

26 **Industrial relevance**

27 The growing demands for natural and nutritious foods have promoted the
28 development of preservation technologies to ensure consumer safety and to preserve the
29 original nutritional and organoleptic characteristics of the food. Among the emerging
30 technologies, microwave heating has shown great potential for the continuous
31 pasteurization of fluid foods offering rapid volumetric heating, lower surface
32 temperatures and possible enhanced effects. The results of this study shows that
33 microwave pasteurization of apple juice is a promising technology to enhance microbial
34 safety.

35 **Keywords**

36 Apple juice • *Listeria monocytogenes* • *Escherichia coli* • microwave heating •
37 conventional heating • inactivation kinetics.

38 **Highlights**

- 39 • Conventional and microwave thermal treatments of apple juice were evaluated.
- 40 • Weibull parameters for inactivation of *E. coli* and *L. monocytogenes* were estimated.
- 41 • FDA standard of 5-log₁₀ was reached in microwave and conventional conditions.
- 42 • Microbial inactivation showed to be more efficient under microwave heating.

43

44 **1 Introduction**

45

46 Fruit juices are not traditionally recognized as vehicles for foodborne illness due
47 to their inherent acidity, which inhibits the multiplication of most pathogens.
48 Nevertheless, outbreaks involving *Escherichia coli* O157:H7 associated with the
49 consumption of apple juice and apple cider led the FDA to require all fruit juice
50 processors to implement a Hazard Analysis and Critical Control Points (HACCP) plan

51 (CDC, 1996; FDA, 2004). The final critical control point demands a system that
52 achieves at least a 5- \log_{10} reduction of the most resistant organism of public health
53 concern (FDA, 2004). *E. coli* O157:H7 and *Listeria monocytogenes* were identified as
54 pertinent bacterial pathogens for juices safety by the National Advisory Committee on
55 Microbiological Criteria for Foods (FDA, 1997).

56 Currently, conventional pasteurization, combined with other preservation
57 methods, ensures microbiological food safety and stable shelf life. However,
58 commercial pasteurization of apple juice involves heat treatment at 77 - 88 °C for 25 -
59 30 s, which results in detrimental changes in the sensory and nutritional qualities of the
60 juice (Tajchakavit et al., 1998).

61 Alternative technologies are required to satisfy the growing demand for
62 minimally processed foods. Microwave heating has entered the field of food science for
63 various industrial purposes, such as dehydration, cooking, blanching, sterilization and
64 pasteurization. Continuous flow microwave heating is an emerging application for
65 pasteurizing liquid foods. The use of microwave heating instead of conventional heat
66 exchangers offers some advantages for thermal processing, such as rapid volumetric
67 heating, lower equipment surface temperature, and possible preservation of food quality
68 (Heddleson and Doores, 1994; Chandrasekaran et al., 2013).

69 Various studies investigated the interaction of microwave radiation with
70 biological systems, specifically microbial inactivation in fluid foods (Salazar-González
71 et al., 2012; Benlloch-Tinoco et al., 2014; Pina-Pérez et al., 2014; Sung and Kang,
72 2014). However, the literature available regarding microbial inactivation in apple juice
73 by microwave heating is scarce. The studies published in this topic include the
74 inactivation of *Saccharomyces cerevisiae* and *Lactobacillus plantarum* during
75 continuous-flow microwave heating (Tajchakavit et al., 1998), the effect of microwave

76 pasteurization in apple juice inoculated with *E. coli* (Cañumir et al. 2002) and the
77 continuous-flow microwave pasteurization for inactivation of *E. coli* in apple cider
78 (Gentry and Roberts, 2005). Moreover, there are no comparative studies regarding the
79 achieved lethality considering similar treatment conditions for conventional and
80 microwave heating.

81 Some authors have carried out studies to establish the target microorganism for
82 the pasteurization of apple juice using other emerging technologies, such as ultraviolet
83 light, combined heat and ultraviolet light and gaseous ozone (Guerrero-Beltrán and
84 Barbosa-Cánovas, 2005; Gabriel and Nakano, 2009; Choi et al., 2012; Gouma et al.,
85 2015). The 5- \log_{10} reduction of the most resistant pathogen depends on the specific
86 processing conditions and technology.

87 The purposes of this study were: 1) to investigate the influence of microwave
88 heating on the inactivation of *E. coli* O157:H7 and *L. monocytogenes* in apple juice; 2)
89 to describe the inactivation kinetics of these microorganisms; 3) to compare the
90 effectiveness of microwave and conventional heating in the inactivation rate of
91 foodborne pathogens in apple juices.

