and 74°C for 10 min (1 cycle). PCR products were mixed in  
158 equimolar amounts, 200 ng mutagenic signal peptide and 200 ng mature non-mutagenized  
159 protein, and transformed with linearized pJRoC30 (200 ng) into chemically competent cells, as  
160 described above.

### 161 **2.3.3 High-throughput screening (HTS) assay**

162 Individual clones were picked and cultured in sterile 96-well plates containing 50 μL of  
163 minimal medium. In each plate, column number 6 was inoculated with the parental type  
164 (internal standard) and well H1 with URA3- *S. cerevisiae* cells (negative control). Plates were  
165 sealed to prevent evaporation and incubated at 30°C, 225 rpm and 80% relative humidity in a  
166 humidity shaker (Minitron-INFORS, INFORS-HT, Switzerland). After 48 hours, 160 μL of  
167 expression medium were added to each well and cultured for additional 48 hours. Aliquots of  
168 20 μL of yeast supernatants were transferred to a 96-well plate with liquid handler robotic  
169 station Freedom EVO (Tecan, Männedorf, Switzerland) and 180 μL of HRP-ABTS reagent (final  
170 concentrations of HRP-ABTS reagent in the well: 1mM *p*-methoxybenzyl alcohol, 2.5 mM ABTS,  
171 1μg/mL HRP in 100 mM phosphate buffer pH 6.0) were dispensed with Multidrop™ Combi  
172 Reagent Dispenser (Thermo Scientific, Massachusetts, USA). The plates were incubated at  
173 room temperature and measured in kinetic mode at 418nm ( $\epsilon_{\text{ABTS}^{**}} = 36000 \text{ M}^{-1} \text{ cm}^{-1}$ ). The

174 HTS-assay incorporated two consecutive re-screenings to rule out the selection of false  
175 positives as described elsewhere (Viña-Gonzalez et al., 2016).

## 176 **2.4 AAO in *S. cerevisiae***

### 177 **2.4.1 Shake-flask fermentation**

178 A single colony from the *S. cerevisiae* clone containing the AAO fusion gene was picked  
179 from a SC drop-out plate, inoculated in minimal medium (20 mL) and incubated for 48 h at  
180 30°C and 220 rpm. An aliquot of cells was removed and used to inoculate minimal medium  
181 (100 mL) in a 500 mL flask ( $OD_{600} = 0.25$ ). The cells completed two growth phases (6–8 h;  $OD_{600}$   
182 = 1) and then expression medium (900 mL) was inoculated with the pre-culture (100 mL)  
183 ( $OD_{600}$  of 0.1). After incubating for 72 h at 25°C and 220 rpm (maximal AAO activity;  $OD_{600} =$   
184 25–30), the cells were recovered by centrifugation at 4500 rpm and 4°C (Avanti J-E centrifuge,  
185 Beckman Coulter Inc. CA, USA) and the supernatant was double-filtered (using both glass  
186 membrane filter and a nitrocellulose membrane of 0.45  $\mu\text{m}$  pore size). The incubation for the  
187 expression in glycosylation deficient *S. cerevisiae* strain YDR483W BY4742 was stopped after  
188 18 h to avoid proteolytic degradation of the AAO by extracellular yeast proteases.

## 189 **2.5 AAO in *P. pastoris***

### 190 **2.5.1 AAO cloning in *P. pastoris***

191 The coding region of the evolved AAO variant (1962 bp) was cloned into the expression  
192 vector pPICZ-B. First, pJRoc30-FX7/FX9 was used to amplify AAO variants with the primers  
193 ppKpnAAO-dir (5'- GGGGTACCATGAGATTTCTTCAATTTACTGC-3') and ppAAO-rev (5'-  
194 GCTCTAGACTACTGATCAGCCTTGATAAGATCGGC-3'), the primers included targets for  
195 restriction enzymes KpnI and XbaI, respectively (underlined). The PCR reactions were prepared  
196 in a final volume of 50  $\mu\text{L}$  containing 250 nM of each primer, 1 mM dNTPs (0.25 mM each), 3%  
197 DMSO, 0.05 U/ $\mu\text{L}$  Phusion DNA polymerase, and 2 ng/ $\mu\text{L}$  template. The parameters for the PCR  
198 were: 95°C for 2 min (1 cycle); 94°C for 30 s, 50°C for 30 s, 74°C for 2 min (30 cycles); and 74°C



199 for 10 min (1 cycle). The pPICZ-B vector and the PCR product were digested with the restriction  
200 enzymes KpnI and XbaI at 37°C for 1 h. The 5' and 3' ends of the linearized pPICZ-B plasmid  
201 were dephosphorylated using antarctic phosphatase at 37°C for 1 h adding 1 U of enzyme per  
202 every 200 ng of linearized vector. The PCR product and the linearized vector were loaded onto  
203 a preparative agarose gel, purified using the Zymoclean Gel DNA Recovery kit and ligated with  
204 T4 DNA ligase at room temperature for 30 min. After transformation of the pPICZ-B-AAO  
205 construct into chemically competent *E. coli* XL2-Blue cells, the plasmid was proliferated,  
206 linearized with the restriction enzyme PmeI at 37°C for 1 h and transformed into electro-  
207 competent *P. pastoris* X-33 cells. Electro-competent *P. pastoris* cells were prepared and  
208 transformed with the construction as described in the protocol from Lin-Cereghino et al. (Lin-  
209 Cereghino et al., 2000) mixing 200 ng of linearized vector and 50 µL of competent cells.  
210 Transformants were grown on YPD plates.

