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- (71) Applicant: AGENCIA ESTALAL CONSEJO SUPERI-OR DE INVESTIGACIONES CIENTIFICAS [ES/ES]; Calle Serrano 117, E-28006 Madrid (ES).
- (72) Inventors: PALACIN, Maria Rosa; Av. Joseph Tarradellas 235, 3r 2a., E-08901 L'hospitalet de Lobregat (ES). PONROUCH, Alexandre; Calle Nonell 3, 2° 4°, Cerdanyola del Vallès, E-08290 Barcelona (ES).
- (74) Agents: GOULARD, Sophie et al.; Ipsilon Brema-Loyer, Le Centralis, 63 avenue du Général Leclerc, F-92340 Bourg-la-Reine (FR).

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(54) Title: METHOD FOR PREPARING CARBON COATED ELECTRODE ACTIVE MATERIAL PARTICLES

(57) Abstract: The present invention is related to a method for preparing particles having a core made of an electrode active material, and a carbon coating Said method is based on a physical deposition of carbon, wherein the particles to be coated remain under dry conditions at a temperature lower than their decomposition temperature, during the whole process, hence avoiding all the drawbacks mentioned above and being generally applicable to all electrode active materials. Said method comprises the steps of: providing active material particles; coating said particles with a carbon film by a thermal vapor deposition (TVD) method using carbon as the carbon source; wherein the particles remain at a temperature lower than their decomposition temperature and under mechanical agitation during the coating process.

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# METHOD FOR PREPARING CARBON COATED ELECTRODE ACTIVE MATERIAL PARTICLES

The present invention is related to a method for preparing particles having a core made of an electrode active material, and a carbon coating.

#### **BACKGROUND OF THE INVENTION**

Batteries comprise a positive and a negative electrode which are electronically insulated from each other but in contact with an ionic conducting medium, the electrolyte. Except for metal electrodes (such as lithium anodes) electrodes are made of a metal current collector onto which a material is deposited by different means, said material comprising an active material and preferably some additives, such as a binder to ensure mechanical strength and an electronic conducting agent (for instance carbon black). Still, active materials must exhibit high intrinsic electronic and ionic conductivities in order to have acceptable reaction kinetics and hence to be able to operate at the required intensities. The higher the charge /discharge rates at which the battery is expected to operate, the larger electronic and ionic conductivities the electrodes must have.

Battery calendar life upon cycling is enhanced if side reactions, which result in slow degradation of the electrode/electrolyte interfaces, can be avoided. These energetically favored side reactions mostly involve charged electrode materials reacting with nonaqueous electrolytes. [J.B. Goodenough, Y. Kim. Chem. Mater. 22 (2010) 587]

A common practice, especially for low intrinsic conductivity electrode materials, such as LiFePO<sub>4</sub>, is to coat the particles surface with a conducting compound which can be a metal, a conducting polymer or, most generally, carbon [J. Wang, X. Sun, Energy & Environmental Science, 5 (2012) 5163]. Following this approach, the poor conductivity is alleviated by creating a conductive carbon coating layer on the active material particles with a minimal amount of adherent carbon (usually less than 2% in weight). [WO 02/27823 A1].

Furthermore, since carbon has a wide electrochemically stable window in organic electrolytes and has good chemical stability, carbon coatings do also prevent surface degradation in electrode materials and hence slow down the capacity fading upon battery cycling [B.L. Cushing, J.B. Goodenough, Solid State Sciences 4 (2002) 1487]. Other advantages of carbon coating include promoting a more uniform SEI (Solid Electrolyte Interphase) layer [C. Natarajan, H. Fujimoto, K. Tokumitsu, A. Mabuchi, T. Kasuh, Carbon 39 (2001) 1409] and buffering of

volume changes in active materials and hence circumventing the peeling-off of active material from the current collector due to cracking and pulverization [Y.J. Kwon, J. Cho, Chem. Commun 9 (2008) 1109].

Carbon coating on powdered active materials used for battery electrode fabrication is currently achieved through chemical procedures [H. Li and, H. Zhou. Chem Commun. 48 (2012) 1201]: (i) Chemical/Thermal Vapor deposition using toluene, benzene or an alternative carbon source, (ii) in situ growth of the carbon coating layer during the materials synthesis thanks to the addition of a carbon source to the reacting medium (e.g sucrose, citric acid) or (iii) a post-synthetic treatment involving either spray pyrolysis of a suspension containing the active material and a carbon source or mixing the powdered electrode active material with a carbon precursor using a liquid dispersing medium and performing thermolysis of the mixture in order to decompose the precursor into carbon at high temperatures (ca. 700°C), mostly under inert gas flow. These multi-step routes are of high cost and energy consuming and may be difficult to upscale. The carbon yield (the efficiency of conversion of precursor into carbon) is difficult to estimate a priori since it is quite independent of the initial mass ratio between the active particle and carbon precursor [J. Moskon, R. Dominko, R. Cerc-Korosec, M.Gaberscek, J. Jamnik. J. Power Sources 174 (2007) 683].

Theses procedures can be applied to a large variety of materials either for the positive or negative electrode and aim at best at achieving a uniform particle shell on the particle powders, which remain at the core. However, they are not applicable for electrode active materials i) which may decompose under the high temperatures needed to decompose the carbon precursor to achieve carbon coating or ii) which may be reduced under the thermal treatment conditions or for materials needing processing under oxidizing conditions which may lead to burn out of added organic precursors. If the electrode active material has a particle size in the nanometric range, the thermal treatment may also induce particle growth and/or agglomeration. Another drawback of such methods is the difficulty of coating materials that can dissolve in the liquid used to prepare the dispersion which will further be thermally treated. Finally, the control of the thickness and uniformity of the carbon layer is also a challenge since it depends on a large amount of parameters: the precursor used, its weight ratio and the homogeneity of the mixture, particle size of the active material etc. While a low amount of carbon precursor may form a thin but hardly a full coating layer on the particle surface, a too thick layer would act as a barrier for ion diffusion.

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Alternatively, ball milling with carbon is also a generally used procedure to promote intimate mixture which sometimes results in enhanced electrochemical properties. In these cases, no continuous conductive film of carbon is achieved but rather a nanocomposite. This can be considered as a variant of the traditional electrode preparation procedure where the active material is mixed with carbon black and a binder, rather than a technique to produce uniform carbon coating on particles.

Carbon evaporation under vacuum (around 10<sup>-2</sup> Pa) from a pre-shaped carbon rod of a woven thread of carbon fiber is known to produce conductive carbon coatings on samples to enable charge free imaging in electron microscopy and microprobe analysis, with a thickness of ca. 2 nm or more [K. Rüdiger-Peters. J. Microscopy 133 (1984) 17]. The technique was introduced by Bradley in the electron microscopy field and produces cohesive films covering even fissured surfaces [I.M. Watt. Cambridge University Press. (1997). ISBN-13: 978-0521435918]. Commercial evaporators are manufactured to that end by various companies but never used to apply a uniform carbon coating on powdered electrode active material.

US-6 733 923 discloses a method for preparing an electrode, said method comprising a step of preparing a composite electrode material containing an oxide, acetylene black as an electronic conducting agent and PVDF as a binder, a step of preparing a film of said composite material and a step of coating said film with carbon through different techniques for instance a heating deposition process. WO 2011/109457 also discloses a surface modified cathode and method of making surface modified cathode, said method comprising a step of coating the free surface of active material particles at the upper surface of a cathode film or the surface of active material particles facing the upper surface of the cathode.

However, in an electrode obtained according to these methods, only the surface of the electrode or only the part of the surface of the particles facing the upper surface is in contact with the carbon coating and not the whole surface of each individual particles, which remain partially uncoated, so the effect is only on the surface of the electrode but not on the bulk thereof.

In contrast, if each particle forming the electrode material was coated, thick (high energy density) electrodes with enhanced electronic conductivity could be manufactured, which would be suitable for battery operation at higher intensities (higher power density).

#### THE INVENTION

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The present invention intends to provide a method for the production of particles having an active material core and a carbon coating on the whole surface of each particles, said particles being then used to manufacture an electrode for a battery.