92

93 **2 Materials and methods**

94

95 2.1. Bacterial strain, culture preparation and inoculation

96 *E. coli* O157:H7 (CECT 4972, isolated from human diarrhea, Innsbruck,
97 Austria) and *L. monocytogenes* (CECT 4032, isolated from a case of meningitis after
98 eating soft cheese, Colindale, London, UK) were provided by the Spanish Type Culture
99 Collection and prepared according to the method described by Benlloch-Tinoco et al.
100 (2014). The stock culture (1 mL of cell suspension with supplemental 1 mL glycerol

101 20%, v/v, added after the stationary phase was reached) was stored frozen at $-80\text{ }^{\circ}\text{C}$.
102 One milliliter of unfrozen *E. coli* O157:H7 and *L. monocytogenes* were cultured in 500
103 mL of Tryptic Soy Broth (TSB, Scharlab Chemie S.A., Barcelona, Spain) at $37\text{ }^{\circ}\text{C}$ for
104 24 h under constant agitation (200 rpm) to reach the stationary growth stage. The
105 cultures were centrifuged twice using an Avanti J-26XP centrifuge (Beckman Coulter,
106 Palo Alto, USA) with a rotor JLA-16.250 (Beckman Coulter, Palo Alto, USA) at 4000
107 g, $4\text{ }^{\circ}\text{C}$ for 15 min, and the pellets were resuspended in 50 mL of TSB. The cells were
108 dispensed in cryogenic vials T310-2A (Simport, Saint-Mathieu-de-Beloeil, Canada)
109 adding 2 mL of TSB with glycerol 20% (v/v) in a 1:1 ratio, and stored at $-80\text{ }^{\circ}\text{C}$ until
110 used for the inactivation kinetics studies. For *E. coli* and *L. monocytogenes* inoculum
111 enumeration, samples were thawed and it was proceeded according to Section 2.4. The
112 approximate concentration in cultures of *E. coli* and *L. monocytogenes* were $4\cdot 10^9 \pm$
113 $7\cdot 10^8\text{ CFU}\cdot\text{mL}^{-1}$ and $7\cdot 10^9 \pm 9\cdot 10^8\text{ CFU}\cdot\text{mL}^{-1}$, respectively.

114 The experiments were performed using a commercial apple juice (Don Simon, J.
115 García Carrión S.A., Spain) with a pH of 3.5 and soluble solids of 12.4 °Brix ($25\text{ }^{\circ}\text{C}$)
116 purchased at a local market in Valencia (Spain). The inoculums of *L. monocytogenes*
117 and *E. coli* (2 mL) were thawed and mixed in the apple juice (8 mL) to obtain initial
118 viable counts of $10^6\text{ CFU}\cdot\text{mL}^{-1}$.

119

120 2.2. Conventional thermal treatment

121 A glass capillary tube (Blaubrand®, BRAND GMBH), previously sterilized at
122 $240\text{ }^{\circ}\text{C}$ for 24 h, was filled with 200 μL of the inoculated apple juice. Both ends were
123 immediately sealed with oxygen flame. The tube was carefully sealed to avoid the
124 heating of the inoculated apple juice. The conventional thermal treatment was carried
125 out by immersion of the capillary tubes for different time intervals (selected between 10

126 and 180 s) in a circulating thermostatic Haake DC5 water bath (Thermo Fischer
127 Scientific, Waltham, USA), which was kept at 55, 60, 65 or 70 °C. Each combination of
128 the temperature and time (sets of ten capillaries) was conducted in two repetitions and
129 both repetitions were considered for estimating the inactivation kinetic parameters.
130 After the processing time, the capillary tubes were immersed in ice-water bath until the
131 apple juice reached 25 °C. A type-T thermocouple (Control Company, Webster, USA)
132 connected to a data logger LZ64 (Digitron instrumentation, Cambridge, UK) was
133 inserted into one capillary tube with apple juice to obtain the average time-temperature
134 profile of the set of ten capillaries. Prior to the thermal treatment, all samples were kept
135 at 25 °C to standardize the come-up time (CUT).

136

137 2.3. Microwave thermal treatment

138 Batch microwave processing was performed using an adapted microwave oven
139 (model 3038GC, Norm, China) at 2450 MHz with a turntable plate. A fiber-optic
140 temperature probe CR/JP/11/11671 (Optocom, Dresden, Germany) was placed in a
141 borosilicate glass test tube (6-mm inner diameter and 68-mm length) with 1 mL of
142 inoculated apple juice, with the tip at the center of the liquid, and connected to a
143 datalogger FOTEMP1-OEM (Optocom, Dresden, Germany) to continuously record the
144 time-temperature history. The test tube was placed vertically at the center of the
145 microwave cavity. All the samples started at an initial temperature around 25 °C and
146 were then heated in the microwave oven. Once the processing time was achieved, the
147 test tube was quickly removed from the cavity and inserted in an ice-water bath. Since
148 the fiber-optic probe was fixed in the oven, the temperature data during cooling was not
149 recorded. For the inactivation study, the inoculated apple juice was subjected in

150 triplicates to microwave heating at four different power levels (1000 W, 800 W, 600 W
151 and 400 W) and different heating times between 50 and 390 s.

152

153 2.4. Enumeration of survivors

154 Right after microwave and conventional treatments, sample aliquots were
155 diluted in duplicate with sterile 1%-peptone water (Scharlab Chemie S.A., Barcelona,
156 Spain), and 0.1 mL of diluent spread-plated onto Tryptic Soy Agar (TSA, Scharlab
157 S.A., Barcelona, Spain). The plates were then incubated at 37 °C for 24 h for *E. coli* and
158 48 h for *L. monocytogenes*. Afterwards, the counting step was performed. The reduction
159 of viable cell count was expressed as the decimal logarithm of the quotient of the treated
160 (N) and untreated samples (N_0).