### 211 **2.5.2 Deep-well plate fermentation**

212 *P. pastoris* colonies containing AAO under the control of the AOX1 promoter (pPICZ-B-  
213 AAO) were picked and cultivated in 96-deep-well plates containing 300 µL of BMD1 medium  
214 per well. The plates were incubated at 25°C, 300 rpm and 80% humidity for 2 days in a  
215 humidity shaker. Afterwards, 300 µL of BMM2 medium were added per well. After 12 hours of  
216 incubation, 70 µL of BMM10 medium were added to each well repeating this addition every 24  
217 hours for 3 days. After 142 h, the activity with *p*-methoxybenzyl alcohol was measured (final  
218 concentrations in the reaction mixture: 1mM *p*-methoxybenzyl alcohol, 2.5 mM ABTS, 1µg/mL  
219 HRP in 100 mM phosphate buffer pH 6.0).

### 220 **2.5.3 Shake-flask fermentation**

221 Transformants with the best activity from the deep-well plate fermentations were  
222 grown in YPD agar plates and inoculated in 3 mL of liquid YPD at 30°C and 250 rpm. The culture  
223 reached the optical density at 600 nm at 1 after 6–7 h and was inoculated in 20 mL of BMMY

224 medium in 100 mL shaken flasks. The cultures were incubated at 25°C or 30°C and they were  
225 supplemented with 250 µL of methanol every 24 h. After 3 days of methanol addition, the best  
226 clone with the highest activity was selected for the bioreactor fermentation.

#### 227 **2.5.4 Production in Bioreactor**

228 The FX9 mutant ( $\pi$ FX9) under the control of the AOX1 promoter in the pPICZ-B-FX9  
229 construct was produced in a 5 L vessel fermenter (Minifors, INFORS-HT, Switzerland). The  
230 bioreactor was filled with 2 L of basal salts medium (initial volume: 2 L). After sterilization, 4.35  
231 mL/L PTM1 trace salts and 1 mL Antifoam 204 were added to the medium and the pH was  
232 adjusted with ammonium hydroxide to 5.0. The fermentation was started with the addition of  
233 0.2 L of preculture grown on YPD medium in several baffled shaken flasks at 150 rpm and 30°C  
234 overnight ( $OD_{600}$  between 6–10). According to the *Pichia Fermentation Process Guidelines* of  
235 Invitrogen the batch fermentation was run at 30°C, 600 rpm and air aeration 1 vvm. Once all  
236 the glycerol from the batch was consumed, the glycerol fed phase was initiated by the addition  
237 of 50 % (w/v) glycerol feed containing 12mL/L PTM1 trace salts to achieve higher cell density at  
238 a 21.8 mL/h feed rate. After 2 h, the glycerol feed faded out by a linear ramp 14.6-0 mL/h over  
239 2 h and the methanol feed containing 12 mL/L PTM1 trace salts started at a 7.2 mL h<sup>-1</sup> for the  
240 culture to transition and adapt to methanol. From this time on the temperature was set to  
241 25°C and the Dissolved Oxygen (DO) above 20% with the control of the stirring speed between  
242 600 and 1200 rpm and aeration using mixtures of air and O<sub>2</sub> within 0.7 and 1 vvm. At the end  
243 of the transition phase the methanol/PTM1 feeding was increased to 14.6 mL/h until the end  
244 of the process. Water evaporation losses were minimized during the process with an exhaust  
245 gas condenser and cooling water at 4°C. The fermentation was controlled by taking samples  
246 for biomass analysis and AAO activity: The cell concentration was monitored by measuring  
247 the optical density of cultures at 600 nm ( $OD_{600}$ ). For wet dry weight (CDW) measurement,  
248 cells were separated from 1 mL culture broth by centrifugation at 10,000 g for 5 minutes using  
249 pre-weighed 1.5 mL tubes. The wet weight is measured immediately after all the yeast

250 supernatant has been removed. AAO activity was measured with HRP/ABTS method with *p*-  
251 methoxybenzyl alcohol as the substrate.

## 252 **2.6 AAO purification**

253 The FX9 variants expressed in *S. cerevisiae* (protease deficient strain BJ5465 and  
254 glycosylation deficient strain YDR483W BY4742) and *P. pastoris* were purified to homogeneity  
255 as described in a former work (Viña-Gonzalez et al., 2015).

## 256 **2.7 AAO biochemical characterization**

### 257 **2.7.1 N-terminal analysis and pI Determination**

258 Purified AAO variants were subjected to SDS/PAGE, and the protein band was blotted  
259 onto PVDF membranes. The PVDF membrane was stained with Coomassie Brilliant Blue R-250,  
260 after which the enzyme band was excised and processed for N-terminal amino acid sequencing  
261 on a precise sequencer at the Protein Chemistry Service at the The Biological Research Center  
262 (Madrid, Spain). Purified FX9 (8  $\mu\text{g}$ ) was subjected to two-dimensional electrophoresis gel in  
263 order to determine the pI.

