



Electrocatalytic Pt-embedded ZIF-8 on nanocellulose-based flexible conductive electrodes for hydrogen evolution reaction

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Abstract Hydrogen fuel cell is a clean green energy device, but it is demanded valid conjugation between catalyst and substrate for generating the effective active site and ion transfer. Here, the hydrogen evolution reaction (HER) efficiency was investigated using Pt-embedded zeolitic imidazolate framework-8 (Pt@ZIF-8) electrocatalysts. Although the Pt content was only 2.8 wt%, the efficiency was equivalent to the reference catalyst (~40 wt% Pt in carbon); The reduction of Pt content improves cost performance and saves resources, making fuel cells more affordable. Furthermore, a flexible substrate consisting

of electroconductive sulfonated polypyrrole and TEMPO-oxidized cellulose nanofiber film was found to be effective for embedding Pt@ZIF-8 electrocatalysts, acting as flexible and lightweight electrodes. Moreover, the generated hydrogen easily diffuses through the porous cellulose film. The fabricated electrocatalytic substrates are promising composite materials for hydrogen fuel cells, which consume significantly small amount of noble metal, making the renewable energy production more reasonable.

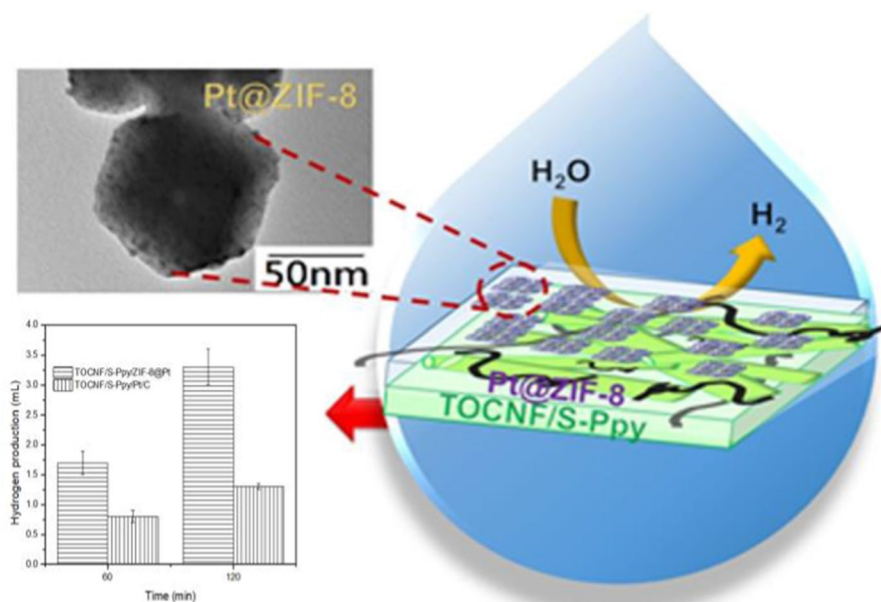
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Graphical abstract



Keywords Hydrogen production · Composite electrode · Caged nanoparticle · Cellulose nanofiber-based flexible substrate · Polypyrrole sulfonation

Introduction

The global climate crisis is mainly derived from human activities, man-made products and burning fossil fuels (Perera 2018). To address these problems, green and renewable energy sources are very important for future development. In this respect, hydrogen is a clean green energy source with many advantages such as availability and high combustion heat value. Renewable sources of hydrogen production are mainly water splitting (electrolysis, thermolysis, and photolysis) and biomass (biological and thermochemical) processes, and one of critical factors is the economical and global scaling up of the hydrogen production (Martino et al. 2021; Agyekumet al. 2022). A hydrogen fuel cell consists of two electrodes namely a positive electrode (cathode) and a negative electrode (anode) separated by a polymer electrolyte membrane (Sarfranz et al. 2020). The cathode electrode also known as the gas diffusion layer (GDL) is a part of the substrate that is coated with electrocatalyst to improve the efficiency of the hydrogen evolution reaction (HER) (Sun et al. 2018). Thus, it regenerates highly purified hydrogen

by means of electrochemical water splitting process (Wei et al. 2020). Platinum (Pt) is a noble metal which is commonly used as an active electrocatalyst in hydrogen generation because it processes a very high exchange current density (Devadas et al. 2019). However, the high cost of this catalyst is a drawback in applications at large scale (Jiang et al. 2019).

Thus, it is critical for materials to satisfy the need for cost-effectivity and earth-abundance. For achieving these conditions, there are two ways, one is to find alternative catalysts to platinum (Devadas et al. 2019; Oh et al. 2021), and another is to reduce the amount of platinum. Some researchers have focused on the state-of-the-art investigations regarding catalysts with reduced platinum content as an increase promising strategy of HER performance (Devadas and Imae 2016; Monteiro et al. 2021), including Pt/ α -molybdenum carbide (Lin et al. 2017), Pt/FeOx (Qiao et al. 2011), PtSn₄ (Boukhalov et al. 2020), Pt/NiFe@ultrathin graphene layer (Davodi et al. 2021) Pt@ porous carbon matrix, (Zhang et al. 2018a, b), and Pt/nitrogen-doped carbon nanotube (NCNT) (Ma et al. 2017). Moreover, works on encapsulating

Pt in metal–organic frameworks (MOFs) have been published (Wang et al. 2012). MOFs attract much attention as new potential templates or supports for electrocatalysts, because they are porous crystalline materials that consist of a rigid three-dimensional structure with large specific surface areas and controllable pore sizes (Meng et al. 2020). Zeolitic imidazolate frameworks (ZIFs) are one type of MOFs with imidazolate linkers bridging metal centers that permit the adsorption and desorption of organic molecules and the encapsulation of metals (Wang et al. 2013).

For fuel cells, substrates for catalyst should have excellent electrical conductivity, good mechanical properties, suitable reactant permeability, high thermal stability, ease of processing, and low cost. Typical substrates are carbon cloth, carbon paper, and metallic foams (Litster and McLean 2004). However, they have disadvantages such as high cost (Taherian et al. 2018) and inefficient complexation with catalyst, resulting in the reduction of active sites and ion transfer (Liu et al. 2021; Komini Babu et al. 2016). The lamellar accumulation with multiple layer phases enhancing strategies on the electrocatalytic HER performance is one method for improving the limitation of effective loss on the catalytic activity (Lin et al. 2019, 2020).

Cellulose nanofibers (CNF) are alternative materials obtained from bioresources that have been used in numerous fields such as medicine, tissue engineering, and electronics devices because they exhibit excellent physical and biological properties including various mechanical properties, highly thermal and chemical stability, and superior water adsorption (Krathumkhet et al. 2021a, b; Do et al. 2021; Rahmawati et al. 2020). These properties of CNF make this material adequate as potential catalyst substrate with characteristic of fiber network (Shah and Imae 2016; Gupta and Gupta 2015). However, since CNF has no electrical conductivity, conductive materials should be added to improve electron transfer property (Chen et al. 2020). Among conductive materials, semiconducting metals, conducting polymers, and carbon-based materials have been utilized in various applications to enhance electrocatalytic activity, specific surface area, and electron transfer kinetics (Chang and Imae 2018; Krathumkhet et al. 2021a, b).

In this work, the preparation of a Pt electrocatalyst encapsulated in ZIF-8 (Pt@ZIF-8) by three methods is reported, and Pt@ZIF-8 is incorporated into

a CNF composite substrate with antimony tin-doped oxide (ATO) or polypyrrole (Ppy) with the lamellar structure by the layer-by-layer deposition. The performance of these materials as catalysts for HER is evaluated. The high HER efficiency and relatively low Pt content of the present system are promising for the improvement of hydrogen fuel cell devices. Thus, the present work proposes the preparation procedure of costless but efficient catalysts which would allow the mass production of hydrogen gas.