Said method is particularly useful for coating particles of an active material that would be degraded at temperatures needed to decompose carbon precursors to yield carbon coating the particles, either because the intrinsic decomposition temperature of said active material is lower than the temperature required for the pyrolitic decomposition of carbon precursor to yield carbon, or because said active material would be degraded under the conditions existing during the pyrolysis process such as the reducing atmosphere. Furthermore the method is particularly useful for particles of an active material that would dissolve in the solvent used for the traditional coating method involving a step where the carbon precursor is mixed with the active material using a liquid dispersing medium prior to pyrolysis.

The method of the present invention is based on a physical deposition of carbon, wherein the particles to be coated remain under dry conditions at a temperature lower than their decomposition temperature, during the whole process, hence avoiding all the drawbacks mentioned above and being generally applicable to all electrode active materials.

The method of the present invention comprises the steps of:

- providing active material particles;
- coating said particles with a carbon film by a physical vapor deposition (PVD) method using carbon as the carbon source;

#### 25 wherein:

- the particles remain at a temperature lower than their decomposition temperature, and
- the physical vapor deposition is a thermal vapor deposition method (TVD) comprising at least the following steps:
- an element made of carbon and surrounded by a metal filament, typically a tungsten filament, is present in a vacuum chamber;
  - ii) an active material in powder form is placed on a support in the vacuum chamber;
  - iii) the powder is agitated by mechanical means;

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- the vacuum chamber is put under vacuum at a pressure lower than 10<sup>-1</sup> Pa iv) (10<sup>-3</sup> mbar), more preferably lower than 10<sup>-2</sup> Pa (10<sup>-3</sup> mbar);
- a current is applied to the tungsten filament to heat the carbon and generate v) carbon vapor in the chamber.

With respect to methods currently used, mostly based on pyrolysis of carbon precursors, the method of the invention has the following advantages: it avoids heating the active material, it avoids submitting the active material to reducing conditions while hot and it avoids processing the active material in liquid medium. Thus, it is specially suited to thermally unstable materials, materials containing transition metals in high oxidation states which would be reduced during the pyrolysis of carbon precursors or materials reacting with liquids which cannot be coated by chemical means. Moreover, since there is no thermal treatment, particle growth is prevented and control of the amount of carbon (i.e. the thickness of the coating layer) is easy through control of deposition time. Furthermore, as the method is implemented at low temperature, the cost thereof is lower. Finally, as the coating is carried out under continuous mechanical agitation, all the sides of the particles are exposed to carbon and hence the claimed process leads to a coating of the whole surface of each individualized particles.

Although the method of the invention is particularly useful to prepare carbon coated particles having a core made of an active electrode material that is thermally unstable, it may be carried out to prepare carbon coated particles from all types of active materials generally used for either the cathode or the anode of various batteries, in particular for a lithium battery.

### Detailed description of the preferred embodiments

The method of the invention is particularly useful for the preparation of 25 electrode active materials that have low thermal stability and/or that may react with solvents.

Active cathode materials may be selected from:

- transition metal oxides having spinel or layered type structures such as  $\text{Li}_{1+x}M_{2-x}O_4$  with  $0 \le x \le 0.3$  or  $A_{1+x}M_{1-x}O_2$ , with  $0 \le x \le 0.3$ ; or
- oxides exhibiting a polyanionic framework with formula A<sub>v</sub>M(XO<sub>4</sub>)<sub>z</sub>F<sub>t</sub> with  $0 \le y \le 2$ ,  $1 \le z \le 1.5$ ,  $0 \le t \le 1$ ;
- lead sulphate

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 $Ni_{1-x}M'_x(OH)_2$  where M' is transition metal

where M is selected from Mn, Fe, Co, Ni, Cu, V, Ti, Mg, Al, Zn or a mixture of them, X is selected from S, P, or Si and A is either Na or Li.

Examples of active cathode materials that are unstable at temperatures required for coating methods involving pyrolysis of an organic carbon precursor are: nickel oxihydroxides or hydroxides as  $Ni_{1-x}M_x(OH)_2$  where M can be any transition metal, and lead sulphate.

Examples of active cathode materials that are unstable because they would degrade within the reducing atmosphere existing during the pyrolysis of an organic carbon precursor are layered  $A_{1+x}M_{1-x}O_2$  materials with  $0 \le x \le 0.3$  where M is a transition metal in high oxidation state. Examples are Li[Li<sub>0.2</sub>Mn<sub>0.5</sub>Ni<sub>0.15</sub>Co<sub>0.15</sub>O<sub>2</sub>], FePO<sub>4</sub> or any other compound containing Fe<sup>3+</sup> such as FeSO<sub>4</sub>F, and LiCoPO<sub>4</sub>.

LiCoPO<sub>4</sub> exhibits the same olivine structure as LiFePO<sub>4</sub> and an operation voltage that is 1.4 V higher than that of LiFePO<sub>4</sub>, but its electronic conductivity is much lower than that of LiFePO<sub>4</sub> and thus carbon coating is necessary. However, cobalt compounds being effective catalysts in the carbon gasification processes, the achievement of a coating through a process involving high temperature treatment is much more difficult since the added carbon can be consumed, causing reduction of LiCoPO<sub>4</sub> at the surface of the particles to  $Co_2P$  [J. Wolfenstine, J. Read, J.L. Allen. J. Power Sources 163 (2007) 1070].

Active cathode material that would dissolve or react with a solvent are LiFeSO<sub>4</sub>F and lithium or sodium transition metal fluorides where transition metal is iron, manganese or vanadium.

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A typical example is MFeSO<sub>4</sub>F (M=Li, Na or a mixture of both). LiFeSO<sub>4</sub>F exhibits interesting performances as positive electrode material for lithium ion batteries with reversible capacities around 140mAh/g at 3.6V vs. Li<sup>+</sup>/Li<sup>o</sup>. [N. Recham, J.N. Chotard, L. Dupont, C. Delacourt, W. Walker, M. Armand, J.M. Tarascon. Nat. Mater. 9 (2010) 68], [WO2010046610 A1]. However, LiFeSO<sub>4</sub>F is not stable at temperature higher than 350°C, which prevents any attempt of performing carbon coating on it by the usual methods involving higher temperatures to promote decomposition of the carbon precursors. Moreover, the compound cannot be processed in aqueous medium since it decomposes to yield FeOOH and LiF.

Active materials useful for an anode are preferably selected from silicon, tin, carbon, graphite, lithium titanium oxide, lithium vanadium oxide, sodium titanium oxide, sodium vanadium oxide, titanium oxide, cobalt oxide, iron oxide, copper oxide, nickel oxide, iron fluoride, lead sulphate or an organic electrode material.

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Active anode materials having a low decomposition temperature are lead sulphate and any organic electrode material [Y. Liang, Z. Tao, J. Chen. Advanced Energy Materials 2 (2012) 742] such as organosulfur compounds (RSSR where R can be any organic moiety) or organosulfur polymers containing disulfide or polysulfide bonds; organic free radical compounds, such as nitroxide-based polymers; or carbonyl compounds like sodium terephtalate, or lithium or sodium rhodizonate.

Active anode materials that are unstable because they would degrade within the reducing atmosphere existing during the pyrolysis of an organic carbon precursor are transition metal oxides such as Fe<sub>2</sub>O<sub>3</sub> or Co<sub>3</sub>O<sub>4</sub> [B. V. L'vov, Thermochim. Acta, 360 (2000) 109].

Active anode material that would dissolve or react in a solvent are organic electrode materials, sodium titanium oxide, sodium vanadium oxide.

The particle size of the active material is preferably in the range between 5 nm and 700 µm.

The carbon coating on the active material core of the carbon coated particles has preferably a thickness in the range of 1 to 20 nm.

According to the thermal vapor deposition method of the invention, when carbon vapor generated in the vacuum chamber is in contact with the surface of the powder particles which are at ambient temperature, carbon is deposited on the whole surface of the particles.

The deposition rate is regulated by means of the current applied and the thickness of the deposit depends on the deposition time. A higher current applied provides a higher deposition rate. A longer deposition time provides a thicker coating.

The deposition rate is preferably in the range of 0.05 to 0.4 nm/s. Deposition time can be varied allowing a direct control on the coating thickness. A deposition time in the range of 1 minute to 2 hours provides generally an efficient coating thickness.