### 264 **2.7.2 Determination of kinetic-thermostability ( $T_{50}$ )**

265 Appropriate dilutions of AAO were prepared for the assay. The gradient scale ranging  
266 from 30 to 80°C was established as follows: 30.0, 31.4, 34.8, 39.3, 45.3, 49.9, 53, 55, 56.8, 59.9,  
267 64.3, 70.3, 75, 78.1 and 80°C. This gradient profile was achieved using a thermocycler. After 10  
268 min of incubation, AAO samples were removed and chilled out on ice for 10 min and incubated  
269 further at room temperature for 5 min. Finally, samples of 20  $\mu\text{L}$  were added to 180  $\mu\text{L}$   
270 volumes of 100 mM sodium phosphate pH 6.0 buffer containing 1mM *p*-methoxybenzyl  
271 alcohol and activity was measured as anisaldehyde production as absorption at 285 nm ( $\epsilon_{285} =$   
272  $16,950 \text{ M}^{-1} \text{ cm}^{-1}$ ). Thermostability values were calculated from the ratio between the residual  
273 activities incubated at different temperature points and the initial activity at room  
274 temperature. The  $T_{50}$  value was determined by the transition midpoint of the inactivation

275 curve of the protein as a function of temperature, which in our case was defined as the  
276 temperature at which the enzyme lost 50% of its activity following an incubation of 10  
277 minutes. All reactions were performed by triplicate.

### 278 **2.7.3 pH activity profile**

279 Appropriate dilutions of enzyme samples were prepared in such a way that aliquots of  
280 20  $\mu\text{L}$  gave rise to a linear response in kinetic mode. The optimum pH activity was determined  
281 using 100 mM citrate-phosphate-borate buffer at different pH values (2.0, 3.0, 4.0, 5.0, 6.0,  
282 7.0, 8.0 and 9.0) containing 0.3 *p*-methoxybenzyl alcohol.

### 283 **2.7.4 Kinetic parameters**

284 Kinetic constants for AAO were estimated in 100 mM sodium phosphate pH 6.0.  
285 Reactions were performed by triplicate and substrates oxidations were followed by measuring  
286 the absorption at 285 nm for *p*-methoxybenzyl alcohol,  $\epsilon_{285} = 16,950 \text{ M}^{-1} \text{ cm}^{-1}$ ; 310 nm for  
287 veratryl alcohol,  $\epsilon_{310} = 9,300 \text{ M}^{-1} \text{ cm}^{-1}$ ; 250 nm for benzyl alcohol,  $\epsilon_{250} = 13,800 \text{ M}^{-1} \text{ cm}^{-1}$ ; 280  
288 nm for 2,4-hexadien-1-ol,  $\epsilon_{280} = 30,140 \text{ M}^{-1} \text{ cm}^{-1}$ . Steady-state kinetics parameters were  
289 determined by fitting the initial reactions rates at different substrate concentrations to the  
290 Michaelis-Menten equation for one substrate,  $v/e = k_{\text{cat}} \cdot S / (K_m + S)$  where  $e$  represent the  
291 enzyme concentration,  $k_{\text{cat}}$  is the maximal turnover rate,  $S$  is the substrate concentration and  
292  $K_m$  the Michaelis constant. Data were fit using SigmaPlot 10.0 (Systat. Software Inc. Richmond,  
293 CA, USA).

### 294 **2.7.5 Protein modeling**

295 A structural model of the AAO from *P. eryngii* crystal structure at a resolution of 2.55  $\text{\AA}$   
296 (Protein Data Bank Europe [PDB] accession number 3FIM, (Fernandez et al., 2009) was used as  
297 scaffold for the wild type AAO model and the FX9 mutant homology model, obtained by PyMol  
298 (Schrodinger LLC.; <http://www.pymol.org>).

299

### 300 2.7.6 DNA sequencing

301 All genes were verified by DNA sequencing (BigDye Terminator v3.1 Cycle Sequencing  
302 Kit). The primers for the genes cloned in the pJRoC30 plasmid were: primers sense, RMLN and  
303 AAOsec1F 5'-GTGGATCAACAGAAGATTTTCGATCG-3' and primers antisense RMLC 5'-  
304 GCTTACATTACGCCCTCCC-3', AAOsec2R 5'-GTGGTTAGCAATGAGCGCGG-3' and AAOsec3R 5'-  
305 GGAGTCGAGCCTCTGCCCT-3'. For the AAO genes cloned in the pPICZ-B plasmid primers were:  
306 ppKpnAAO-dir and AAOsec1F as primers sense and ppAAO-rev, AAOsec2R and AAOsec3R as  
307 primers antisense.