Experimental section

Materials

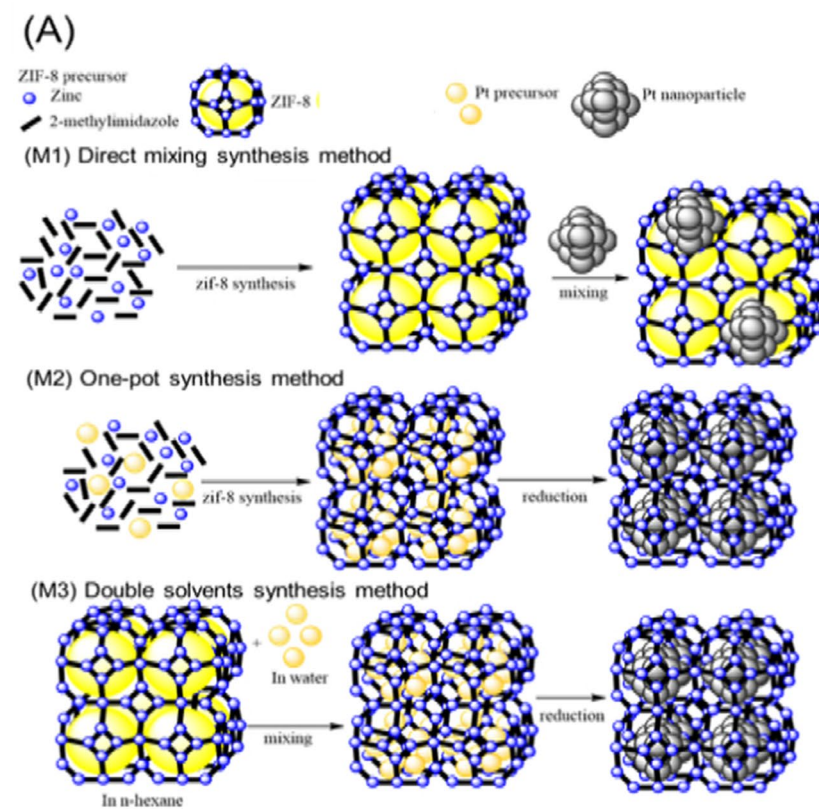
Zinc nitrate hexahydrate ($\text{Zn}(\text{NO}_3)_2 \cdot 6\text{H}_2\text{O}$, 98%), potassium tetrachloroplatinate (K_2PtCl_4), anhydrous hexane (C_6H_{14} , 99%), 2-methyl imidazole ($\text{C}_4\text{H}_6\text{N}_2$, 99%), and sulfanilic acid were purchased from Acros Organics, USA. An aqueous sodium hypochlorite (NaOCl) solution (12% available chlorine) was purchased from Shimakyu Pure Chemicals, Japan. Antimony tin doped oxide (ATO) was obtained from Sigma-Aldrich, USA. Sodium borohydride (NaBH_4) was bought from Wako Pure Chemical Industries, Japan. Other reagents were commercial grade. Ultrapure water (Yamato, Japan) with a resistivity of 18.2 $\text{M}\Omega \text{ cm}$ was used throughout the experiments.

Synthesis of Pt@ZIF-8

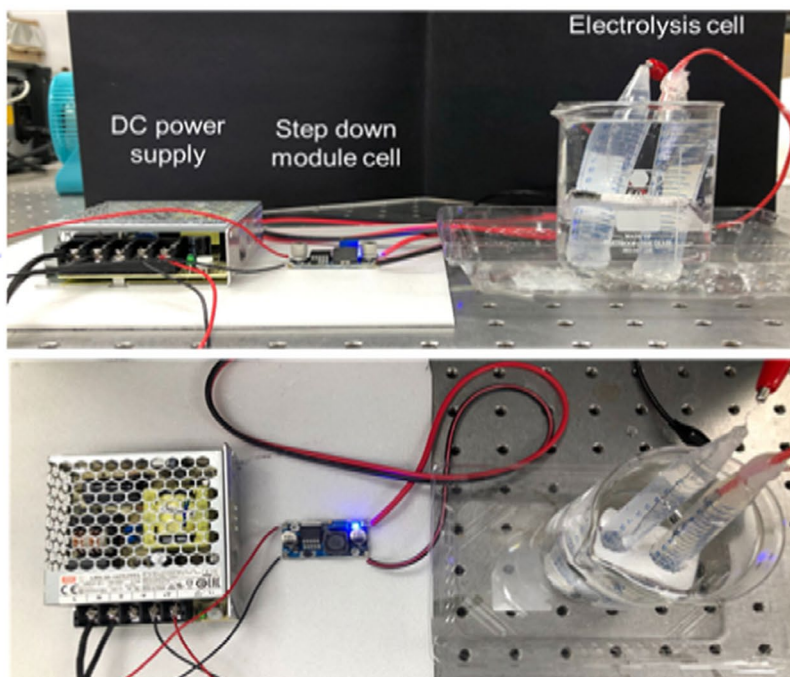
A milky white dispersion of ZIF-8 was obtained by mixing 2-methylimidazole (5.67 g) in water (20 ml) and zinc nitrate hexahydrate (0.29 g) in water (2 ml) and stirring for 5 min. The product was washed with water and ethanol by centrifuging at 25,000 rpm and dried 24 h at 40 °C. Synthesis of Pt@ZIF-8 was carried out by three different methods as illustrated in Fig. 1A.

In the direct mixing synthesis method of Pt@ZIF-8 (M1), potassium tetrachloroplatinate (K_2PtCl_4) (0.029 g) in water (1 ml) and sodium borohydride (28 mg) in water (1.25 ml) were mixed, stirred 3 h, and added to a dispersion of ZIF-8 in water (20 ml). After one day, the collected black precipitate was washed three times with water by centrifugation (10,500 rpm) and dried 24 h at 50 °C. The weight

Fig. 1 **A** Synthesis of Pt@ZIF-8 by three different methods. **B** Electro-station and electrolysis apparatus



(B)



ratio of Zinc nitrate hexahydrate: potassium tetrachloroplatinate (Zn: Pt) was 1: 0.1.

In the one-pot synthesis method of Pt@ZIF-8 (M2), 2-methylimidazole (5.67 g) and zinc nitrate hexahydrate (0.29 g) (ZIF-8 precursors) and K_2PtCl_4 (0.029, 0.058, and 0.116 g) at Zn: Pt weight ratio of 1: 0.1, 1: 0.2, and 1: 0.4 were mixed in water and stirred 5 min. The product was washed three times with water by centrifugation (10,500 rpm) and dried 24 h at 50 °C. The yellow precipitate ($PtCl_4^-$ @ZIF-8) was dispersed in water (40 ml) and mixed with sodium borohydride (28 mg) in water (1.25 ml). The mixture was stirred 3 h, and the obtained black precipitate was washed and dried 24 h at 40 °C.

In the double solvent synthesis method of Pt@ZIF-8 (M3), ZIF-8 was mixed with n-hexane (30 ml), sonicated 1 h to obtain a homogeneous dispersion, and added K_2PtCl_4 (0.029, 0.058 and 0.116 g) in water (0.3 ml), keeping Zn: Pt weight ratio of 1: 0.1, 1: 0.2, and 1: 0.4. After 24 h, the precipitate was collected by centrifugation at 25,000 rpm and dried 24 h at 40 °C. The yellow precipitate was further dispersed in water (40 ml) and sodium borohydride (28 mg) in water (1.25 ml) was added. The mixture was stirred 3 h, and the obtained black precipitate was washed and dried 24 h at 40 °C.