161

162 2.5. Absorbed microwave power

163 The mean of the volumetric microwave power absorption, P'_{abs} (W/mL), was
164 calculated from the temperature rise of the 1.0 mL sample from $T_{initial}$ to T_{final} using
165 Eq. (1):

$$P'_{abs} = \frac{m \cdot c_p \cdot (T_{final} - T_{initial})}{t \cdot (1.0 \text{ mL})} \quad (1)$$

166 where m is the mass of the sample (kg), c_p is the average specific heat (J/°C·kg) of the
167 mixture of apple juice (0.8 mL), TSB (0.1 mL) and glycerol (0.1 mL) and t is the
168 microwave processing time (s). In order to estimate the average specific heat of the
169 sample, the mixture of apple juice and TBS (0.8 + 0.1 mL) was assumed to have the
170 density and specific heat of apple juice reported by Constenla et al. (1989), while the
171 density and specific heat of glycerol (0.1 mL) came from Cheng (2008) and Righetta et
172 al. (1998), respectively. The specific heat estimate was obtained as:

$$c_p = \frac{(0.9) \cdot \rho_{apple} \cdot c_{p,apple} + (0.1) \cdot \rho_{glycerol} \cdot c_{p,glycerol}}{(0.9) \cdot \rho_{apple} + (0.1) \cdot \rho_{glycerol}} \quad (2)$$

173 where densities (ρ_{apple} , $\rho_{glycerol}$) and specific heats ($c_{p,apple}$, $c_{p,glycerol}$) were
 174 calculated at the average temperature of the sample.

175

176 2.6. Modeling of survival curves

177 The inactivation Weibull model in decimal logarithmic form (Eq. (3)) was fitted
 178 to the data of surviving population for conventional and microwave thermal treatments
 179 *versus* processing time through non-linear regression (Statgraphics Centurion XV
 180 version 15.2.11, StatPoint Technologies, Warrenton, USA) to obtain a mathematical
 181 description of the survival curves:

$$\log(S) = -\left(\frac{t}{\alpha}\right)^\beta \quad (3)$$

182 where S is the survival ratio (N/N_0) after processing time t , α is the scale parameter (s^{-1})
 183 ¹) that represents the time of the first decimal reduction and β is the shape parameter (-)
 184 (Mafart et al., 2002). The goodness of the fit was assessed from the adjusted coefficient
 185 of determination (R_{adj}^2), the mean squared error for the prediction of $\log(S)$ (MSE) and
 186 the parity charts of predicted *versus* experimental survival ratios.

187 Analogous to the Bigelow z value, van Boekel (2002) shows that the
 188 temperature dependence of the scale parameter (α) can be modeled by a logarithmic
 189 relationship as given by Eq. (4):

$$\alpha = a \cdot 10^{-bz'} \quad (4)$$

190 where a and b are parameters and $z' = 1/b$ is the temperature increase necessary to
 191 reduce the scale parameter by 90%. Since the conventional treatments in hot water bath
 192 could be assumed isothermal, Eq. (4) was fitted to the α *versus* T data to obtain the z'
 193 value for *E. coli* and *L. monocytogenes* inactivation in apple juice.

194

195 2.7. Comparing conventional and microwave treatments on *E. coli* and *L.*
196 *monocytogenes* inactivation

197 Unlike the conventional heat treatments using the hot water bath, the microwave
198 treatments were not isothermal. In order to compare the inactivation of *E. coli* and *L.*
199 *monocytogenes* in apple juice using conventional and microwave heating, the adjusted
200 Weibull model for conventional heating was used to predict the survival ratio for the
201 recorded temperature history $T(t)$ of the microwave treatments, which were compared
202 to the experimental values.

203 Peleg et al. (2005) showed that the momentary inactivation rate for the Weibull
204 model derived from Eq. (3) is:

$$\left(\frac{d\log(S)}{dt}\right)_T = -\frac{\beta}{\alpha} \cdot (-\log(S))^{\frac{\beta-1}{\beta}} \quad (5)$$

205 which can be numerically integrated to provide the survival rate for a non-isothermal
206 treatment (Chen et al., 2007):

$$\log(S) = -\sum_i \frac{\beta_i}{\alpha_i} \cdot (-\log(S_{i-1}))^{\frac{\beta_i-1}{\beta_i}} \cdot \Delta t \quad (6)$$

207 where Weibull parameters α and β are evaluated at the momentary temperature T_i of
208 the time temperature profile and Δt is the time increment. An initial value $\log(S_0) =$
209 1×10^{-6} was used as suggested by Peleg and Pechina (2000).

210 Using the recorded time temperature profile of the microwave treatments and the
211 adjusted Weibull parameters for conventional heating, Eq. (6) provided the predicted
212 survival ratio, $\log S_{pred}$, for that given treatment. This result was compared with the
213 experimental survival ratio of the microwave treatment, $\log S_{mw}$. If non-thermal effects
214 of the microwaves in the microbial inactivation are present, then the predicted survival

215 ratio would be significantly lower than the experimental value, assuming that the kinetic
216 model for conventional heating is well adjusted and provides a reliable prediction.

217

218 **3. Results and discussion**

219

220 3.1. Time-temperature profiles of apple juice

221 Some of the recorded time-temperature histories of apple juice samples
222 inoculated with *E. coli* and *L. monocytogenes* during the processing time under
223 conventional and microwave heating are shown in Fig. 1. Results from the microwave
224 heating of pure apple juice showed that the inoculation of *E. coli* or *L. monocytogenes*
225 did not result in significantly different time-temperature profiles, indicating that the
226 thermal and dielectric properties of the mixture are close to those of the apple juice.