## 308 3. RESULTS AND DISCUSSION

### 309 3.1 Improved secretion in *S. cerevisiae* by in vivo shuffling and MORPHING of the chimeric 310 signal peptide

311 During the first evolutionary campaign to increase AAO secretion in yeast, six mutants  
312 (carrying 7 beneficial mutations) were identified with improvements in total activity that  
313 ranged from roughly 2- up to 100-fold (for *sac*FX7), **Fig. 1** (Viña-Gonzalez et al., 2015). Given  
314 that most of these mutations were >20 residues from one another, they were shuffled in vivo  
315 by taking advantage of the homologous recombination machinery of *S. cerevisiae* (Gonzalez-  
316 Perez et al., 2012). The mutant library was screened in the HRP-ABTS assay using *p*-  
317 methoxybenzyl alcohol as the substrate as described previously (Viña-Gonzalez et al., 2015;  
318 Viña-Gonzalez et al., 2016). The best mutant from this round of DNA shuffling was *sac*FX8,  
319 which showed 2.6-fold and 250-fold improved total activity over *sac*FX7 and the parental AAO,  
320 respectively. As planned, several crossover events took place that allowed mutations from  
321 different parental types to be convened: the consensus-ancestral mutation H91N from *sac*FX7;  
322 the L170M mutation from *sac*10G5; and the T50A mutation at the K<sub>1</sub> killer toxin pro-leader  
323 inherited from *sac*12G12, **Fig. 1**. To further enhance secretion, we evolved the pre $\alpha$ proK signal  
324 leader by MORPHING, a domain-focused mutagenesis technique that allows mutations and

325 crossover events to be randomly introduced in defined stretches (Gonzalez-Perez et al., 2014).  
326 With this strategy 3 new mutations were included in the pre $\alpha$ proK (F3S at the pre $\alpha$ , and H25N-  
327 F52L at the K<sub>1</sub> pro-leader), giving rise to the final *sac*FX9 secretion variant with a 350-fold  
328 improvement in activity relative to the parental AAO type and with expression levels of 4.5  
329 mg/L in flask culture.

330 The evolved leader sequence of *sac*FX9 derived from the DNA shuffling and the focused  
331 evolution experiments carried four substitutions relative to the original pre $\alpha$ proK chimeric  
332 construction, **Fig. 1, Fig. 2A**. The pre $\alpha$ -leader segment carries the F[3 $\alpha$ ]S mutation which agrees  
333 well with substitutions at the same position (F[3 $\alpha$ ]P/L) previously found in  $\alpha$ -factor prepro-  
334 leaders that improved antibody secretion (Rakestraw et al., 2009). An acidic residue was  
335 introduced into the proK-peptide with the new substitution N[25 $\kappa$ ]D, whereas mutation  
336 T[50 $\kappa$ ]A, inherited from parental type 12G12, together with F[52 $\kappa$ ]L increase the hydrophobic  
337 load of the middle sequence. In the mature protein, the mutation L170M from the parental  
338 10G5 is located in an  $\alpha$ -helix at the surface and mutation H91N from FX7 is in the catalytic  
339 pocket, **Fig. 2B, C**. As we described previously, Asn91 is a consensus residue situated at the si-  
340 face of the FAD that stabilizes the conformation of the cofactor, thereby enhancing secretion  
341 and AAO stability (Viña-Gonzalez et al., 2015).

### 342 **3.2 Functional expression of recombinant AAO in *P. pastoris* and scaling-up**

343 The use of compatible tandem-expression systems for protein engineering and  
344 overproduction can overcome certain limitations when dealing with complex eukaryotic  
345 enzymes like AAO (Alcalde et al., 2015). In particular, combining *S. cerevisiae* as the host of  
346 choice for the directed evolution of eukaryotic ligninases with the methylotrophic yeast *P.*  
347 *pastoris* (currently reclassified as *Komagataella phaffii*) for overproduction offers many  
348 attractive advantages, as demonstrated recently (Mate et al., 2013; Molina-Espeja et al.,  
349 2015). Heterologous expression in *S. cerevisiae* and *P. pastoris* falls under the lowest-common-

350 denominator of a well-defined secretory apparatus and the ability to perform complex post-  
351 translational modifications, which frequently results in reasonable secretion of the active and  
352 stable enzyme. However, *S. cerevisiae* has a broad variety of episomal vectors, high-  
353 transformation efficiencies and a precise recombination apparatus to aid the creation and  
354 screening of mutant libraries for directed evolution. While *P. pastoris* lacks such properties, it  
355 outperforms *S. cerevisiae* in terms of protein production under the control of strong and  
356 tightly regulated promoters, reaching extremely high cell densities in bioreactors (Ahmad et  
357 al., 2014). Hence, during the heterologous expression of AAO in yeast, the question that arises  
358 is can the improvements in secretion obtained by directed evolution in *S. cerevisiae* be  
359 transferred to *P. pastoris*, or in other words, how well are the improvements in secretion  
360 preserved in both yeasts.