Preparation of electrode films

Ppy was prepared following a previously reported procedure (Chang and Imae 2018). The sulfonated-Ppy (S-Ppy) was synthesized by dispersing Ppy (50 mg) into a mixed aqueous solution of KNO_3 (2 ml, 6 mM) and HCl (2 ml, 0.1 M) under stirring at 5 °C for 15 min and adding sulfanilic acid (8 ml, 0.06 M) under stirring at 80 °C for 24 h. The product was collected by centrifugation and washed thoroughly with water (Chien et al. 2013).

GDL substrates were prepared from a TEMPO-oxidized cellulose nanofiber (TOCNF, 20 ml, 0.4 wt%) dispersion (Rahmawati et al. 2020) by mixing with ATO or S-Ppy (120 mg) at room temperature (~25 °C) for 2 h. The dispersion was spread into a petri dish (diameter = 7.5 cm) and dried at 40 °C. Pt@ZIF-8 in water (15 mg/ml, 4 ml) was sonicated for 2 min, coated on the dried substrates in the petri dish and then dried at 40 °C for 24 h.

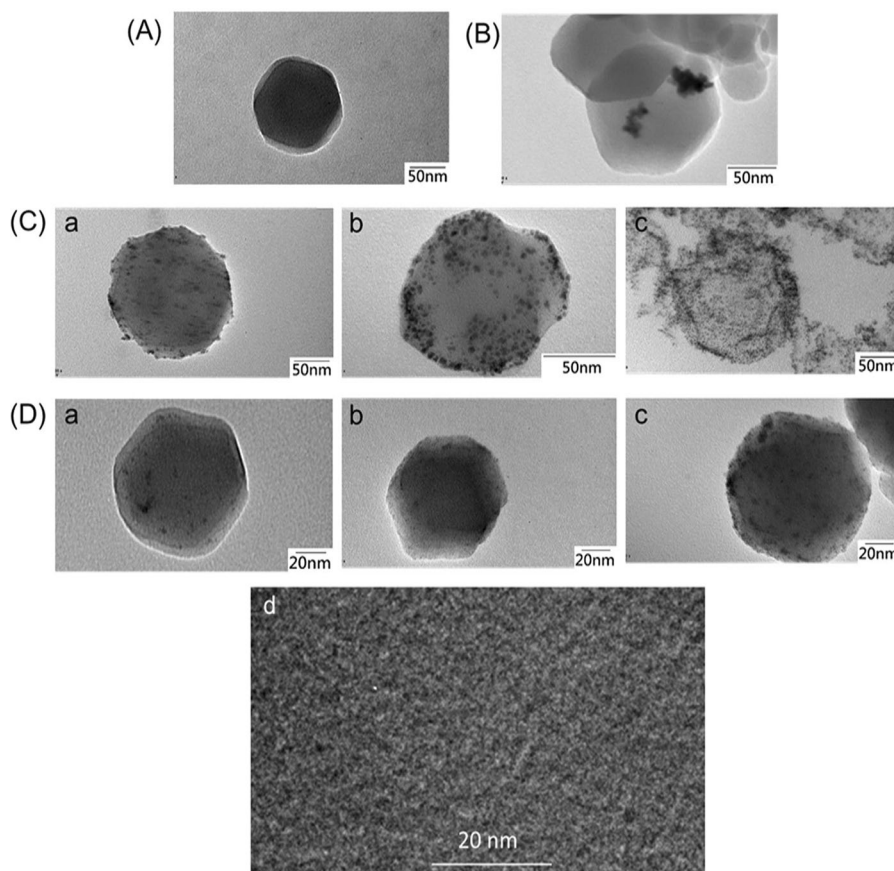
Measurements

The X-ray diffraction (XRD) was recorded at 5–60° and a 4 min⁻¹ step on an SC-XR Bruker AXS, D8, USA, with $CuK\alpha$ at 40 kV and 4 mA. N_2 adsorption–desorption isotherms were measured on an Autosorb instrument (Quantachrome, Japan) and analyzed using the Brunauer–Emmett–Teller (BET) equation. All samples were degassed at 30 °C for 12 h before the measurement. The thermal properties were investigated using a thermo gravimetric analyzer (TGA, Q500 TA appliance, USA) for 4–10 mg samples under air flow in a temperature range of 25–800 °C at a 10 °C min⁻¹ heating rate. Scanning electron microscopic images were collected on Hitachi TM-1000 at 15 kV and JEOL JSM-6390, Japan, at 50 kV. The samples were attached to stubs by a carbon tape. A transmission electron microscope (TEM, JEOL, Japan) and the high-resolution TEM (HRTEM, Philips Tecnai F30) were operated at 120 and 300 kV, respectively. A drop of sample dispersion (5 μ l) was deposited on a copper TEM grid and dried before observation. The infrared absorption spectra were obtained on a FTIR spectrometer (Thermo Nicolet, Nexus 6700, Japan) with 500 scans; samples were embedded in KBr pellets. Electrochemical impedance spectra (EIS) (Zennium—ZAHNER®, Germany) were obtained at 2 MHz–20 Hz. The content of platinum in ZIF-8 was measured by inductively coupled plasma-atomic emission spectroscopy (ICP-AES, Jobin Yvon HORIBA, JY 2000-2, Japan) using standard solutions of platinum precursor at concentrations of 0, 1, 2, 4, 6, 8 and 10 ppm in 2% HNO_3 . Then the analyte (Pt@ZIF-8, 100 μ g) was treated overnight with an aqua regia (HNO_3 :HCl = 1:3 volume ratio) solution (900 μ l) to ionize, and the solution was diluted 10 times with a 2% HNO_3 solution to be 10 ppm of Pt@ZIF-8 (10 ml).

Electrochemical measurements

On a glassy carbon electrode (surface area: 0.079 cm²) polished beforehand with fluff, a dispersion of Pt@ZIF-8 (1 mg/ml, 5 μ l) in ethanol was dropped and dried. Then Nafion in ethanol (0.5 wt%, 2 μ l) was deposited and subsequently dried. Electrochemical measurements of film electrodes were performed in 0.5 M H_2SO_4 (at acid condition) with an HZ-3000 instrument, Japan, with a linear sweeping

Fig. 2 TEM images of **A** ZIF-8, **B** M1-Pt@ZIF-8 at Zn:Pt weight ratio of 1:0.1, **C** M2-Pt@ZIF-8 at Zn:Pt weight ratio of (a) 1:0.1, (b) 1:0.2 and (c) 1:0.4, and **D** M3-Pt@ZIF-8 at Zn:Pt weight ratio of (a) 1:0.1, (b) 1:0.2 and (c) 1:0.4. (d) and HRTEM image of M3-Pt@ZIF-8 at 1:0.4



voltammetry (LSV) from 0 to -0.8 V and a 5 mV/s scan rate. The H_2 production was measured with electro-station at applied voltage 2.3 V and electrolysis apparatus as shown in Fig. 1B.

Results and discussion

Characterizations of Pt@ZIF-8 materials obtained from three different methods

Pt@ZIF-8 was prepared through three different synthesis routes as illustrated in Fig. 1A. In the TEM image of Fig. 2A, ZIF-8 appears as particle with a hexagonal shape and a size of 70–100 nm in agreement with previous reports (Wu et al. 2014; Xu et al. 2018). As seen in the TEM image of M1-Pt@ZIF-8 at Zn:Pt weight ratio of 1:0.1 in Fig. 2B, platinum nanoparticles aggregated on the surface of ZIF-8, suggesting that nanoparticles did not penetrate into ZIF-8 pores because platinum nanoparticles are adsorbed

on ZIF-8 easier than encapsulated inside of ZIF-8 due to too large size of platinum nanoparticles for passing through the pore channel in ZIF-8. In contrast, Fig. 2C shows that in M2-Pt@ZIF-8, platinum nanoparticles were embedded into ZIF-8, although a small number of platinum nanoparticles were detected on the surface of ZIF-8 at low platinum ratio (Zn:Pt weight ratio = 1:0.1) (Fig. 2(C)a). However, when the platinum ratio was increased (Zn:Pt weight ratio = 1:0.4), the internal structure of ZIF-8 was inadequately formed, as seen in Fig. 2(C)c, because of too much amount of platinum precursors.