The amount of active material particles put in the vacuum chamber depends on the size of said vacuum chamber.

The size of the active material particles is preferably in the range of 5 nm to 700 micrometers.

The carbon source is preferably a carbon rod or a woven thread of carbon fiber.

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Figure 1 is a high resolution transmission microscopy image of carbon coated LiFeSO $_4$ F particles.

Figure 2 is the X-ray diffraction pattern for the carbon coated LiFeSO<sub>4</sub>F (curve C) and uncoated LiFeSO<sub>4</sub>F (curve U), respectively.

Figures 3a and 3b are Mössbauer spectra for the uncoated LiFeSO<sub>4</sub>F and the carbon coated LiFeSO<sub>4</sub>F, respectively. T is the transmission and V is the velocity (in mm/s). The curves represented by 00000 and —— correspond to the experimental data and to the calculated data, respectively. The calculated data result from the addition of contributions for the Fe<sup>2+</sup> (1) and Fe<sup>2+</sup> (2) crystallographic sites of Fe<sup>2+</sup> in the LiFeSO<sub>4</sub>F tavorite structure represented by - - - - - and ———, respectively.

Figure 5 shows first cycle Potential (P, in V vs Li<sup>+</sup>/Li) versus capacity (C, in mAhg<sup>-1</sup>) profiles for tape electrodes prepared with coated LiFeSO<sub>4</sub>F (curve −□−□−□−□−□−□) and for tape electrodes prepared with uncoated LiFeSO<sub>4</sub>F (curve ▲ - ▲ - ▲ - ▲ - ), both cycled in 1M LiBOB in EC electrolyte at 100°C with a lithium metal counter electrode in Swagelok type cells.

Figure 7 is an expanded view of Figure 6.

Figure 8 represents the Nyquist plots with the imaginary (I) versus the real components (R) of the impedance, plotted for various frequencies (ranging from 500 kHz to 50 mHz) for powder electrodes prepared with carbon coated (\(\sigma \sigma \sigma \sigma \sigma)\) and for powder electrodes prepared with uncoated (\(\sigma \sigma \sigma \sigma)\) LiFeSO<sub>4</sub>F. Electrochemical impedance spectroscopy measurements were performed in 3 electrode Swagelok cells at room temperature using LP30 electrolyte and lithium metal counter and reference electrodes.

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Figure 9 is a high resolution transmission microscopy image of carbon coated  $LiCoPO_4$ .

Figure 10 shows first cycle Potential (P, in V vs Li<sup>+</sup>/Li) versus capacity (C, in mAhg<sup>-1</sup>) profiles for tape electrodes prepared with coated LiCoPO<sub>4</sub> (curve 5 -□-□-□-□-□-□) and for tape electrodes prepared with uncoated LiCoPO<sub>4</sub> (curve ▲ - ▲ - ▲ - ▲ - ), both cycled in LP30 electrolyte at room temperature with a lithium metal counter electrode in Swagelok type cells.

Figure 11 represents a) the Coulombic efficiency CE (in %) and b) the capacity retention CR (%) versus the number of cycles N for tape electrodes prepared with carbon coated  $LiCoPO_4$  ( $\square\square\square\square\square\square\square\square$ ) and for tape electrodes prepared with uncoated  $LiCoPO_4$  ( $\blacktriangle \blacktriangle \blacktriangle$ ) cycled in LP30 electrolyte at room temperature with a lithium metal counter electrode in Swagelok type cells.

Figure 12 shows high resolution transmission microscopy images of carbon coated Co<sub>3</sub>O<sub>4</sub> nanoparticles with (a) 5 minutes, (b) 15 minutes and (c) 30 minutes deposition time.

Figure 14 represents the capacity (C, in mAhg<sup>-1</sup>) versus the number of cycles N for tape electrodes prepared with carbon coated  $Co_3O_4$  ( $\square\square\square\square\square\square\square\square$ ) with 5 minutes deposition time and for tape electrodes prepared with uncoated  $Co_3O_4$  ( $\triangle \triangle \triangle \triangle \triangle$ ), both cycled in LP30 at room temperature with a lithium metal counter electrode in Swagelok type cells.

Figure 15 shows a picture of  $\text{Li}_4\text{Ti}_5\text{O}_{12}$  powder (a) uncoated, and of carbon coated  $\text{Li}_4\text{Ti}_5\text{O}_{12}$  powder after a deposition time of 10 minutes (b), 20 minutes (c) and 30 minutes (d).

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Figure 16 is a high resolution transmission microscopy image of carbon coated  $\mathrm{Li}_4\mathrm{Ti}_5\mathrm{O}_{12}$ .

Figure 17 shows the Potential (P, in V vs  $\text{Li}^+/\text{Li}$ ) versus capacity (C, in mAhg<sup>-1</sup>) profiles for tape electrodes prepared with a) coated  $\text{Li}_4\text{Ti}_5\text{O}_{12}$  and for tape electrodes prepared with b) uncoated  $\text{Li}_4\text{Ti}_5\text{O}_{12}$  both cycled in LP30 at room temperature at rates ranging from C/5 to 8C.

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Figure 18 represents the capacity (C, in mAhg<sup>-1</sup>) versus the number of cycles (N) for tape electrodes prepared with carbon coated Li<sub>4</sub>Ti<sub>5</sub>O<sub>12</sub> ( $\square\square\square\square\square$ ) and for tape electrodes prepared with uncoated Li<sub>4</sub>Ti<sub>5</sub>O<sub>12</sub> ( $\blacktriangle \blacktriangle \blacktriangle$ ), both cycled in LP30 at room temperature with a lithium metal counter electrode in Swagelok type cells.

Figure 19 is a high resolution transmission microscopy image of carbon coated sodium rhodizonate particles.

Figure 20 is a high resolution transmission microscopy image of carbon coated Sn particles.

Figure 21 is a high resolution transmission microscopy image of carbon coated Si particles.

Figure 23 is a high resolution transmission microscopy image of carbon coated Ni(OH)<sub>2</sub> particles.

Figure 24 is a high resolution transmission microscopy image of carbon coated Na<sub>2</sub>Ti<sub>3</sub>O<sub>7</sub> particles.

Figure 25 is a high resolution transmission microscopy image of carbon coated LiFePO<sub>4</sub> particles.

#### **EXAMPLES**

The products used in the examples are:

EC

	25	PVDF	polyvinylidene fluoride, provided by Arkema
		Csp	Super P carbon, provided by Timcal
		NMP	N-methylpyrrolidone, provided by Sigma-Aldrich
		Al foil	a 20 µm thick aluminum foil provided by Goodfellow
		Li foil	a lithium foil provided by Chemetall
30		Whattman GF/d	a borosilicate glass fiber provided by Whattman
		LP30	a 1M LiPF <sub>6</sub> in EC:DMC 1:1 electrolyte provided by Merck
		LiBOB	Lithium bis(oxalato)borate by Chemetall

ethylene carbonate provided by Sigma-Aldrich

LiCoPO<sub>4</sub> provided by Sigma-Aldrich
Co<sub>3</sub>O<sub>4</sub> provided by Sigma-Aldrich
Li<sub>4</sub>Ti<sub>5</sub>O<sub>12</sub> provided by Sigma-Aldrich
Sodium rhodizonate provided by Sigma-Aldrich
5 Sn provided by Sigma-Aldrich
Si provided by Sigma-Aldrich

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LiFeSO<sub>4</sub>F is prepared as by ionothermal synthesis starting from FeSO<sub>4</sub>·H<sub>2</sub>O and LiF as described in N. Recham, J.N. Chotard, L. Dupont, C. Delacourt, W. Walker, M. Armand, J.M. Tarascon. Nat. Mat. 9 (2010) 68.

Hard C is prepared by pyrolysis of sugar as described in A. Ponrouch, E. Marchante, M. Courty, J.M. Tarascon, M. R. Palacín. Energy&Environmental Science 2012, 5, 8572-83.

Ni(OH)<sub>2</sub> is prepared by direct precipitation after mixing a 1M solution of nickel sulphate hexahydrate and 2M solution of sodium hydroxide as described in M. Casas-Cabanas, J. Rodríguez-Carvajal, J. Canales-Vázquez, M.R. Palacín. J. Mater. Chem. 2006, 16, 2925-2939.