361 To assess the compatibility of these two systems, the evolved variants  $_{sac}FX7$  and  $_{sac}FX9$   
362 were cloned into *P. pastoris* to determine if the improvements in secretion furnished by the  
363 mutations are consistent between hosts. Under the methanol inducible AOX1 promoter,  
364 transformants were grown in deep-well plate microfermentations and screened for secretion -  
365 *P. pastoris* can integrate up to six copies of the foreign gene into its genome-. Selected clones,  
366  $_{\pi}FX7$  and  $_{\pi}FX9$ , were then produced in 100 mL shaking flask cultures, producing total activity  
367 values of 50 and 235 U/L, respectively. Hence, the beneficial mutations for secretion in *S.*  
368 *cerevisiae* retained their effects in *P. pastoris* and they were even associated with an  
369 improvement in total activity from 3.6 to 4.7-fold in both the variants. To harness the high cell  
370 titers of *P. pastoris* in the bioreactor,  $_{\pi}FX9$  was transferred to a 5L fed-batch fermenter and  
371 after six days, maximal volumetric activity was reached (1378 U/L) with the production of AAO  
372 (25.5 mg/L) surpassing that obtained in shaking-flask cultures roughly 6-fold. Since AAO is  
373 secreted similarly by *S. cerevisiae* and *P. pastoris* (**Table 1**), this improved production can be  
374 solely attributed to the high cell densities achieved by *P. pastoris* in the bioreactor (up to 260 g  
375 wet biomass/L; OD<sub>600</sub> ~ 430), **Fig. 3A**.

376

377 **3.3 Influence of glycosylation on biochemical parameters**

378 The  $_{sac}FX9$  and  $_{\pi}FX9$  variants were purified to homogeneity and characterized  
379 biochemically. N-terminal sequencing confirmed the correct cleavage of the chimeric pre $\alpha$ proK  
380 by the KEX2 protease in the Golgi compartment in both yeasts, **Table 1**. It is well known that *S.*  
381 *cerevisiae* produces strong glycosylation during heterologous protein expression. Indeed, as  
382 occurred with the parental  $_{sac}FX7$  (Viña-Gonzalez et al., 2015),  $_{sac}FX9$  underwent  
383 hyperglycosylation (~60% glycosylation) and the wide smear produced by the different  
384 glycoforms (ranging from ~200 to 63 kDa in SDS-PAGE) collapsed into a single 63 kDa band  
385 after deglycosylation with EndoH, **Fig. 3B, Table 1**. By contrast, in *P. pastoris* the same variant  
386 ( $_{\pi}FX9$ ) produced a single ~63 kDa band before and after treatment with EndoH, highlighting  
387 the weak glycosylation expected in *P. pastoris*, **Fig. 3B**. The  $T_{50}$  (the temperature at which the  
388 enzyme retains 50% of its activity after a ten minute incubation) of  $_{sac}FX9$  was slightly higher  
389 (1.7°C) than that of  $_{\pi}FX9$ , possibly due to this hyperglycosylation, **Table 1, Fig. 2C**. As such, the  
390 kinetic thermostability of both the recombinant variants expressed by the yeasts exceeded  
391 that reported for wild type AAO expressed in *E. coli* after in vitro refolding by ~15 °C ( $T_{50} = 47.5$   
392 °C), emphasizing the beneficial effect of: i) natural folding and heterologous secretion in yeast;  
393 and ii) the introduction of the stabilizing consensus-ancestor mutation H91N, as described  
394 previously (Viña-Gonzalez et al., 2015). The pH activity profile of  $_{sac}FX9$  and  $_{\pi}FX9$  with *p*-  
395 methoxybenzyl alcohol was similar, maintaining over 90 % of their activity from pH 2.0 to 6.0,  
396 **Fig. 3D**. When the steady kinetic parameters were measured for the oxidation of aromatic and  
397 aliphatic alcohols, **Table 2**, the catalytic efficiencies of  $_{sac}FX9$  were similar to those of the  
398 parental type  $_{sac}FX7$ , as was the order of preference for the different substrates. By contrast,  
399  $_{\pi}FX9$  retained similar  $K_m$  values to that of  $_{sac}FX9$  but improved by ~2-fold the  $k_{cat}$  irrespective of  
400 the alcohol tested.



401 The discrepancies in the kinetic parameters and thermostability between  $_{sac}$ FX9 and  
402  $_{\pi}$ FX9 may be related to the different degrees of glycosylation in *S. cerevisiae* and *P. pastoris*. To  
403 assess this, FX9 was also cloned into the glycosylation-deficient  $\Delta kre2$  *S. cerevisiae* strain.  
404  $\Delta kre2$  is thought to attach smaller mannose oligomers than wild type strains to the 7 predicted  
405 N-glycosylation motifs (Asn-X-Ser/Thrs) in AAO (*i.e.* N62, N138, N151, N222, N303, N325 and  
406 N369). After production and purification, the variant secreted by  $\Delta kre2$  ( $\Delta$ FX9) was  
407 characterized biochemically. As predicted, noticeable lower glycosylation was evident by SDS-  
408 PAGE, resolving to a smooth smear with a concentration of the protein at ~63 kDa, and it  
409 unequivocally tightened into a single band upon deglycosylation, **Fig. 3B, Table 1**. The  $\Delta$ FX9  
410 variant displayed a similar pH activity profile to its AAO counterparts together with a  $T_{50}$  value  
411 identical to that of  $_{\pi}$ FX9 (*i.e.* 1.7°C lower than  $_{sac}$ FX9), **Fig. 3C, D**. To complete the breakdown of  
412 the biochemical properties of the recombinant AAOs, the kinetic parameters of  $\Delta$ FX9 were  
413 measured. As expected, they came close to those of  $_{\pi}$ FX9 due to the ~1.5-fold enhancement in  
414 the  $k_{cat}$  while the  $K_m$  was maintained, **Table 2**. Together, the expression of FX9 in  $\Delta kre2$   
415 confirmed that the variation in kinetics and thermostability between  $_{sac}$ FX9 and  $_{\pi}$ FX9 were  
416 produced by the distinct degree of glycosylation.