In M3-Pt@ZIF-8, platinum nanoparticles were embedded into ZIF-8 without structural disruption even at Zn:Pt weight ratio of 1:0.4 as shown in Fig. 2(D)a–c. When ZIF-8 uniformly dispersed in nonpolar solvent was mixed with the platinum precursor dispersed in a small amount of polar solvent, the hydrophilic platinum precursor could approach the hydrophilic ZIF-8 pore and be transported into ZIF-8 by the capillary force (Aijaz et al. 2012). Thus, the

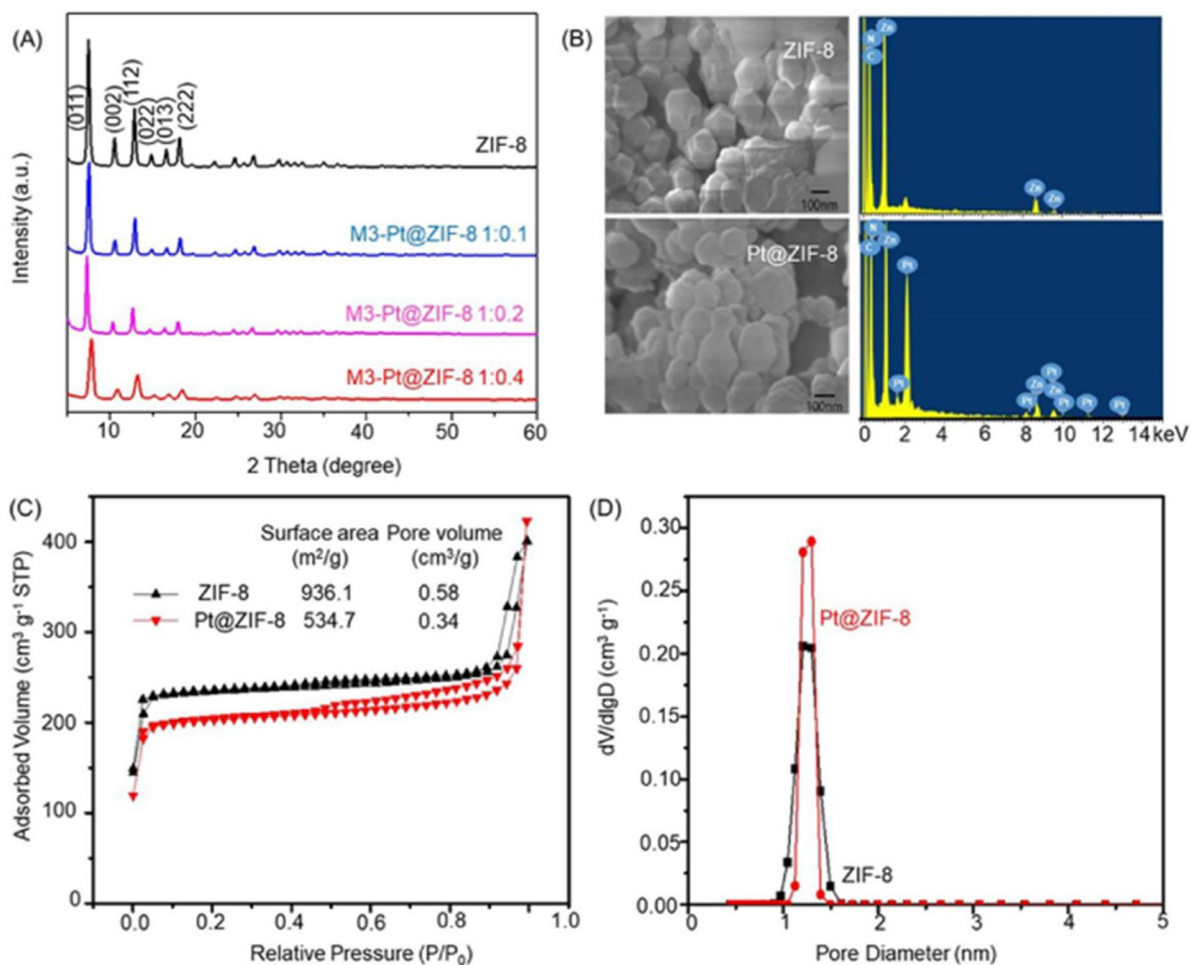


Fig. 3 **A** XRD patterns of ZIF-8 and M3-Pt@ZIF-8 (1:0.1, 1:0.2 and 1:0.4), **B** SEM (left side) and EDX (right side), **C** nitrogen-adsorption/desorption isotherms and **D** pore-size distribution of ZIF-8 and M3-Pt@ZIF-8(1:0.4)

pristine morphology of ZIF-8 was maintained, even when platinum nanoparticles were embedded into the ZIF-8 structure. Figure 2(D)d is an HRTEM image of ZIF-8, where many small black dots with size less than 1 nm to be platinum particles are observed. Thus, M3-Pt@ZIF-8 was selected as the best sample for the following experiments.

The XRD pattern of ZIF-8 (Fig. 3 A) features Bragg peaks at $2\theta = 7.4^\circ$, 10.3° , 12.6° , 14.5° , 16.4° , and 17.9° , corresponding to (011), (002), (112), (022), (013) and (222) planes, respectively, in

agreement with the literature (Nordin et al. 2017; Zhang et al. 2018a, b). The XRD of M3-Pt@ZIF-8 showed no significant variations relative to that of the ZIF-8, i.e. the crystalline structure is maintained even after platinum doping. The main Bragg peak ((111) plane) of platinum at $2\theta = 39^\circ$ (Kumar et al. 2017) was not identified in the XRD pattern of M3-Pt@ZIF-8, probably due to the low Pt content.

The SEM image of ZIF-8 powder in Fig. 3B shows nanocrystals of approximately 50–100 nm size with sharp hexagonal facets, similar to that