227 The capillary tube subjected to conventional heating conditions had a come-up
228 time (CUT) of 8 s and come-down time (CDT) of 6 s, making the contribution of
229 heating and cooling rates insignificant when compared with the holding times, which
230 were between 50 and 390 s. Therefore, isothermal conditions were assumed for
231 conventionally treated samples.

232 The mechanism of microwave heating, conversion of electromagnetic energy
233 into heat by selective absorption and dissipation, is different from conventional heating
234 through conduction and convection (Dorantes-Alvarez and Parada-Dorantes, 2005).
235 Microwaves generate heat constantly and, consequently, there is no holding period
236 (Tajchakavit et al., 1998; Brewer, 2005; Benlloch-Tinoco et al., 2014). The time-
237 temperature profiles during the microwave treatment presented almost linear heating
238 ramps at different rates depending on the power levels (Fig. 1). Some tests were carried
239 out to evaluate the contribution of the CDT to the time-temperature profile, and the

240 CDT (less than 14 s) was verified to be insignificant when compared with the heating
241 time.

242 The volumetric microwave power absorption of the samples (P'_{abs}) was
243 calculated from Eq. (1) and it was linearly correlated with the power setting (P_{input} =
244 400, 600, 800 and 1000 W) through Eq. (7) ($R^2 = 0.961$, P'_{abs} in W/mL and P_{input} in
245 W). The power absorbed by the sample, $P'_{abs} \cdot (1.0 \text{ mL})$, was smaller than the power
246 setting (P_{input}) because most of the power was lost due to the reflection in the
247 microwave cavity and the small dimensions of the sample. However, the linear trend of
248 the time-temperature profiles (Figs. 1B and 1D) indicate that the energy absorbance was
249 constant during the heat treatments.

$$P'_{abs} = (8.65 \cdot 10^{-7}) \cdot P_{input}^2 + (7.06 \cdot 10^{-4}) \cdot P_{input} \quad (7)$$

250

251 3.2. Inactivation kinetics by conventional and microwave treatments

252 The adjusted parameters with their standard deviations and fit criteria are
253 presented in Tables 1 and 2. For conventional heating, the model was fitted for each
254 processing temperature (isothermal treatment), while the model was fitted for each
255 power level for microwave processing (non-isothermal treatment). However, the power
256 absorbed by the sample depends on the shape and dimensions of the sample and
257 microwave cavity. Consequently, the specific power absorption (P'_{abs} from Eq.(7)) is
258 also included in Table 2. Results are valid assuming uniform temperature distribution.

259 The goodness of fit for the Weibull model was described by the R_{adj}^2 and MSE
260 values. The adequacy of the Weibull model to represent *E. coli* and *L. monocytogenes*
261 inactivation in apple juice under conventional and microwave treatments can be seen in
262 Figs. 2 and 3 through the parity charts of predicted microbial reduction by the adjusted
263 model ($\log S_{mod}$) versus that of experimental microbial reduction ($\log S_{exp}$).

264 Figs. 2A, 2C, 3A and 3C show the adjusted inactivation curves of the Weibull
265 model for the processing conditions. For both microorganisms, the number of survivors
266 dropped over time for a given temperature or power. For *E. coli* under conventional
267 heating, no inactivation was detected at temperatures under 55 °C, whereas it was
268 “completely” inactivated, *i.e.*, under detection levels, for at least 10 s at temperatures
269 above 70 °C. For *L. monocytogenes*, the safety criterion given by the FDA (2004) was
270 satisfied by conventional treatment at 55 °C for 180 s. This criterion requires that at least
271 a 5- \log_{10} reduction of the most resistant organism of public health concern must be
272 achieved. In the case of microwave heating, the FDA standard was reached when
273 processing times were higher than 110 s for *E. coli* and 130 s for *L. monocytogenes* at a
274 power setting of 1000 W ($P'_{abs} = 1.57$ W/mL).

275 Gentry and Roberts (2005) reported that a 5- \log_{10} reduction of *E. coli* 25922 was
276 obtained in apple cider using a continuous-flow microwave system at 2000 W for about
277 270 s (mean residence time). In the work by Picouet et al. (2009), after a treatment by
278 microwave radiation at 652 W and 35 s, 7- \log_{10} reduction of *L. innocua* in apple purée
279 was achieved. However, they observed a 1- \log_{10} reduction of *E. coli* O157:H7 after 35 s
280 at the same power of 652 W. As observed by other authors, microbial inactivation was
281 faster for increasing microwave power (Fig. 3) (Cañumir et al., 2002; Sung and Kang,
282 2014; Valero et al., 2014; Benlloch-Tinoco et al., 2014).

283 Even though the classical inactivation model with D and z values (Bigelow,
284 1921) is widely accepted and practiced to describe the inactivation of microorganisms
285 (Tajchakavit et al., 1998; Gentry and Roberts, 2005; Benlloch-Tinoco et al., 2014) and
286 enzymes (Matsui et al., 2008; Riener et al., 2008; Aguiar et al., 2012), microbial
287 survival behavior can change according to the conditions and can be better described by
288 the Weibull model in Eq. (3) (van Boekel, 2002; Surowsky et al., 2014; Rojas et al.,

289 2017). In our work, both microorganisms in the apple juice samples exposed to the
290 microwave energy as well as the conventional heating showed semi-logarithmic
291 survival curves with upward ($\beta < 1$) or downward ($\beta > 1$) concavities (Figs. 2 and 3).
292 The downward concavities in Fig. 3 are consistent with the temperature increase that
293 occurs during microwave treatment (Fig. 1B, 1D), which increases the inactivation rate.