### 417 3.4 CONCLUSIONS

418 This study shows how to harness a tandem-yeast expression system to engineer a  
419 fungal AAO by directed evolution and overproduce it in a bioreactor. The properties acquired  
420 during the evolution cycles in *S. cerevisiae* are easily decoded by *P. pastoris*, which can  
421 produce the recombinant enzyme while retaining its improved catalytic properties and general  
422 stability. As a natural progression, future studies could focus on the production of the  
423 recombinant enzyme at the g/L scale in other strong industrial hosts like *Trichoderma* or  
424 *Aspergillus sp.* Certainly, the findings presented here invite a further exploration and extension  
425 of the biotechnological potential of AAO, for example tailoring its activity to oxidize secondary

426 alcohols and resolve chiral mixtures, or tuning the AAO catalysis to furfural-derivative cascade  
427 reactions (Hernandez-Ortega et al., 2012b; Carro et al., 2015; Martinez et al., 2017).

#### 428 **ACKNOWLEDGEMENTS**

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497 **FIGURE LEGENDS**

498 **Figure 1.** Laboratory evolution of the AAO from *Pleurotus eryngii* towards functional expression  
 499 in yeast. New mutations are represented as stars and accumulated mutations as squares. The  
 500 pre $\alpha$ -leader segment is depicted in green, the prok-leader segment in light blue and the  
 501 mature AAO in dark blue. The TAI (total activity improvement) is the value indicating the  
 502 improvement in AAO activity detected in *S. cerevisiae* supernatants relative to the parental  
 503 type: \*1<sup>st</sup> G, results from the first generation of variants published in Viña-Gonzalez et al.,  
 504 2015.

505 **Figure 2.** Mutations presented by FX9. (A) Substitutions in the chimeric pre $\alpha$ proK signal  
 506 peptide. (B and C) Molecular model using the *Pleurotus eryngii* AAO crystal structure as a  
 507 template (PDB code 3FIM). (B) wild type AAO and (C) the FX9 variant. FAD is depicted in yellow  
 508 and the details of the two mutations in FX9 (blue) are compared with the corresponding  
 509 residues in the wild type (red).

510 **Figure 3.** (A) Fermentation in a 5L bioreactor of recombinant  $\pi$ FX9 expressed in *P. pastoris*.  
 511 Fermentation was performed in four steps: glycerol-batch phase for 26 h, glycerol-fed phase  
 512 for 4h, transition phase for 4 h and methanol induction phase for 112 h. The black circles  
 513 represent the wet biomass, the white triangles the volumetric AAO activity and the dotted  
 514 vertical line the beginning of the induction phase. (B) Molecular mass of recombinant AAO.  
 515 10% SDS-polyacrylamide gel: Lanes 1 and 8, protein markers; 2, purified  $_{sac}$ FX9 mutant; 3,  
 516 deglycosylated  $_{sac}$ FX9; 4, purified  $_{\Delta}$ FX9; 5, deglycosylated  $_{\Delta}$ FX9; 6, purified  $_{\pi}$ FX9; 7  
 517 deglycosylated  $_{\pi}$ FX9. (C) Kinetic thermostability ( $T_{50}$ ) of the recombinant variants:  $_{sac}$ FX9 (grey  
 518 triangles),  $_{\Delta}$ FX9 (black squares) and  $_{\pi}$ FX9 (white circles). (D) pH activity profiles for  $_{sac}$ FX9 (grey  
 519 triangles),  $_{\Delta}$ FX9 (black squares) and  $_{\pi}$ FX9 (white circles) with *p*-methoxybenzyl alcohol (1 mM).  
 520 Each point represents the mean and standard deviation of three independent experiments.