 $Na_2Ti_3O_7$  is prepared by solid state reaction between  $TiO_2$  and  $Na_2CO_3$  at 800°C as described in P. Senguttuvan, G. Rousse, V. Seznec, J.M. Tarascon, M.R. Palacín. Chem. Mater., 2011, 23, 4109.

LiFePO<sub>4</sub> is prepared by solid state reaction between LiH<sub>2</sub>PO<sub>4</sub> and FeC<sub>2</sub>O<sub>4</sub>·2H<sub>2</sub>O by two successive thermal treatments at 350 and 800°C as described in S.S Zhang, J.L Allen, K Xu, T.R Jow, J. Power Sources, 2005, 147, 234.

In each example, the coated particles were prepared using a high vacuum coating system provided under the trade name Bal-Tec Med 020, by Leica 25 Microsystems. Said device comprises a clean high-vacuum pump in combination with a removable vacuum chamber, rotary-planetary-tilting sample holder and quartz crystal film thickness monitor system. A system allowing continuous mechanical agitation of the particles during the coating process has been added, said system consisting of a spatula fixed to the deposition chamber in direct contact with the rotary-planetary-tilting sample holder. The deposition rate was measured through a quartz crystal film inside the vacuum chamber and hence was directly read.

# Example 1 Carbon coated LiFeSO<sub>4</sub>F

## Preparation of the carbon coated particles

Carbon coated LiFeSO $_4$ F was prepared using the above mentioned Bal-Tec 5 Med 020 coating system.

An amount of 600 mg of LiFeSO<sub>4</sub>F having a particle sizes ranging from 50 to 400 nm was put in the vacuum chamber. The carbon source in the vacuum chamber was a carbon rod, the pressure in the vacuum chamber was about  $10^{-2}$  Pa ( $10^{-4}$  mbar) .The deposition time was around 2 hours. The deposition rate was around 0.1 nm/s.

The high resolution transmission microscopy represented on figure 1 shows that the resulting carbon coated particles have a uniform coating of about 20 nm.

### Mössbauer spectroscopy and X-ray diffraction

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Mössbauer spectroscopy and X-ray diffraction analysis were performed before and after carbon coating. They indicate that neither the structure nor the oxidation state of iron in the compound are modified by the carbon coating process. The iron XRD pattern (represented on figure 2) does not change and the Mössbauer spectra (represented on figure 3) are identical. The Mössbauer spectra were fitted with two doublets in accordance with the two crystallographic sites of Fe<sup>2+</sup> in the tavorite LiFeSO<sub>4</sub>F structure and the Mössbauer parameters are identical to those already reported for that phase. No trace of Fe<sup>3+</sup> is detected.

The Raman spectrum (represented on figure 4) for carbon coated LiFeSO<sub>4</sub>F powder exhibits two broad bands at 1350 and 1580 cm<sup>-1</sup> (D and G bands of carbon). The ratio between them allows evaluating the degree of disorder in the carbon as previously reported for carbon coated LiFePO<sub>4</sub>. [M. M. Doeff, Y. Hu, F. Mc Larnon, R. Kostecki, Electrochem. Solid-State Lett. 6 (2003) A207], for which a D/G ratio of ca. 2 or lower has been found to be optimum. In this case, a D/G bands ratio of ca. 1.5 was calculated from figure 4, indicating a high degree of graphitization of the carbon coated layer and thus high electronic conductivity.

### 30 Preparation of "tape" electrodes

Slurries were prepared by mixing 80wt.% of the active material with or without carbon coating, 5wt.% of PVDF as a binder and 15wt.% of Csp as carbon additive in NMP. Mixing of the slurries was performed by magnetic stirring during 3 h, the vial containing the slurry being placed in an ultrasonic bath for 10 minutes every 1 h.

Composite electrodes were prepared by depositing the slurry on a 20  $\mu m$  thick aluminum foil with a 250  $\mu m$  Doctor-Blade and further dried at 120 °C under vacuum. Once dried, 0.8 cm<sup>2</sup> disk electrodes were cut and pressed at 7.8 · 10<sup>8</sup> Pa.

### Electrochemical testing

Tape" electrodes were tested in Swagelok type cells [D. Guyomard, J.M. Tarascon. J. Electrochem. Soc. 139 (1992) 937] with a disk of Li metal foil as counter electrode. Two sheets of Whattman GF/d borosilicate glass fiber were used as a separator, soaked with the electrolyte (ca. 0.5 cm³ of 1M LiBOB in ethylene carbonate (EC). Electrochemical experiments were made at 100°C to promote electrolyte decomposition and better evaluate the impact of carbon coating reactivity of the active material with the electrolyte. These experiments were done in galvanostatic mode with potential limitation (GCPL) at a C/20 rate, meaning one mol of Li<sup>+</sup> per mol of LiFeSO<sub>4</sub>F inserted in 20 hours. Almost full theoretical capacity (i.e. 151 mAhg<sup>-1</sup>) is obtained in both cases for first oxidation (see figure 5). Better coulombic efficiency (difference of capacity recorded between the discharge and charge) is achieved in the case of carbon coated LiFeSO<sub>4</sub>F with ca. 73.5% compared to 65.7% for uncoated LiFeSO<sub>4</sub>F.

Cyclic voltamperommetry at 1 mVs<sup>-1</sup> was also performed. Significant oxidation current is measured above 4 V vs Li<sup>+</sup>/Li in both cases due to the electrolyte decomposition at the interface with the active material (cf. figure 6). The current intensity for such decomposition is decreased for carbon coated LiFeSO<sub>4</sub>F and the onset potential significantly shifted to higher values, being observed at 4.31V for carbon coated LiFeSO<sub>4</sub>F and at 4.18V for uncoated LiFeSO<sub>4</sub>F (cf. figure 7). These results confirms the full coverage of LiFeSO<sub>4</sub>F particles by carbon coating.

### Preparation of powder type electrodes and electrochemical impedance

Powder type electrodes were prepared by simple mixing the carbon coated LiFeSO<sub>4</sub>F with Csp in a weight ratio of 80/20, in an agate mortar for 15 min.

Said electrodes (typical loading ca.  $7 \pm 1$  mg) were used for electrochemical impedance tests at room temperature in three electrode Swagelok type cells with a disk of Li metal foil as counter and reference electrodes. Two sheets of Whattman GF/d borosilicate glass fiber were used as a separator, soaked with the electrolyte (ca.  $0.5 \text{ cm}^3$  of LP30). The charge transfer resistance in the carbon coated sample appeared to be significantly reduced, demonstrating the improved electronic conductivity of the carbon coated particles compared with the uncoated particles (cf. figure 8).

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## Example 2 Carbon coated LiCoPO<sub>4</sub>

### Preparation of carbon coated particles

Carbon coated LiCoPO<sub>4</sub> were prepared according to the method described in example 1, using 600 mg of LiCoPO<sub>4</sub> having a particle sizes ranging from 100 nm to 1µm, and a deposition time of around 30 minutes

The resulting carbon coated particles have a uniform coating of about 5 nm, as shown on figure 9. A gradual change in coloration was observed upon carbon deposition from purple for the uncoated powder to grey for the coated sample.

### Preparation of "tape" electrodes

Tape electrode were prepared using the coated and the uncoated LiCoPO<sub>4</sub> particles according to method described in Example 1.

### Electrochemical testing

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"Tape" electrodes were tested in Swagelok type cells with a disk of Li metal foil as counter electrode. Two sheets of Whattman GF/d borosilicate glass fiber were used as a separator, soaked with the electrolyte (ca. 0.5 cm<sup>3</sup> LP30) at room temperature. These experiments were done in galvanostatic mode with potential limitation (GCPL) at a C/20 rate, meaning one mol of Li<sup>+</sup> per mol of LiCoPO<sub>4</sub> inserted in 20 hours.

High capacity is observed upon first oxidation (ca. about 120 mAhg<sup>-1</sup>) for both coated and uncoated LiCoPO<sub>4</sub> (cf figure 10). Higher coulombic efficiency (58.2%) is achieved for carbon coated LiCoPO<sub>4</sub> when compared to uncoated LiCoPO<sub>4</sub> (46.8%). Better capacity retention upon cycling is also observed for the former (cf. figure 11).