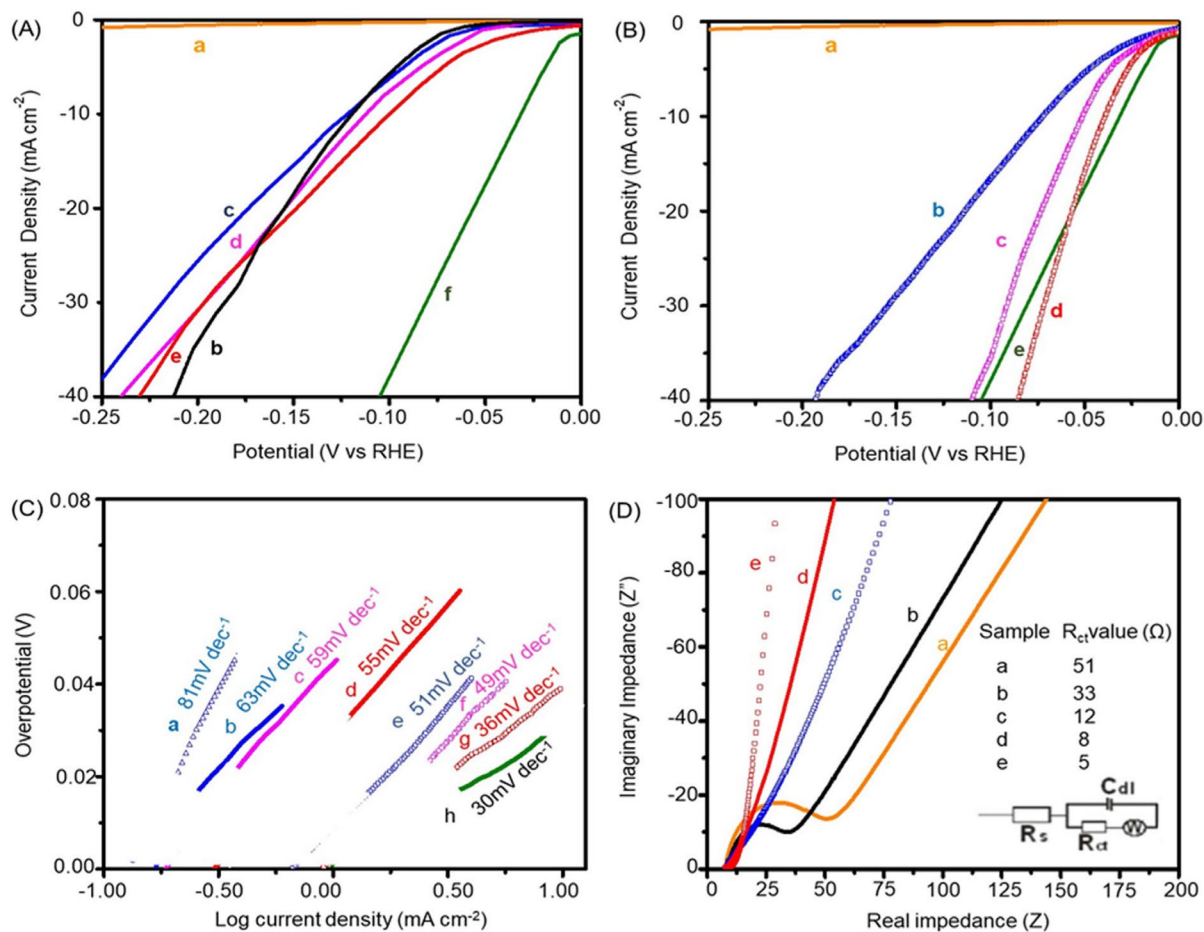


Fig. 4 **A** HER polarization curves of (a) bare electrode, (b) M1-Pt@ZIF-8(1:0.1), (c) M2-Pt@ZIF-8(1:0.1), (d) M2-Pt@ZIF-8(1:0.2), (e) M2-Pt@ZIF-8(1:0.4), and (f) Pt(40 wt%)/C, **B** (a) bare electrode, (b) M3-Pt@ZIF-8(1:0.1), (c) M3-Pt@ZIF-8(1:0.2), (d) M3-Pt@ZIF-8(1:0.4), and (e) Pt(40 wt%)/C, **C** Tafel plots for (a) M1-Pt@ZIF-8(1:0.1), (b) M2-Pt@ZIF-

8(1:0.1), (c) M2-Pt@ZIF-8(1:0.2), (d) M2-Pt@ZIF-8(1:0.4), (e) M3-Pt@ZIF-8(1:0.1), (f) M3-Pt@ZIF-8(1:0.4), and (g) M3-Pt@ZIF-8(1:0.1), (d) M3-Pt@ZIF-8(1:0.2), (e) M3-Pt@ZIF-8(1:0.4). Inset is the equivalent Randles circuit used for theoretical analysis

obtained from TEM. The size of M3-Pt@ZIF-8 particles was not significantly different from pristine ZIF-8. The elemental analysis (EDX spectrum) of M3-Pt@ZIF-8 confirmed that Pt is contained in ZIF-8. The Pt content in M3-Pt@ZIF-8 (Zn:Pt=1:0.4) was 2.82 wt% according to ICP-AES analysis.

N_2 gas adsorption/desorption isotherms at 77 K are shown in Fig. 3C. The specific surface area and pore volume of Pt@ZIF-8 were lower than those of pristine ZIF-8 due to the filling of Pt in ZIF-8 pores. The pore size distribution in Pt@ZIF-8, as seen in Fig. 3D was unimodal with a range

1.0–1.5 nm, similarly to the pore size distribution of ZIF-8 (0.9–1.6 nm). This pore size allows the incorporation of platinum nanoparticles.

HER activity of Pt@ZIF-8 catalyst electrodes

Figure 4A, B shows HER polarization curves of three different Pt@ZIF-8 catalyst electrodes. The initial potential gradually decreased, indicating that the electrocatalytic effect is gradually enhanced. The overpotential at -50 mV increased significantly with increasing Pt content in the order of 0, 2.56 and 16 mA cm^{-2} , respectively, for M1-, M2- and M3-Pt@

Table 1 Comparison of Pt contents and HER results between present and reported electrocatalysts

Electrocatalyst*	Pt content (wt%)	Onset potential (mV)	Current density	Tafel slope (mV/decade)	Reference
Pt(40 wt%)/C	40	0	17 mA/cm ² at 50 mV	32	This work
M1-Pt@ZIF-8(1:0.1)	–	–73	0.49 mA/cm ² at 50 mV	81	This work
M2-Pt@ZIF-8(1:0.4)	–	–31	2.56 mA/cm ² at 50 mV	55	This work
M3-Pt@ZIF-8(1:0.4)	2.82	–5	16 mA/cm ² at 50 mV	36	This work
GO/DenPtNPs	1.12	–26	0.4 mA/cm ² at 50 mV	58	Devadas and Imae (2016)
CNH/DenPtNPs	0.86	–16	2.5 mA/cm ² at 50 mV	53	Devadas and Imae (2016)
CNT/DenPtNPs	1.03	–16	2.5 mA/cm ² at 50 mV	42	Devadas and Imae (2016)
Pt@PCM	0.095	–281	6 mA/cm ² at 200 mV	132	Zhang et al. (2018a, b)
Pt/NCNT	0.74	–	10 mA cm ^{–2} at 40 mV	33	Ma et al. (2017)
Pt/MoS ₂ /carbon fiber	2.03	–	0.09 mA/cm ² at 200 mV	53.6	Hou et al. (2015)
PtP ₂ @PNC	3.50	–	10 mA/cm ² at 183 mV	30	Pu et al. (2020)
Pt@MOF-808-EDTA	9.58	–42.1	10 mA/cm ² at 50 mV	24.4	Li et al. (2019)
PtCu-MoO ₂ @C	11.3	–42	10 mA/cm ² at 24 mV	36	Zhang et al. (2020)

*PCM, porous carbon matrix; EDTA, ethylenediaminetetraacetic acid; NCNT, nitrogen-doped carbon nanotube; CNT, carbon nanotube; CNH, carbon nanohorn; GO, graphene oxide; DenPtNP, platinum nanoparticle-encapsulated dendrimer; MoS₂, molybdenum disulphide; CF, carbon fiber; PtP₂, platinum phosphide; PNC, phosphorus and nitrogen dual-doped carbon; MoO₂@C, porous octahedral carbon matrix

ZIF-8, where the value of M3-Pt@ZIF-8 was quite close to 17 mA cm^{–2} of the standard electrode (Pt(40 wt%)/C). The LSV polarization curves were converted to Tafel slope to evaluate the catalytic performance of electrode based on three mechanisms of hydrogen evolution reaction of (I) Volmer reaction (120 mV/dec), (II) Heyrovsky reaction (40 mV/dec) and (III) Tafel reaction (30 mV/dec) (Devadas and Imae 2016). The Tafel slope value of 36 mV/dec for M3-Pt@ZIF-8 indicates that the reaction would theoretically take place via the Volmer-Heyrovsky mechanism and the Volmer-Tafel mechanism, while the Tafel slope of 30 mV/dec for Pt(40 wt%)/C confirms the Volmer-Tafel mechanism (Kumar et al. 2017, 2020; Li et al. 2011) (see Fig. 4C). Then the hydrogen production by a Volmer-Tafel mechanism is preferable over a Volmer-Heyrovsky mechanism, because less amount of electron concerns in the reaction.