521

522

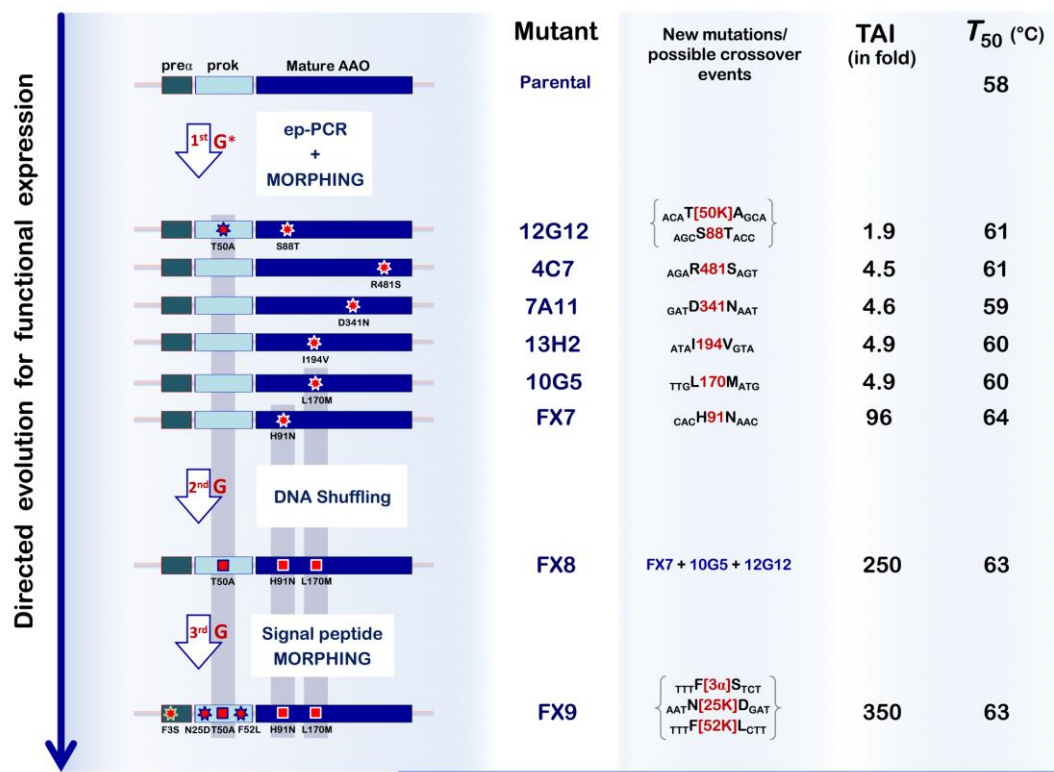
523 **TEXT FOR GRAPHICAL TABLE OF CONTENTS:**

524 Fungal aryl-alcohol oxidases (AAO) are precious biocatalysts whose presence in industrial  
525 biotechnology is being impeded by the absence of proper heterologous expression system. In  
526 the present study, the functional expression of AAO from white rot fungus *Pleurotus eryngii*  
527 was adapted to a tandem-yeast expression system aimed at boosting secretion. After applying  
528 different directed evolution strategies in *S. cerevisiae*, the evolved AAO was successfully  
529 overproduced in *Pichia pastoris* in bench-bioreactor.

530

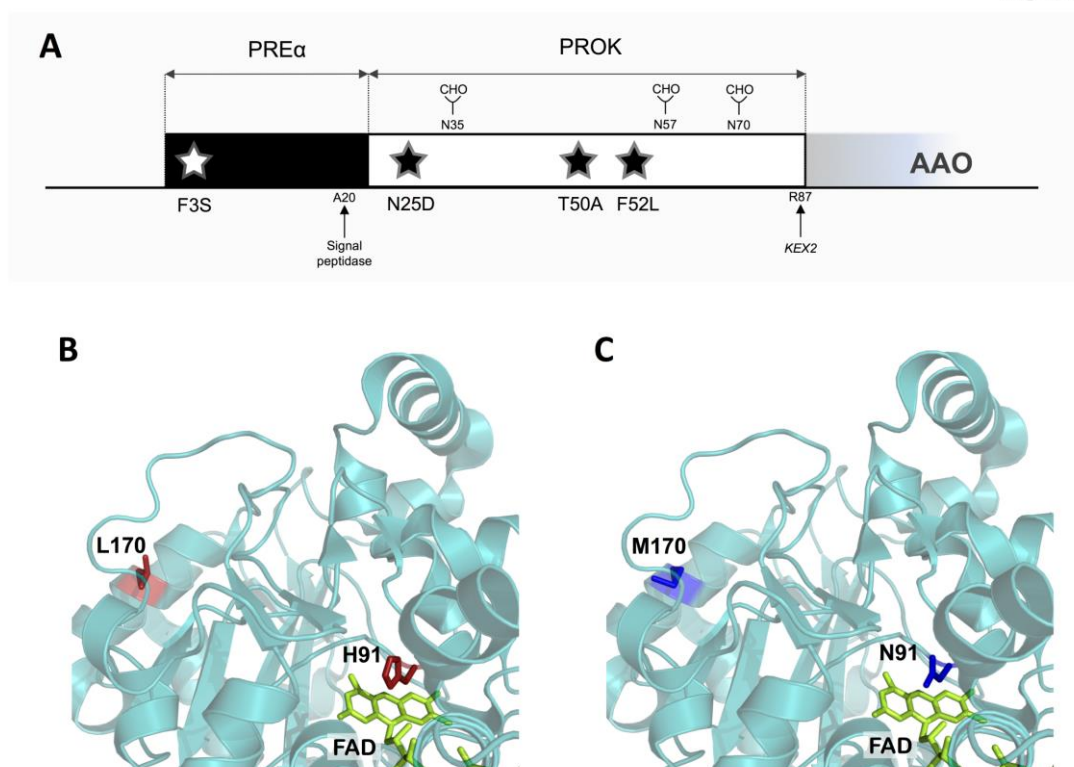
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Figure 1