294 The data in Tables 1 and 2 show that, for both microorganisms treated with
295 conventional or microwave heating, the α values presented a negative log-linear
296 dependence with temperature or power level (Eq. (4)), while the β values for *E. coli* and
297 *L. monocytogenes* inactivation do not seem to indicate a clear trend with the temperature
298 or power level.

299 Peleg and Pechina (2000) related changes in the curvature of survival curves to
300 physiological effects. A concave upward curve indicates that the most sensitive
301 members of the population are inactivated first and the more resistant ones remain. A
302 downward concavity may be explained by accumulated damage to the microbial
303 population, which leads the surviving cells to become increasingly more vulnerable.
304 Table 2 and Fig. 2A indicate that the *E. coli* inactivation curves have an upward
305 concavity ($\beta < 1$) indicating the presence of different heat resistances in the population.
306 On the other hand, the concavity of the inactivation curves of *L. monocytogenes*
307 depended on the temperature as can be seen in Table 2 and in Fig. 2C. For longer
308 processing times at the lowest temperature (55 °C), the effect of accumulated damage
309 could be observed, while for shorter times at the highest temperature (70 °C), the effect
310 of thermal resistance variation in the population was more prominent.

311 The temperature dependence on the α parameter for conventional treatment was
312 properly modeled as described in Eq. (4). The z' values and the α values at a reference
313 temperature of 70 °C of *E. coli* and *L. monocytogenes* in apple juice are shown in Table

314 3. The z' value of *E. coli* is similar to that found in the literature; Enache et al. (2001)
315 compared the thermal resistance of seven serotypes with three strains in apple juice (pH
316 3.7) and the z value for each strain of *E. coli* O157:H7 ranged between 4.9 and 5.5 °C.
317 The heat resistance of *L. monocytogenes* (z' value) determined in our study was also in
318 accordance with Mazzota (2001), who reported a z value of 6.3 for *L. monocytogenes* in
319 the stationary phase in apple juice (pH 3.9).

320

321 3.3. Comparing conventional and microwave treatments on *E. coli* and *L.*
322 *monocytogenes* inactivation

323 As explained in section 2.7, Eq. (6) was used to predict the final survival ratio of
324 *E. coli* and *L. monocytogenes* based on the recorded time temperature profiles of
325 microwave processing at four power levels (examples in Figs. 1B and 1D) using the
326 Weibull kinetic parameters determined for conventional heating (Tables 1 and 3). The
327 isothermal treatment was considered the reference treatment for the nature of the
328 survival of microorganisms. Since the dependence of β with temperature was not clear,
329 it was decided to use a piecewise linear approximation of the data in Table 1. The scale
330 parameter was calculated for each temperature using a modified form of Eq. (4) using
331 the z' and $\alpha_{70^\circ\text{C}}$ values from Table 3:

$$\alpha = \alpha_{70^\circ\text{C}} \cdot 10^{\left(\frac{70^\circ\text{C}-T}{z'}\right)} \quad (8)$$

332 Fig. 4 shows the parity charts of the survival ratio predicted for the microwave-
333 treated samples based on the kinetics adjusted for conventional heating ($\log S_{pred}$)
334 versus the experimental survival ratio after microwave processing ($\log S_{mw}$) for *E. coli*
335 (Fig. 4A) and *L. monocytogenes* (Fig. 4B). If the inactivation of microorganisms were
336 similar under conventional and microwave heating, the points would be distributed
337 evenly around the 45° dotted line as in Figs. 2B and 2D; however, results show that for

338 most of the microwave experiments, the microbial inactivation was more efficient than
339 predicted (18 out of 28). The largest differences in survival ratio were observed in the
340 experiments with shorter duration of microwave exposure. Moreover, larger differences
341 were obtained for experiments with *E. coli* than with *L. monocytogenes*.

342 The distinction between the thermal and non-thermal effects during microwave
343 heating of foods on pathogenic microorganisms is a controversial topic, since
344 conflicting scientific viewpoints can be found in the literature (Tajchakavit et al., 1998;
345 Anantheswaran and Ramaswamy, 2001; Shazman et al., 2007; Shaheen et al., 2012;
346 Valero et al., 2014; Benlloch-Tinoco et al., 2014). Results from this work suggest that
347 microwave heating can be more effective for the inactivation of *E. coli* and *L.*
348 *monocytogenes* in apple juice than conventional thermal processing. There seems to
349 exist enhancement effects associated with microwave radiation.

350 In a review about the specific effects of microwave radiation on bacterial cells,
351 Shamis et al. (2012) report results from the literature that suggests that microwaves
352 enhance enzyme and bacterial inactivation in comparison with conventional heating.
353 Regarding enzyme inactivation, the hypothesis of instantaneous temperature effect may
354 be proposed: some molecules can receive microwave energy at a higher rate than can be
355 dissipated, leading to a high instantaneous temperature that cannot be directly measured.
356 Since this effect is thermal in nature, authors suggest that the expression “specific
357 microwave effect” is more suitable than “non-thermal effect”. For the case of bacterial
358 inactivation, besides the enzyme activity reduction, there are evidences that microwaves
359 may increase the porosity of the cell membrane, thus changing their morphology.