## Example 3 Carbon coated Co<sub>3</sub>O<sub>4</sub>

### Preparation of carbon coated particles

Carbon coated Co<sub>3</sub>O<sub>4</sub> were prepared according to the method described in example 1, using 600 mg of Co<sub>3</sub>O<sub>4</sub> having a particle sizes ranging from 30 to 40 nm. 30

Transmission electron microscopy images taken on samples after 5, 15 and 30 min deposition time are given in figure 12. They show the evolution of the deposit thickness, which correspond respectively to 1, 2 and 4 nm.

### Preparation of "tape" electrodes

Slurries were prepared by mixing 65wt.% of the active material with or without carbon coating, 8wt.% of PVDF as a binder and 27wt.% of Csp as carbon additive in NMP. Mixing of the slurries was performed by magnetic stirring during 3 h, the vial containing the slurry being placed in an ultrasonic bath for 10 minutes every 1 h.

Composite electrodes were prepared by depositing the slurry on a 20  $\mu m$  thick copper foil with a 250  $\mu m$  Doctor-Blade and further dried at 120 °C under vacuum. Once dried, 0.8 cm<sup>2</sup> disk electrodes were cut and pressed at 7.8  $10^8$  Pa.

### 10 Electrochemical testing

"Tape" electrodes were tested in Swagelok type cells with a disk of Li metal foil as counter electrode. Two sheets of Whattman GF/d borosilicate glass fiber were used as a separator, soaked with the electrolyte (ca. 0.5 cm³ LP30) at room temperature. These experiments were done in galvanostatic mode with potential limitation (GCPL) with a succession of 10 cycles at different C rates. First, 10 cycles were performed at C/5 followed by 10 cycles at C, C/5, 2C and finally C/5. Results are shown on figures 13 and 14.

The first cycle for both carbon coated and uncoated Co<sub>3</sub>O<sub>4</sub> are very similar in terms of capacity, coulombic efficiencies and voltage hysteresis (cf. figure 13a). However, the electrode prepared with carbon coated Co<sub>3</sub>O<sub>4</sub> exhibits lower overpotential between discharge and charge at the end of the first reduction (cf. figure 13b). This is in agreement with the conductivity of carbon coated particles higher than the conductivity of the uncoated particles. A much better capacity retention is observed for carbon coated Co<sub>3</sub>O<sub>4</sub> with a stable capacity of about ca. 1200 mAhg<sup>-1</sup> achieved at C/5 after 90 cycles (cf. figure 14). Very good capacity retention is also observed at higher rates for carbon coated Co<sub>3</sub>O<sub>4</sub> with capacities higher than 700 mAhg<sup>-1</sup> at 2C, compared to only 300 mAhg<sup>-1</sup> for uncoated Co<sub>3</sub>O<sub>4</sub>. Since the non-uniform growth of a gel like film upon cycling, limits the diffusion of Li<sup>+</sup> within the electrode and induces capacity fade in electrodes prepared using Co<sub>3</sub>O<sub>4</sub> nanoparticles as active materials [A. Ponrouch and M.R. Palacín, J. Power Sources, 212 (2012) 233], it is straightforward to conclude that carbon coating on Co<sub>3</sub>O<sub>4</sub> nanoparticles allows the growth of more uniform gel like film and therefore a better diffusion of Li<sup>+</sup> through the bulk of the electrode.

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# Example 4 Carbon coated Li<sub>4</sub>Ti<sub>5</sub>O<sub>12</sub>

Carbon coated  $\text{Li}_4\text{Ti}_5\text{O}_{12}$  was prepared according to the method of example 1. An amount of 600 mg of  $\text{Li}_4\text{Ti}_5\text{O}_{12}$  having a particle sizes ranging from 10 to 100 nm was put in the vacuum chamber. The carbon source in the vacuum chamber was a carbon rod, the pressure in the vacuum chamber was about  $10^{-2}\,\text{Pa}$  ( $10^{-4}$  mbar). The deposition rate was around 0.1 nm/s.

A gradual change in coloration was observed upon carbon deposition from white for the uncoated powder to grey for the coated sample. Figure 15 shows the change of color from uncoated Li<sub>4</sub>Ti<sub>5</sub>O<sub>12</sub> powder (a), and of carbon coated Li<sub>4</sub>Ti<sub>5</sub>O<sub>12</sub> powder after a deposition time of 10 minutes (b), 20 minutes (c) and 30 minutes (d). After 30 minutes deposition time, the resulting carbon coated particles have a uniform coating of about 4 nm, as shown on figure 16.

### Preparation of "tape" electrodes

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Slurries were prepared by mixing 65wt.% of the active material with or without carbon coating, 8wt.% of PVDF as a binder and 27wt.% of Csp as carbon additive in NMP. Each slurry was mixed by magnetic stirring during 3 h, the vial containing the slurry being placed in an ultrasonic bath for 10 minutes every 1 h.

Composite electrodes were prepared by depositing the slurry on a 20  $\mu$ m thick copper foil with a 250  $\mu$ m Doctor-Blade and further dried at 120 °C under vacuum. Once dried, 0.8 cm<sup>2</sup> disk electrodes were cut and pressed at 7.8 · 10<sup>8</sup> Pa.

### Electrochemical testing

"Tape" electrodes were tested in Swagelok type cells with a disk of Li metal foil as counter electrode. Two sheets of Whattman GF/d borosilicate glass fiber were used as a separator, soaked with the electrolyte (ca. 0.5 cm³ LP30) at room temperature. These experiments were done in galvanostatic mode with potential limitation (GCPL) with a succession of 6 cycles at different C rates. First, 6 cycles were performed at C/5 followed by 10 cycles at C, C/5, 2C, C/5, 5C, C/5, 8C and finally C/5. Results are shown on figure 17 and 18.

The first cycle for both electrodes appeared to be very similar in terms of capacity, coulombic efficiencies and voltage hysteresis (cf. figure 17) for coated and uncoated Li<sub>4</sub>Ti<sub>5</sub>O<sub>12</sub>. The voltage hysteresis between charge and discharge at high C rates is much lower for carbon coated Li<sub>4</sub>Ti<sub>5</sub>O<sub>12</sub> in agreement with higher electronic conductivity. Upon cycling a much better capacity retention is observed for carbon coated Li<sub>4</sub>Ti<sub>5</sub>O<sub>12</sub> with a stable capacity of about ca. 155 mAhg<sup>-1</sup> achieved at C/5 compared to only 140 mAhg<sup>-1</sup> for uncoated Li<sub>4</sub>Ti<sub>5</sub>O<sub>12</sub>. Very good

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capacity retention at high C rates is also achieved for carbon coated  $\text{Li}_4\text{Ti}_5\text{O}_{12}$  with capacities higher than 135 mAhg<sup>-1</sup> obtained at 8C compared to 120 mAhg<sup>-1</sup> for uncoated  $\text{Li}_4\text{Ti}_5\text{O}_{12}$ .

# Example 5 Carbon coated sodium rhodizonate

### Preparation of carbon coated particles

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Carbon coated sodium rhodizonate was prepared according to the method described in example 1, using 600 mg of sodium rhodizonate having a particle size ranging from 500 nm to  $10\mu m$ , and a deposition time of around 30 minutes.

The resulting carbon coated particles have a uniform coating of about 3 nm, as shown on figure 19. A gradual change in coloration was observed upon carbon deposition from dark green for the uncoated powder to dark grey for the coated sample.

# Example 6 Carbon coated Sn

### Preparation of carbon coated particles

Carbon coated Sn was prepared according to the method described in example 1, using 600 mg of Sn having a particle size ranging from 30 nm to 500 nm, and a deposition time of around 30 minutes.

The resulting carbon coated particles have a uniform coating of about 3 nm, as shown on figure 20.

# Example 7 Carbon coated Si

### Preparation of carbon coated particles

Carbon coated Si was prepared according to the method described in example 1, using 600 mg of Si having a particle size ranging from 200 nm to 5  $\mu$ m, and a deposition time of around 30 minutes.

The resulting carbon coated particles have a uniform coating of about 4 nm, as shown on figure 21.