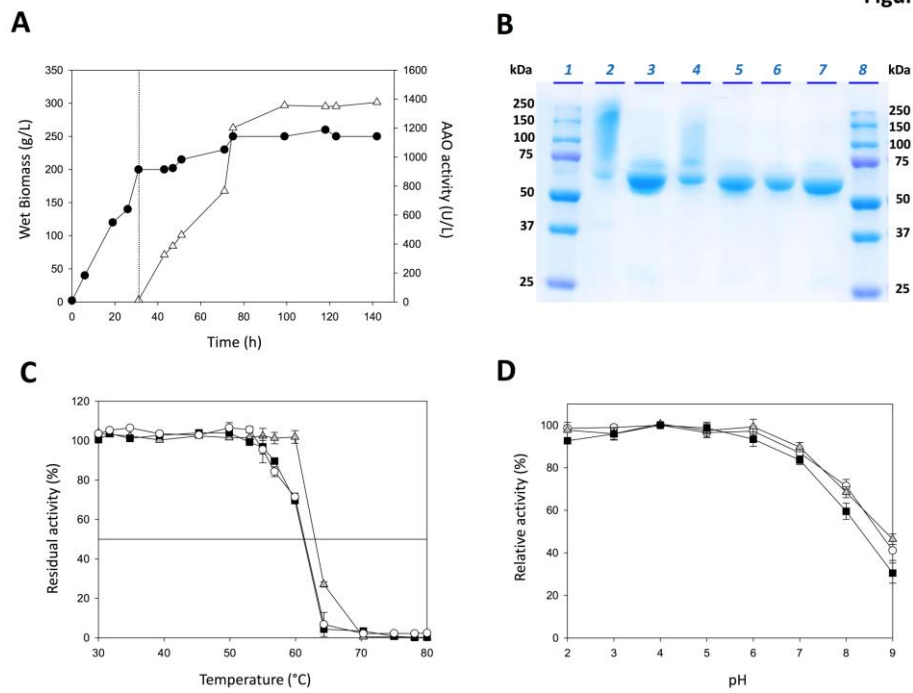
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Figure 2

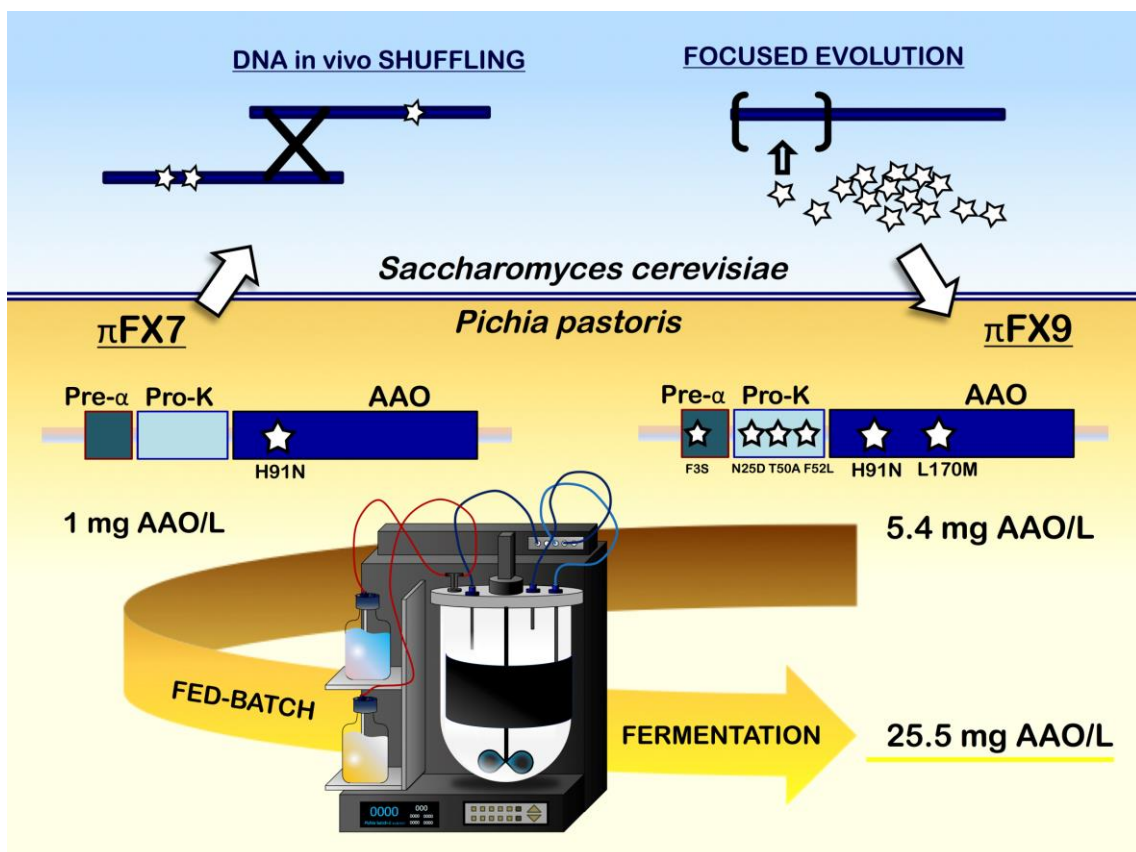


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Figure 3



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