360 Microwave radiation demonstrated to be a promising technology to enhance the
361 microbial safety of pasteurized and sterilized foods. Therefore, further studies should
362 focus on the development of industrial equipment for scaling up microwave

363 pasteurization processes thus allowing the development of products and applications
364 (Orsat and Raghavan, 2005).

365

366 **4 Conclusion**

367 Microwave heating presents a promising alternative for conventional heating
368 since it is effective against *E. coli* and *L. monocytogenes* in apple juice (inactivation up
369 to 5-log₁₀ cycles). For most of the microwave treated samples, the inactivation was
370 higher than that predicted from the time temperature history. However, to confirm the
371 existence of these enhancement effects, obtaining identical time-temperature profiles by
372 conventional and microwave treatment will be required, besides comparing the survival
373 ratios. Additionally, future works are necessary to evaluate the quality and safety of
374 apple juice pasteurized by microwave heating, for example, the study enzyme
375 inactivation since they are usually more resistant than pathogenic and spoilage
376 microorganisms.

377

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386

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513 **FIGURE CAPTIONS**

514

515 **Fig. 1.** Examples of time-temperature histories of apple juice samples inoculated with *E.*
516 *coli* during conventional and microwave treatments (A and B, respectively), and for
517 samples inoculated with *L. monocytogenes* during conventional and microwave
518 treatments (C and D, respectively).

519

520 **Fig. 2.** *E. coli* (A) and *L. monocytogenes* (C) survival curves under conventional
521 thermal treatment (experimental data and adjusted Weibull model curves) and the parity
522 chart of *E. coli* (B) and *L. monocytogenes* (D) between experimental and model
523 predicted inactivation data.

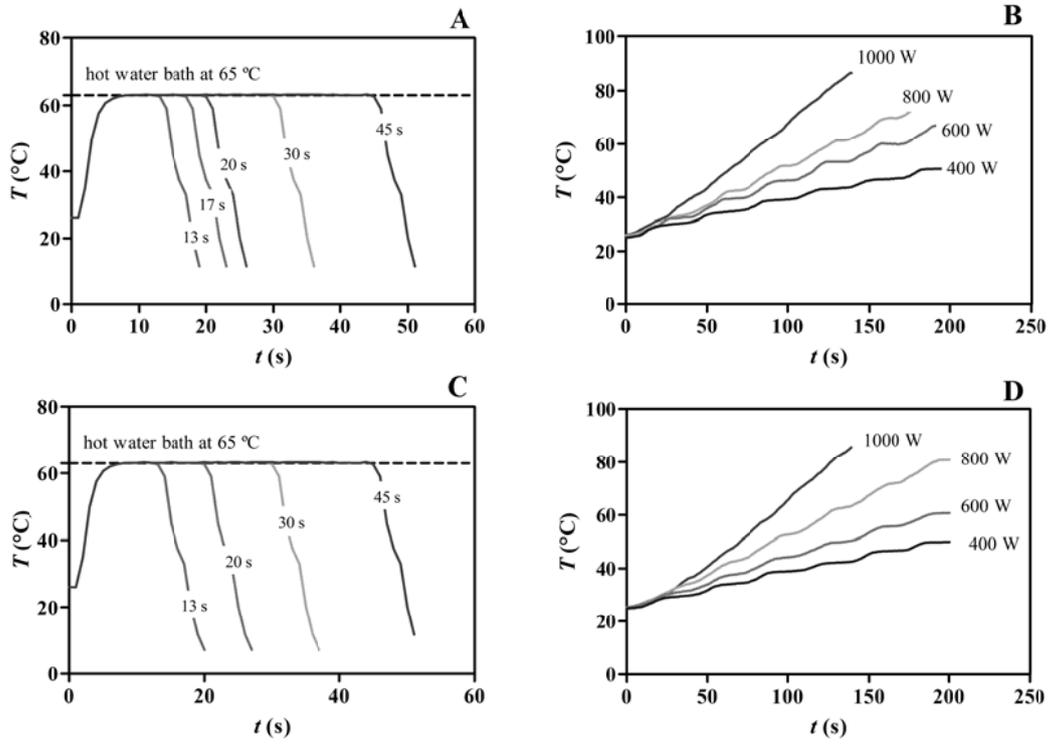
524

525 **Fig. 3.** Survival curves for *E. coli* (A) and *L. monocytogenes* (C) after microwave
526 thermal treatment (experimental data and adjusted Weibull model curves) and the parity
527 chart of *E. coli* (B) and *L. monocytogenes* (D) between experimental and model
528 predicted inactivation data.

529

530 **Fig. 4.** The survival ratio of *E. coli* (A) and *L. monocytogenes* (B) by microwave
531 treatment ($\log S_{mw}$) versus the survival ratio predicted from the time temperature
532 history and the adjusted Weibull model for conventional heating ($\log S_{pred}$). The 45°
533 dashed lines indicate equivalent survival ratio.