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# Example 8 Carbon coated hard carbon

### Preparation of carbon coated particles

Carbon coated hard carbon was prepared according to the method described in example 1, using 600 mg of hard carbon having a particle size ranging from 1 to 500µm, and a deposition time of around 30 minutes.

### Preparation of "tape" electrodes

Tape electrode were prepared using the coated and the uncoated hard carbon particles according to method described in Example 1.

### 10 Electrochemical testing

"Tape" electrodes were tested in Swagelok type cells with a disk of Na metal foil as counter electrode. Two sheets of Whattman GF/d borosilicate glass fiber were used as a separator, soaked with the electrolyte (ca. 0.5 cm<sup>3</sup> 1M NaClO<sub>4</sub> in EC<sub>0.45</sub>:PC<sub>0.45</sub>:DMC<sub>0.1</sub>) at room temperature. These experiments were done in galvanostatic mode with potential limitation (GCPL) at a rate equivalent to one mol of Na<sup>+</sup> per six moles of hard carbon inserted in 10 hours.

High capacity is observed upon first reduction (ca. about 500 mAhg<sup>-1</sup>) for both coated and uncoated hard carbon (cf figure 22) but higher coulombic efficiency (70%) is achieved for carbon coated hard carbon when compared to uncoated hard carbon (60%) in agreement with the coating diminishing electrolyte decomposition.

# Example 9 Carbon coated Ni(OH)<sub>2</sub>

### Preparation of carbon coated particles

Carbon coated Ni(OH)<sub>2</sub> was prepared according to the method described in example 1, using 600 mg of Ni(OH)<sub>2</sub> having a particle size ranging from 10 nm to 200 nm, and a deposition time of around 1 hour.

The resulting carbon coated particles have a uniform coating of about 8 nm, as shown on figure 23.

# Example 10 Carbon coated Na<sub>2</sub>Ti<sub>3</sub>O<sub>7</sub>

### Preparation of carbon coated particles

Carbon coated Na<sub>2</sub>Ti<sub>3</sub>O<sub>7</sub> was prepared according to the method described in example 1, using 600 mg of Na<sub>2</sub>Ti<sub>3</sub>O<sub>7</sub> having a particle size ranging from 500 nm to 5 µm, and a deposition time of around 5 minutes.

The resulting carbon coated particles have a uniform coating of about 3 nm, as shown on figure 24.

# Example 11 Carbon coated LiFePO<sub>4</sub>

## Preparation of carbon coated particles

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Carbon coated LiFePO<sub>4</sub> was prepared according to the method described in example 1, using 600 mg of LiFePO<sub>4</sub> having a particle size ranging from 1 to 50  $\mu$ m, and a deposition time of around 5 minutes.

The resulting carbon coated particles have a uniform coating of about 3 nm, as shown on figure 25.

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#### **CLAIMS**

- 1. A method for preparing particles having a core made of an electrode active material and a carbon coating, characterized in that said method comprises the steps of:
- 5 providing active material particles;
  - coating said particles with a carbon film by a physical vapor deposition (PVD) method using carbon as the carbon source;

#### wherein

- the particles remain are at a temperature lower than their decomposition temperature; and
  - the physical vapor deposition is a thermal vapor deposition method (TVD) comprising at least the following steps:
  - i) an element made of carbon and surrounded by a metal filament, typically a tungsten filament, is present in a vacuum chamber;
- 15 ii) an active material in powder form is placed on a support in the vacuum chamber;
  - iii) the powder is agitated by mechanical means;
  - iv) the vacuum chamber is put under vacuum at a pressure lower than 10<sup>-1</sup> Pa (10<sup>-3</sup> mbar), more preferably lower than 10<sup>-2</sup> Pa (10<sup>-3</sup> mbar);
- 20 v) a current is applied to the tungsten filament to heat the carbon and generate carbon vapor in the chamber.
  - 2. The method of claim 1, wherein the deposition rate is controlled by means of the current applied, a higher current applied providing a higher deposition rate.
- 25 3. The method of claim 1 or 2, wherein thickness of the deposit is controlled by the deposition time, a longer deposition time providing a thicker coating.
  - 4. The method of claim 3, wherein the deposition rate is in the range of 0.05 to 0.4 nm/s.
- 5. The method of claim 3, wherein the deposition time in the range of 1 minute to 2 hours.
  - 6. The method of claim 1, wherein the size of the active material particles to be coated is in the range of 5 nm to 700  $\mu$ m.

7. The method of claim 1, wherein the element made of carbon is a carbon rod or a woven thread of carbon fiber.

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- 8. The method of claim 1, characterized in that the electrode active material is a cathode active material selected from:
- 5 transition metal oxides having spinel or layered type structures such as  $\text{Li}_{1+x}M_{2-x}O_4$  with  $0 \le x \le 0.3$  or  $A_{1+x}M_{1-x}O_2$ , with  $0 \le x \le 0.3$ ; or
  - oxides exhibiting a polyanionic framework with formula  $A_yM(XO_4)_zF_t$  with  $0 \le y \le 2, 1 \le z \le 1.5, 0 \le t \le 1$ ;
  - lead sulphate;
- 10  $Ni_{1-x}M'_x(OH)_2$  where M' is transition metal; and

where M is selected from Mn, Fe, Co, Ni, Cu, V, Ti, Mg, Al, Zn or a mixture of them, X is selected from S, P, or Si and A is either Na or Li.

9. The method of claim 1, characterized in that the electrode active material is an anode material selected from silicon, tin, carbon, graphite, lithium titanium oxide, lithium vanadium oxide, sodium titanium oxide, sodium vanadium oxide, titanium oxide, cobalt oxide, iron oxide, copper oxide, nickel oxide, iron fluoride, lead sulphate or an organic electrode material.

Fig. 1

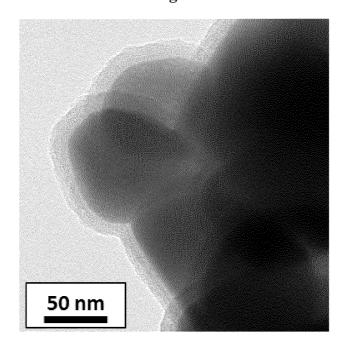


Fig. 2

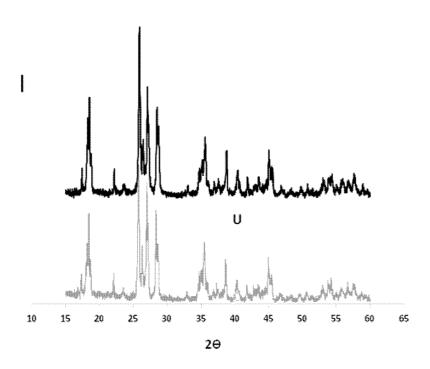


Fig. 3

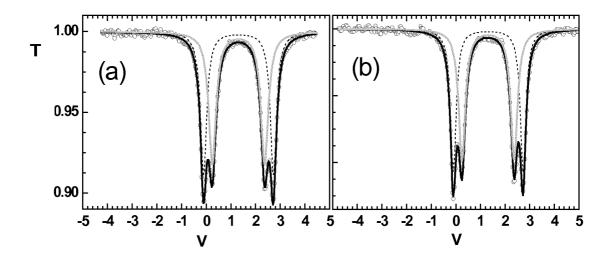


Fig. 4

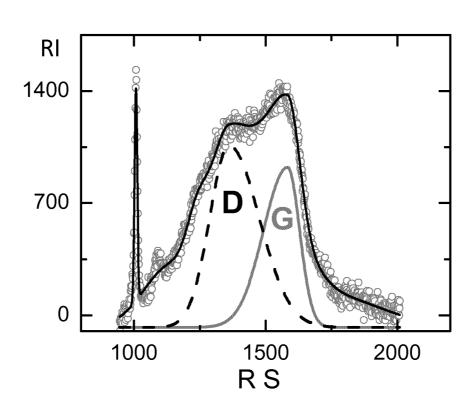


Fig. 5

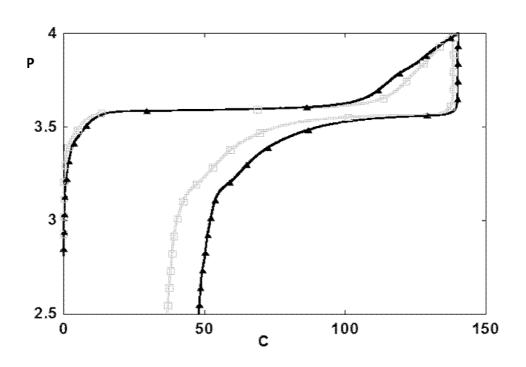
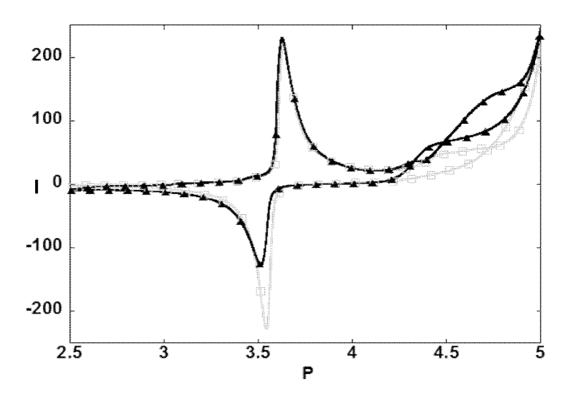