The impedance characteristics of M3-Pt@ZIF-8 catalyst electrodes are compared to bare and ZIF-8 electrodes in Fig. 4D. The bare and ZIF-8 electrodes showed high electron transfer resistance (R_{ct}) values (51 and 33 Ω , respectively), indicating the low electron transfer rate. With increasing Pt content against ZIF-8, R_{ct} value decreased to 12, 8, and 5 Ω . That is, the electrode with M3-Pt@ZIF-8(1:0.4) provided the lowest R_{ct} value, demonstrating that M3-Pt@

ZIF-8(1:0.4) provides the fastest electron transfer on the HER reaction.

Table 1 shows the comparison of Pt-based electrocatalysts for HER. Particles in the list have far smaller platinum contents than the standard sample (Pt(40 wt%)/C). The Pt content is smaller than 3 wt% (Devadas and Imae 2016; Hou et al. 2015) except for PtP₂@PNC (3.5 wt%), Pt@MOF-808-EDTA (9.58 wt%) and PtCu-MoO₂@C (11.3 wt%) with current density of 10 mA/cm (Pu et al. 2020; Zhang et al. 2020; Martino et al. 2021). However, the onset potential of M3-Pt@ZIF-8 was close to that of Pt(40 wt%)/C and lower than those of other Pt-based electrodes (Devadas and Imae 2016; Li et al. 2019). Tafel slope (36 mV/decade) of M3-Pt@ZIF-8 electrocatalysts was also similar to that of Pt(40 wt%)/C and Pt@MOF-808-EDTA but lower than other electrodes. Although Pt/NCNT has a smaller Pt content (0.17 wt%) and Tafel slope (33 mV/decade), as well as PtCu-MoO₂@C with Tafel slope of 30 mV/decade, than M3-Pt@ZIF-8, it had a lower current density (10 mA/cm²) than M3-Pt@ZIF-8 and Pt(40 wt%)/C. Thus, M3-Pt@ZIF-8 is excellent from the viewpoint of the electrocatalytic activity towards HER alongside of the standard Pt(40 wt%)/C, but it is far better than Pt(40 wt%)/C in terms of the cost performance.

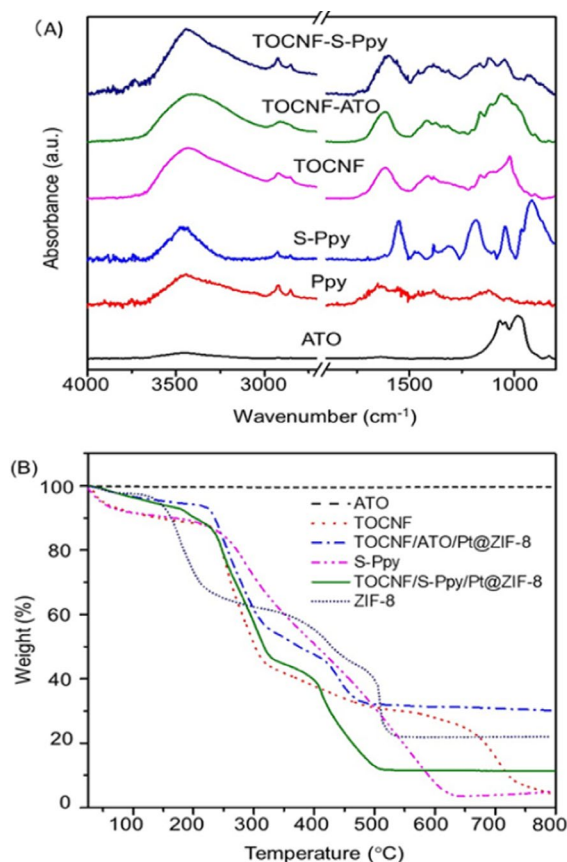


Fig. 5 **A** FTIR absorption spectra of ATO, Ppy, S-Ppy, TOCNF, TOCNF/ATO, and TOCNF/S-Ppy and **B** TGA of ATO, TOCNF, TOCNF/ATO/Pt@ZIF-8, S-Ppy, TOCNF/S-Ppy/Pt@ZIF-8, and ZIF-8

Characterizations of TOCNF/ATO and TOCNF/S-Ppy substrates

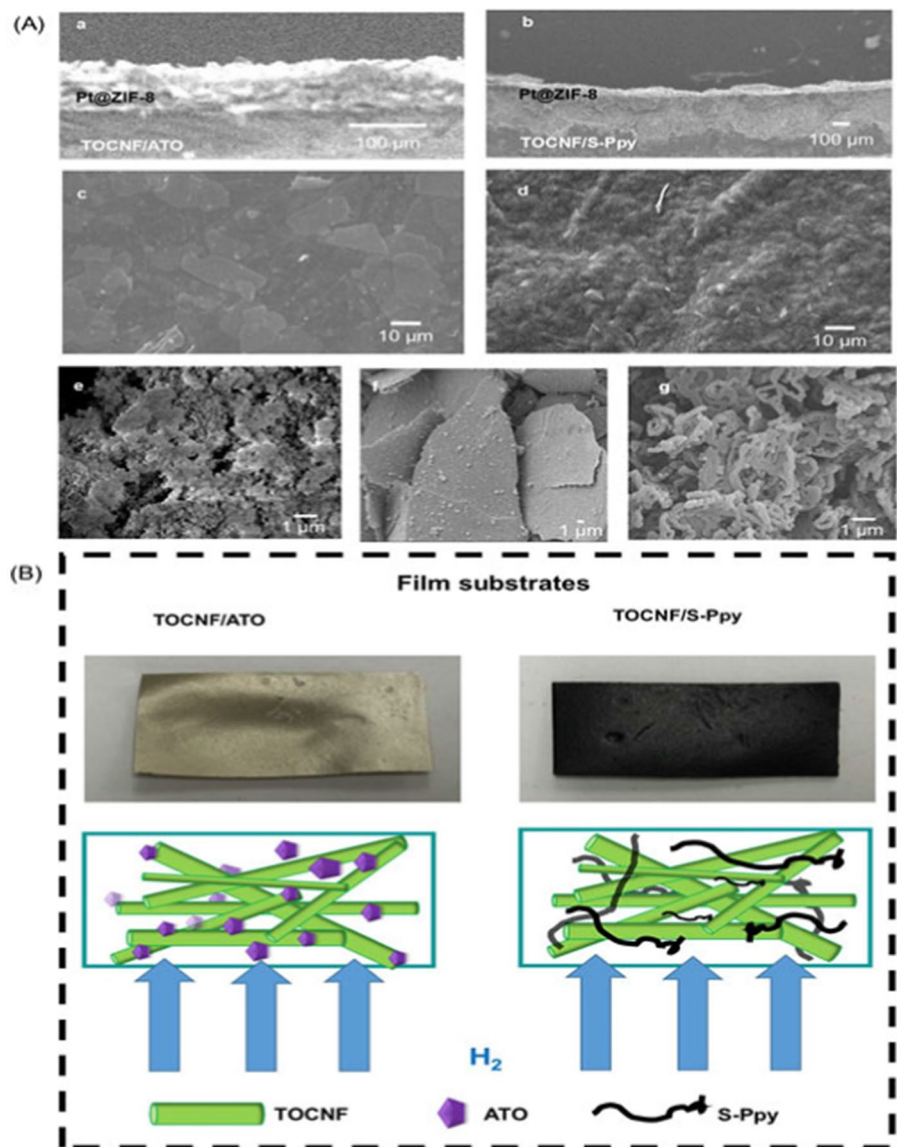
The FTIR spectrum of TOCNF (Fig. 5A) shows a characteristic broad band of an O–H stretching vibration mode at $3600\text{--}3100\text{ cm}^{-1}$. Bands at 1610 and 1420 cm^{-1} are assigned to antisymmetric and symmetric stretching vibration modes of COO^- groups, respectively, although they are overlapped on O–H and C–H bending modes, respectively. A band at 1154 cm^{-1} points to C–O–H out-of-plane bending, while a C–O–C stretching mode is associated to a strong band at 1029 cm^{-1} (Kebede et al. 2017). An FTIR spectrum of TOCNF/ATO shows additional characteristic bands at 1068 and 980 cm^{-1} due to the O–Sb–O and O–Sn–O vibration modes, respectively. An IR band of TOCNF/S-Ppy observed at 3440 cm^{-1}

is assigned to an N–H stretching vibration mode of Ppy, whereas stretching bands of O–S–O and S=O groups are at 1047 and 948 cm^{-1} , respectively.