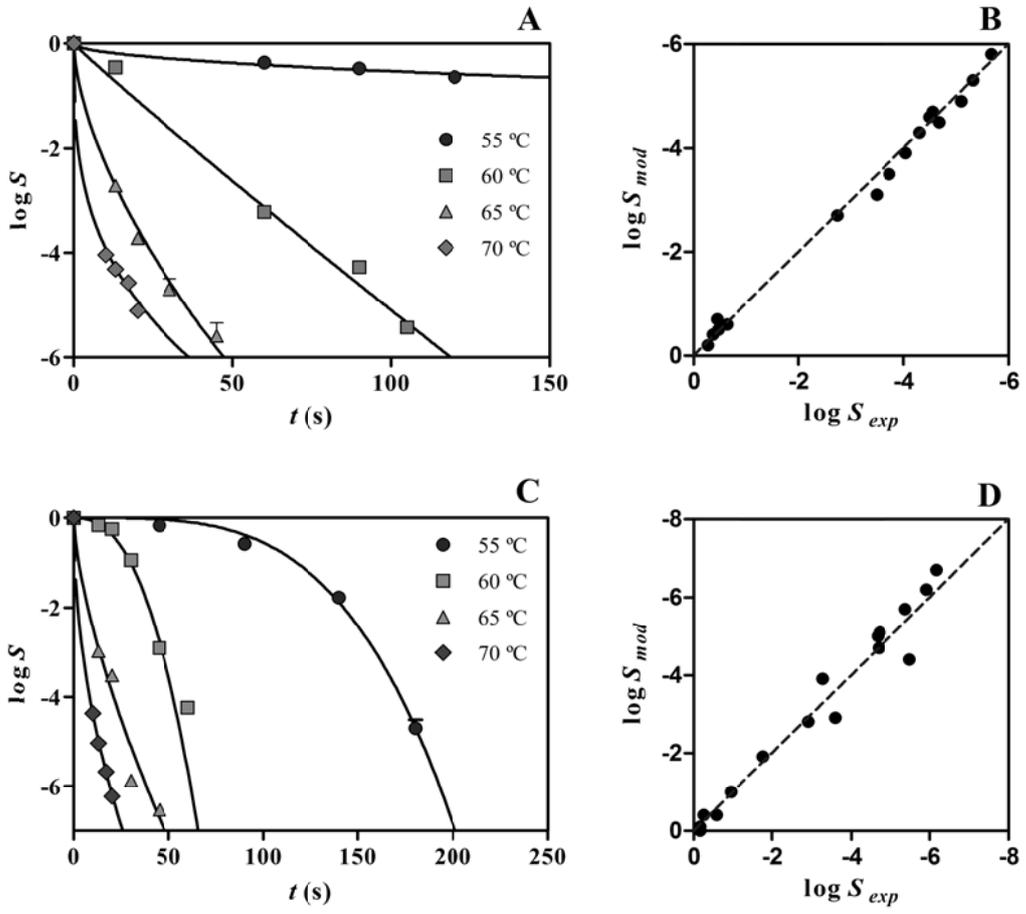
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539 **FIGURE 2**