Fig. 6



**Fig. 7** 

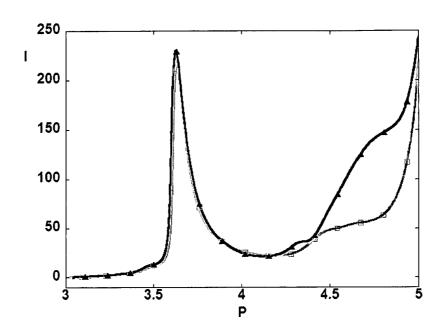


Fig. 8

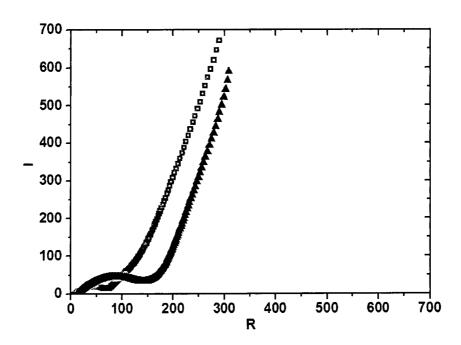


Fig. 9

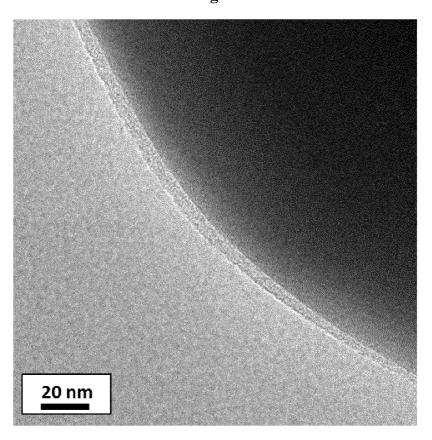
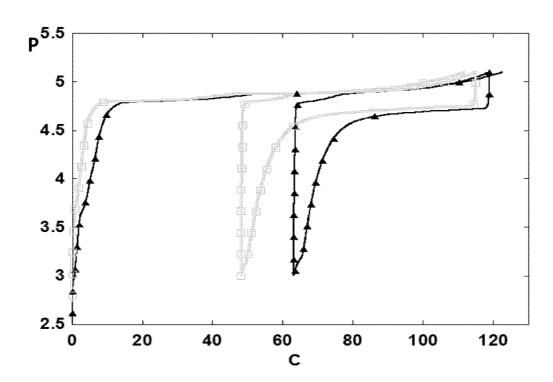