Figure 5B shows the thermal decomposition profiles of materials. TOCNF was decomposed through three weight loss steps except the removal of water and residual solvent below $150\text{ }^{\circ}\text{C}$. A first weight loss between 230 and $350\text{ }^{\circ}\text{C}$ was attributed to cellulose depolymerization. The second thermal degradation was assigned to polymer backbone degradation, which occurred at $\sim 500\text{ }^{\circ}\text{C}$ (Shah and Imae 2017). The third degradation step at $650\text{--}720\text{ }^{\circ}\text{C}$ indicates decomposition of the oxidized fiber attributed to carbonization through a self-sustained exothermic process (Kebede et al. 2017). ZIF-8 exhibited the first weight loss in temperature range of $25\text{--}200\text{ }^{\circ}\text{C}$, corresponding to the removal of solvent molecules from the cavities (Lo et al. 2016; Pan et al. 2011). Then, a second thermal degradation up to $500\text{ }^{\circ}\text{C}$ corresponds to the degradation of organic ligands namely 2-methylimidazole of ZIF-8 (Li et al. 2020). In addition, ATO showed no weight loss, but S-Ppy was almost decomposed up to $630\text{ }^{\circ}\text{C}$ (residue = $\sim 4.8\text{ wt}\%$). The thermal degradation of TOCNF/ATO/Pt@ZIF-8 and TOCNF/S-Ppy/Pt@ZIF-8 follows the degradation of their components (TOCNF, or S-Ppy and ZIF-8), although the third degradation of TOCNF at $650\text{--}720\text{ }^{\circ}\text{C}$ was not observed. The high residue ($30.2\text{ wt}\%$) of TOCNF/ATO/Pt@ZIF-8 above $500\text{ }^{\circ}\text{C}$ is attributed to ATO, inorganic moiety of ZIF-8, and Pt. The residue ($11.4\text{ wt}\%$) of TOCNF/S-Ppy/Pt@ZIF-8 probably consists of inorganic moieties of ZIF-8 and Pt.

The cross-sectional and surface morphologies of electrode films were observed by SEM. The electrode films prepared by coating Pt@ZIF-8 on TOCNF/ATO or TOCNF/S-Ppy film have a layered morphology as shown in Fig. 6A(a, b), where an upper layer is Pt@ZIF-8 and a bottom layer is TOCNF/ATO or TOCNF/S-Ppy. It was elucidated from Fig. 6A(c–g) that Pt@ZIF-8 consists of aggregates of ZIF-8 nanoparticles, ATO is large particles with flat faces, S-Ppy is a network of flexible chains. SEM images of TOCNF/ATO and TOCNF/S-Ppy were characterized by large particles of ATO and chain-like texture of S-Ppy, respectively, reflecting the presence of component materials. Especially, S-Ppy shows a chain-like texture combined with fibrous TOCNF that provided the flexibility of an electrode film more than TOCNF/ATO

Fig. 6 **A** Cross-sectional SEM images of film substrates of (a) TOCNF/ATO/Pt@ZIF-8 and (b) TOCNF/S-Ppy/Pt@ZIF-8, and surface SEM images of (c) TOCNF/ATO, (d) TOCNF/S-Ppy (e) Pt@ZIF-8, (f) ATO, and (g) S-Ppy. **B** Photos and structural schemes of TOCNF/ATO and TOCNF/S-Ppy film substrate for H₂ gas diffusion



and, moreover, net-like texture of TOCNF/S-Ppy may promote the permeation of H₂ more than TOCNF/ATO as shown in Fig. 6B.

HER activity of electrode films

EIS of electrode films was analyzed to examine the electron transfer resistance (see Fig. 7A). The electron transfer resistance (R_{ct}) of electrodes was calculated based on a Randles circuit model. The TOCNF/ATO and TOCNF/S-Ppy substrates without catalyst-loading exhibited large R_{ct} values of 2.4 and 1.8 Ω , respectively, indicating the rather poor charge

transport. After Pt@ZIF-8 catalyst was loaded, both TOCNF/ATO and TOCNF/S-Ppy substrates showed smaller R_{ct} values (1.5 Ω and 0.9 Ω , respectively), verifying the increase of charge transport. The relaxation time constant (τ parameter) on the relaxation process of the electrical double layer was determined from a phase angle maximum of the Bode plot (Fig. 7B) using an equation $\tau = 1/2\pi f$, where f is the relaxation frequency (Kumar et al. 2020). The relaxation time constants for TOCNF/S-Ppy/Pt@ZIF-8, TOCNF/ATO/Pt@ZIF-8, TOCNF/S-Ppy, and TOCNF/ATO were 1.8, 1.5, 1.0, and 0.6 ms, respectively. The higher relaxation time of TOCNF/S-Ppy/

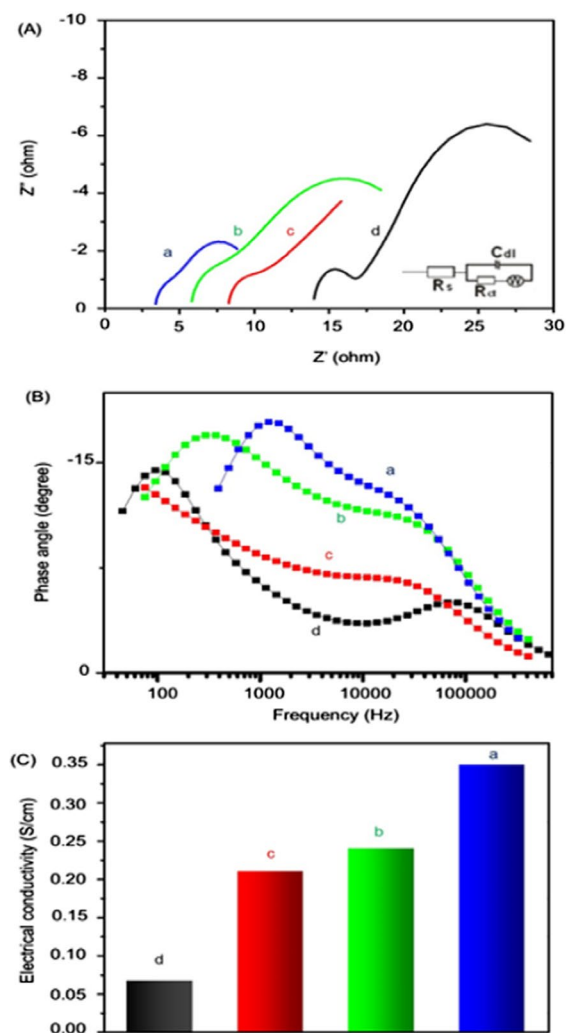


Fig. 7 **A** EIS spectra (inset: a Randles circuit model), **B** Bode plot and **C** electrical conductivity of (a) TOCNF/S-Ppy/Pt@ZIF-8, (b) TOCNF/ATO/Pt@ZIF-8, (c) TOCNF/S-Ppy, and (d) TOCNF/ATO

Pt@ZIF-8 suggests its more efficient electrochemical reaction. EIS results were also used to calculate electrical conductivity σ (S/cm) by $\sigma = l/R \times A$ (Tangkitthanachoke et al. 2017), where R is the resistance (Ω), l is the thickness (cm), and A is the area (cm^2). Here, $l = \sim 0.16$ cm and $A = 1$ cm^2 . As shown in Fig. 7C, the electrical conductivity increased in the order of TOCNF/ATO < TOCNF/S-Ppy < TOCNF/ATO/Pt@ZIF-8 < TOCNF/S-Ppy/Pt@ZIF-8. Thus, TOCNF/S-Ppy/Pt@ZIF-8 performs efficiently the electrochemical reaction due to the high electrical conductivity.