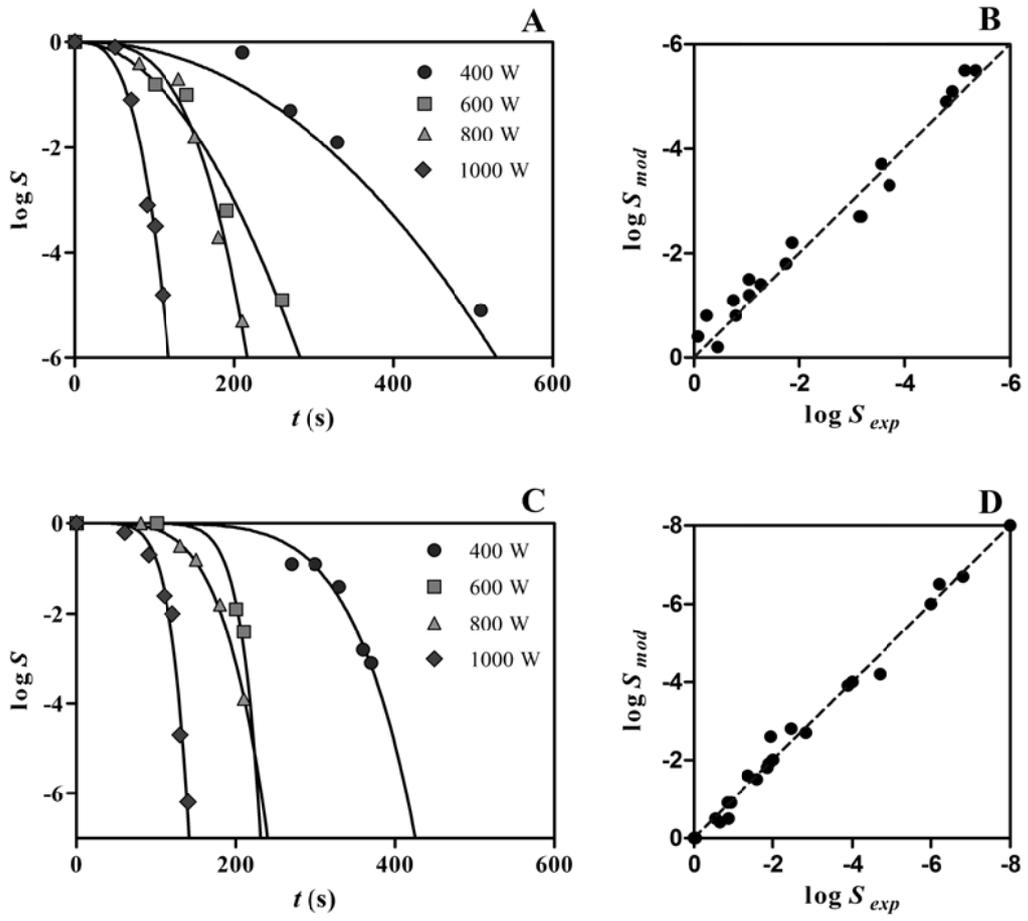


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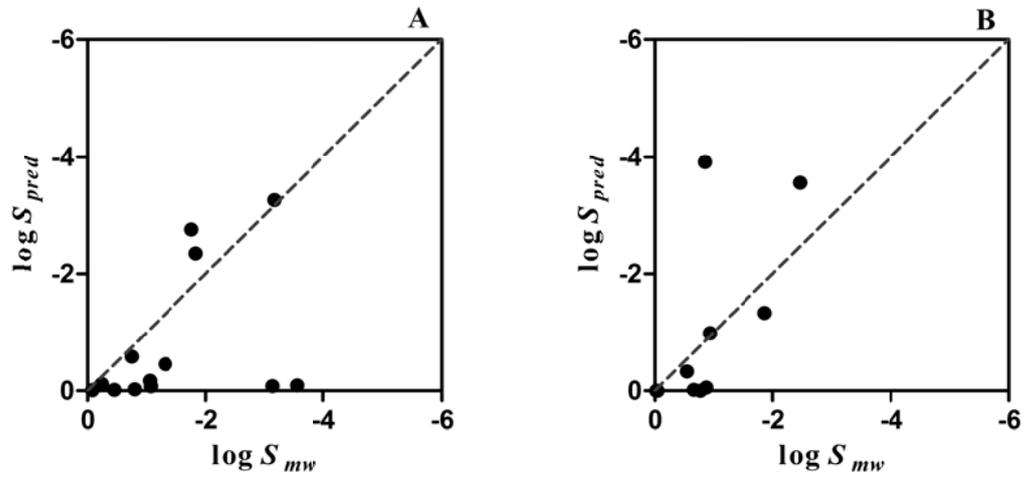
543 **FIGURE 3**



544

545

546 **FIGURE 4**



547

548

548 **Table 1.** Adjusted Weibull kinetic parameters for inactivation of *E. coli* and *L.*
 549 *monocytogenes* in apple juice under conventional heating at different temperatures

<i>T</i> (°C)	<i>E. coli</i>				<i>L. monocytogenes</i>			
	α (s ⁻¹)	β (-)	<i>MSE</i>	<i>R</i> _{adj} ²	α (s ⁻¹)	β (-)	<i>MSE</i>	<i>R</i> _{adj} ²
55	354 ± 24	0.51 ± 0.01	0.0052	99.68	117.8 ± 3.2	3.64 ± 0.36	0.0213	99.27
60	18.23 ± 0.89	0.96 ± 0.03	0.0710	98.49	29.84 ± 0.8	2.47 ± 0.50	0.0223	98.71
65	2.56 ± 0.53	0.61 ± 0.03	0.0539	98.22	2.69 ± 0.29	0.68 ± 0.02	0.1230	97.95
70	0.158 ± 0.072	0.33 ± 0.03	0.0129	99.65	0.53 ± 0.15	0.50 ± 0.04	0.0073	99.89

550

551

552 **Table 2.** Adjusted kinetic parameters for inactivation of *E. coli* and *L. monocytogenes*
 553 in apple juice subjected to microwave heating at four power levels

<i>P</i> (W)	<i>P'</i> _{abs} (W/mL)	<i>E. coli</i>				<i>L. monocytogenes</i>			
		α (s ⁻¹)	β (-)	<i>MSE</i>	<i>R</i> ² _{adj}	α (s ⁻¹)	β (-)	<i>MSE</i>	<i>R</i> ² _{adj}
400	0.42	228.9 ± 7.2	2.13 ± 0.11	0.1091	96.53	302.8 ± 5.3	5.73 ± 0.09	0.1783	95.78
600	0.74	114.7 ± 11.4	1.99 ± 0.29	0.1009	97.41	188.6 ± 1.8	9.60 ± 0.51	0.0067	99.65
800	1.12	126.5 ± 3.6	3.34 ± 0.31	0.1339	95.15	155.3 ± 0.7	4.48 ± 0.21	0.1120	97.20
1000	1.57	65.3 ± 2.9	3.06 ± 0.37	0.4265	88.59	102.8 ± 2.5	6.08 ± 0.47	0.0626	91.66

554

555

556 **Table 3.** *E. coli* and *L. monocytogenes* z' and $\alpha_{70^\circ\text{C}}$ values obtained in apple juice
557 treated by conventional heating

	z' ($^\circ\text{C}$)	$\alpha_{70^\circ\text{C}}$ (s)	MSE	R_{adj}^2
<i>E. coli</i>	4.56 ± 0.25	0.161 ± 0.042	0.1093	98.88
<i>L. monocytogenes</i>	6.17 ± 0.23	0.511 ± 0.073	0.0983	98.48

558

559