Fig. 10



**Fig. 11** 

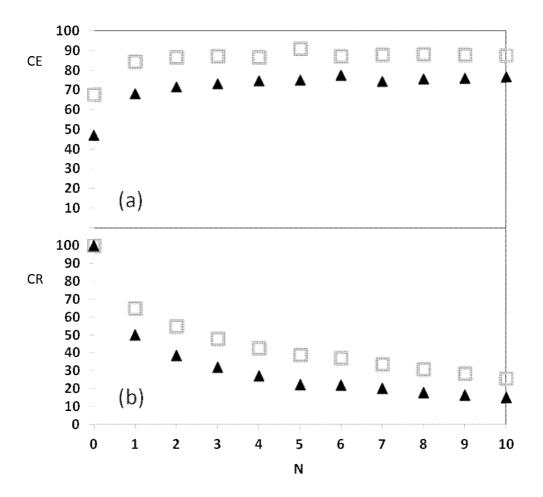


Fig. 12

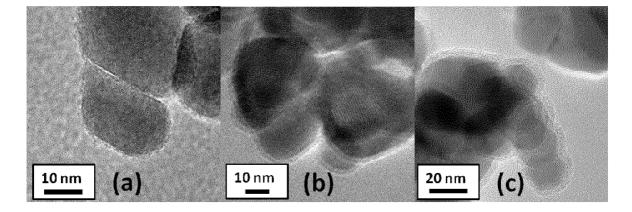


Fig. 13

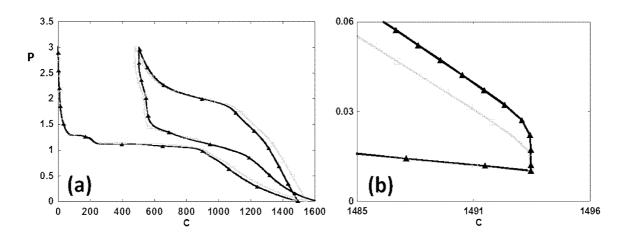


Fig. 14

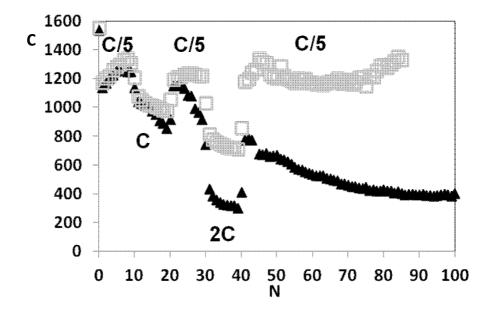


Fig. 15

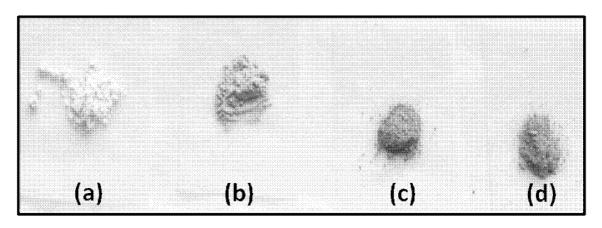


Fig. 16

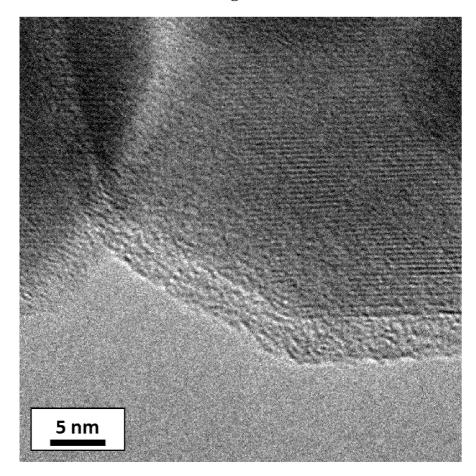


Fig. 17

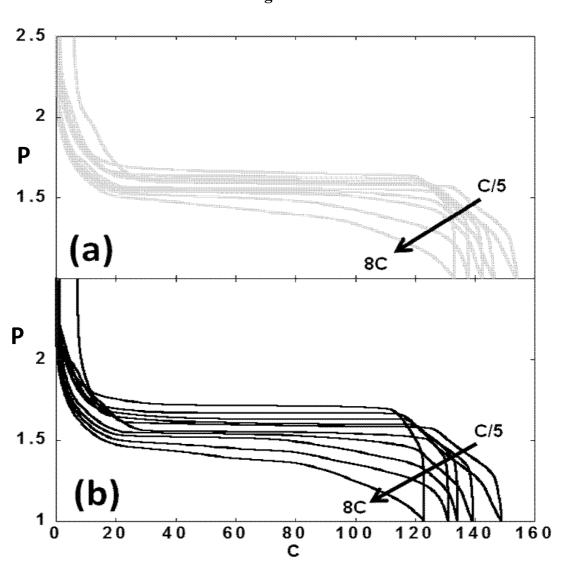


Fig. 18

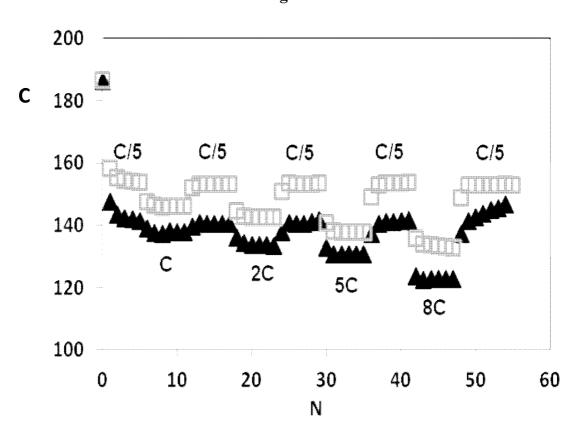


Fig. 19

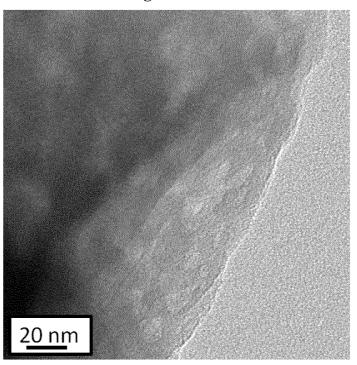


Fig. 20

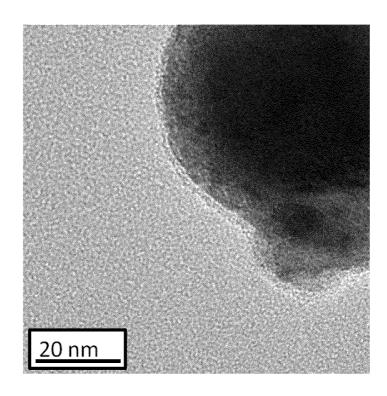


Fig. 21

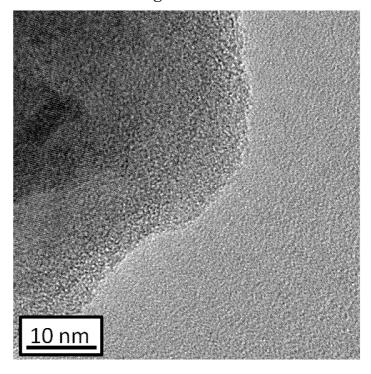


Fig. 22

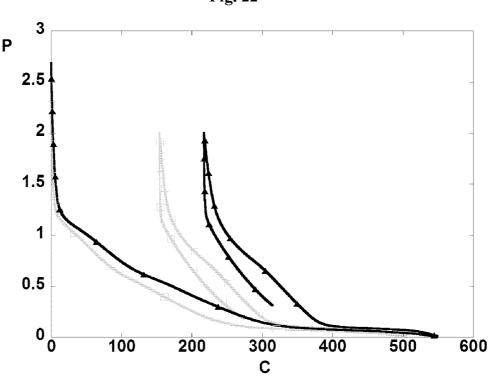


Fig. 23

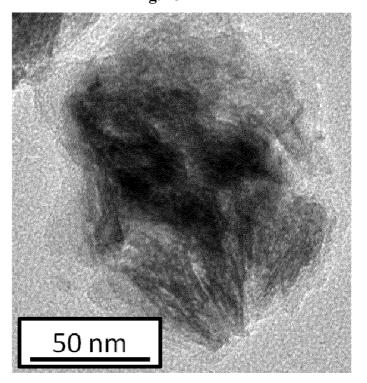


Fig. 24

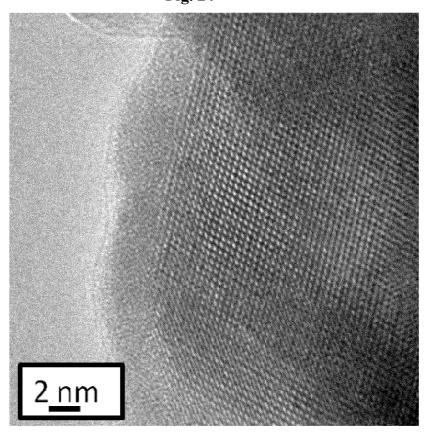
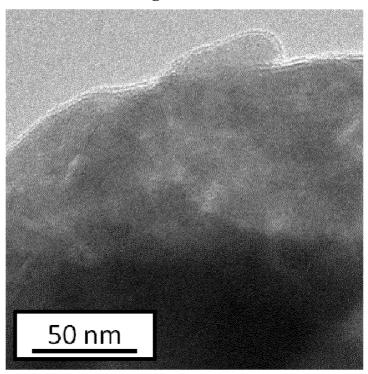


Fig. 25



#### **INTERNATIONAL SEARCH REPORT**

International application No
PCT/EP2013/068107

A. CLASSIFICATION OF SUBJECT MATTER INV. H01M10/0525 H01M4/485 H01M4/505 H01M4/525 H01M4/587 H01M4/36

ADD.

According to International Patent Classification (IPC) or to both national classification and IPC

#### B. FIELDS SEARCHED

Minimum documentation searched (classification system followed by classification symbols)  $\mbox{H}01\mbox{M}$ 

Documentation searched other than minimum documentation to the extent that such documents are included in the fields searched

Electronic data base consulted during the international search (name of data base and, where practicable, search terms used)

EPO-Internal, WPI Data

Category*	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
A	WO 2011/109457 A2 (UNIV TEXAS [US]; MANTHIRAM ARUMUGAM [US]; LIU JUN [US]; JAYAN BABY REE) 9 September 2011 (2011-09-09) paragraph [0094] - paragraph [0099]; figures 18-20	1-9
A	US 6 733 923 B2 (YUN KYUNG-SUK [KR] ET AL) 11 May 2004 (2004-05-11) cited in the application column 4, line 53 - column 7, line 2	1-9
Α	EP 1 482 581 A2 (SONY CORP [JP]) 1 December 2004 (2004-12-01) paragraph [0057] - paragraph [0061]; table 1	1-9

Further documents are listed in the continuation of Box C.	X See patent family annex.		
* Special categories of cited documents :	WT		
"A" document defining the general state of the art which is not considered to be of particular relevance	"T" later document published after the international filing date or priority date and not in conflict with the application but cited to understand the principle or theory underlying the invention		
"E" earlier application or patent but published on or after the international filing date	"X" document of particular relevance; the claimed invention cannot be considered novel or cannot be considered to involve an inventive		
"L" document which may throw doubts on priority claim(s) or which is	step when the document is taken alone		
cited to establish the publication date of another citation or other special reason (as specified)	"Y" document of particular relevance; the claimed invention cannot be considered to involve an inventive step when the document is combined with one or more other such documents, such combination being obvious to a person skilled in the art  "&" document member of the same patent family		
"O" document referring to an oral disclosure, use, exhibition or other means			
"P" document published prior to the international filing date but later than the priority date claimed			
Date of the actual completion of the international search	Date of mailing of the international search report		
10 December 2013	17/12/2013		
Name and mailing address of the ISA/	Authorized officer		
European Patent Office, P.B. 5818 Patentlaan 2 NL - 2280 HV Rijswijk Tel. (+31-70) 340-2040, Fax: (+31-70) 340-3016	Barenbrug-van Druten		

1

### INTERNATIONAL SEARCH REPORT

International application No
PCT/EP2013/068107

C(Continua	tion). DOCUMENTS CONSIDERED TO BE RELEVANT	
Category*	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
A	HUIQIAO LI ET AL: "Enhancing the performances of Li-ion batteries by carbon-coating: present and future", CHEMICAL COMMUNICATIONS, vol. 48, no. 9, 1 January 2012 (2012-01-01), page 1201, XP05504980, ISSN: 1359-7345, DOI: 10.1039/c1cc14764a the whole document	1-9

1

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Information on patent family members

International application No
PCT/EP2013/068107

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