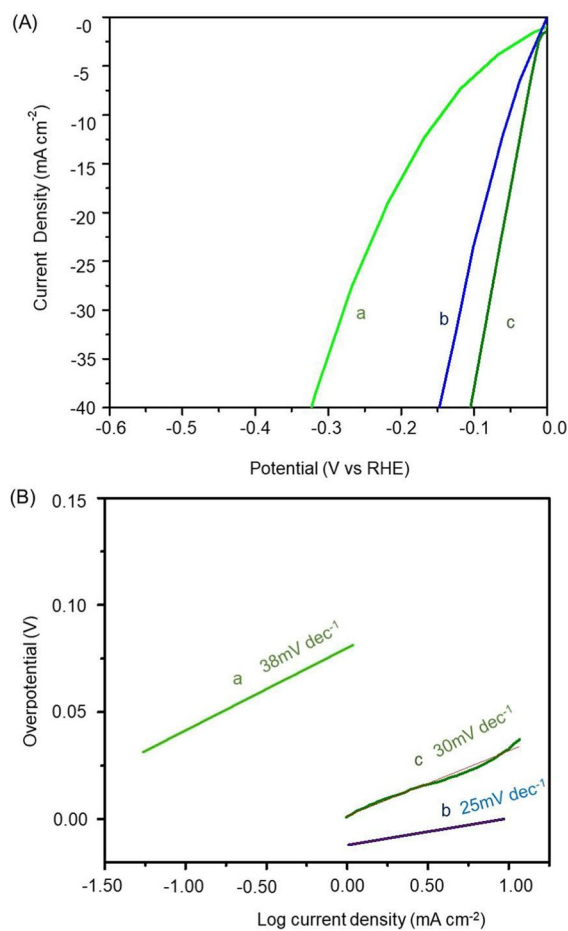


Fig. 8 **A** HER polarization curves and **B** Tafel plots of (a) TOCNF/ATO/Pt@ZIF-8, (b) TOCNF/S-Ppy/Pt@ZIF-8 and (c) Pt(40 wt%)/C

Figure 8A, B shows HER polarization and Tafel slope curves for two electrodes. The overpotentials of electrodes at a current density of 40 mA cm^{-2} were -321 and -147 mV and Tafel slope values were 38 and 25 mV dec^{-1} for active Pt@ZIF-8 on TOCNF/ATO and TOCNF/S-Ppy, respectively. The overpotential value of TOCNF/S-Ppy/Pt@ZIF-8 was only slightly higher than those of Pt(40 wt%)/C and Pt@ZIF-8 (Fig. 4B). Thus, TOCNF/S-Ppy is a more promising electrode in HER activity than TOCNF/ATO. The great HER activity of TOCNF/S-Ppy/Pt@ZIF-8 rises from its high electrical conductivity (Fig. 7C) which may be promoted by the network structure of flexible S-Ppy chains, free voids in

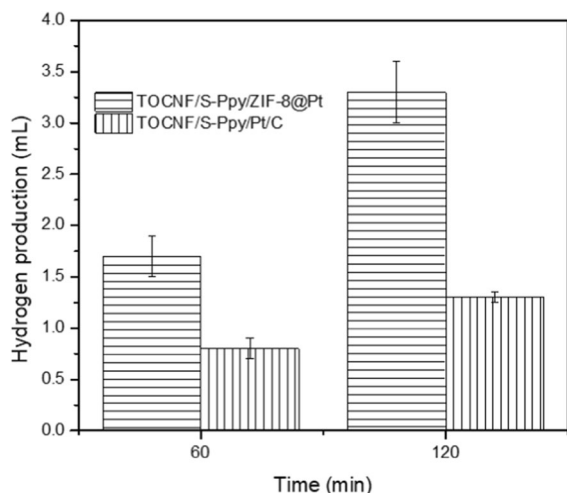


Fig. 9 Hydrogen production from TOCNF/S-Ppy/Pt@ZIF-8 and TOCNF/S-Ppy/Pt(40 wt%)/C electrodes (0.5×3 cm electrode films) at 1.5 V in $0.5 \text{ M H}_2\text{SO}_4$

network and a rough aggregate structure of Pt@ZIF-8 (Fig. 6A). Then electrons pass effectively through the TOCNF/S-Ppy/Pt@ZIF-8 electrode, but the electron-passing is not easy in an ATO-including electrode because of the compact morphology of ATO. The open structure of TOCNF/S-Ppy/Pt@ZIF-8 electrode may be available as gas channel (Fig. 6B). Moreover, the TOCNF/S-Ppy/Pt@ZIF-8 film electrode was more effective than Pt@ZIF-8 on a glassy carbon electrode. Thus, the former electrode is superior for practical application.

As shown in Fig. 9., the H_2 production rates of TOCNF/S-Ppy/Pt@ZIF-8 (2.8 wt% Pt content) and TOCNF/S-Ppy/Pt(40 wt%)/C were 1.7 mL/min H_2 and 0.8 mL/min H_2 , respectively, at 60 min; the H_2 production increased after 120 min. The results proved that Pt@ZIF-8 can produce more H_2 than Pt(40 wt%)/C. Moreover, the hydrogen generation on TOCNF/S-Ppy/Py@ZIF-8 was almost double (98%) at 120 min in comparison with it at 60 min, but it on TOCNF/S-Ppy/Pt(40 wt%)/C at 120 min was only 81% of double of amount at 60 min. This indicates that Pt in ZIF-8 is stable different from Pt(40 wt%)/C, which was simply adsorbed on TOCNF/S-Ppy. Thus, Pt@ZIF-8 is a good candidate as cost-effective, low Pt content and stable electrocatalyst for HER.

Conclusions

This work demonstrated the efficiency of an electrocatalyst on HER using Pt@ZIF-8, which has a platinum content of only 2.8 wt% and a Tafel slope of 36 mV/decade, keeping the distributed metal active sites in ZIF-8. The efficiency was comparable to a standard Pt(40 wt%)/C electrode, indicating that Pt@ZIF-8 has a merit of low amount of platinum. The electrocatalyst was deposited on flexible conducting substrate electrode via the layer-on-layer method. The potential of the substrate occurred by structural contribution of TOCNF/S-Ppy with better conductivity and void volume for electron transfer and gas diffusion in a comparison with TOCNF/ATO. Moreover, a TOCNF/S-Ppy/Pt@ZIF-8 electrode generated larger volume of H_2 gas than a Pt(40 wt%)/C electrode. As a result, it can be concluded that the material preparation based on catalyst-embedded MOF-coated conducting flexible film electrode promotes effective hydrogen generation. Thus, this report promises a future benefit in fuel cells development with improved cost performance.

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Authors' contribution NK managed conceptualization, NK, CK worked methodology, investigation, visualization, NK performed writing—original draft the manuscript, TI and CR-A played Supervision, and writing—review and editing the manuscript. CR-A managed funding acquisition.

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Declarations

Conflict of interest The authors report no declarations of interest.

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